

Refrigeration Load Estimating Manual (RLE)

Technical Bulletin



Engineering ManualRefrigeration Load Estimating

Krack Corporation

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This Krack Manual was published for the purpose of providing a concise, complete and convenient load estimating reference volume for the commercial refrigeration industry. Application suggestions and unit cooler selection examples are representative for halocarbon direct expansion fed systems.

Load estimating data can be used for industrial refrigeration systems using ammonia or brine as the refrigerant.

Estimating guidelines and rules of thumb, are necessarily general in nature, and should not be utilized as the sole design criteria.

Product freezing and cooling data was developed in the Krack product testing laboratory. Other data has been extracted by permission from various ASHRAE Guide and Data Book publications.



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PRINCIPLES OF HEAT TRANSMISSION

PRELIMINARY CONSIDERATIONS

Calculation of the heat transfer through the walls, floor and ceiling of a refrigerated space requires determination of the overall coefficient of heat transmission (or 'U' value, as it is commonly called) for the building structure.

Accordingly, the procedures utilized to determine this coefficient, and the several factors which affect its value, are briefly discussed below.

It is to be noted that rapidly increasing energy costs have made obvious the desirability of optimum insulation efficiency. First-versus-operating cost comparisons are therefore worthwhile, and will often justify an increase in the indicated insulation thickness.

Letter symbols utilized herein are those most commonly employed to designate the various heat transfer factors.

THERMAL CONDUCTIVITY (K)

Thermal conductivity is defined as the rate of heat transfer through a homogeneous material in Btu per hour per square foot of area per °F temperature differential per inch of thickness (NOTE: A homogeneous material is one whose thermal conductivity is essentially unaffected by a change in surface area or thickness).

Conduction heat transfer varies directly with thermal conductivity, surface area, temperature differential and time, and varies inversely with material thickness. Accordingly, the heat transfer into a refrigerated space may be reduced either by selecting an insulating medium with a lower K value, or by increasing the insulation thickness.

The daily heat transfer through any homogeneous material of a given thickness may be calculated by utilizing the following formula:

Q Btu / 24 hrs =
$$\frac{K \times Area_{sq ft} \times TD_{op} \times 24}{Thickness_{in}}$$

K always expresses a heat transfer value per inch of thickness in air conditioning and refrigeration considerations.

CONDUCTANCE (C)

Thermal conductance (C) differs from thermal conductivity (K) only in that it is a heat transfer factor for a specific building material having a standard thickness. All non-homogeneous materials are necessarily rated in this manner (as opposed to K), examples being tile & concrete block. Building boards and paper, flooring materials, air spaces and various materials common in general construction are also rated by C values.

Thermal conductance is by definition, therefore, the rate of heat transfer through a specific material in Btu per hour per square foot of area per °F temperature differential.

Conductances for various material categories are tabulated in Table 1B in the Appendix.

It is to be noted that the formula listed above for calculating heat transfer through various thicknesses of homogeneous substances would not apply for materials rated by conductance.

SURFACE FILM CONDUCTANCE (f)

The surface of any material offers an additional resistance to heat flow, with the absolute value being dependent upon its reflectivity, degree of roughness, attitude (vertical or horizontal), length and the air velocity over the surface.

The reciprocal of this resistance is the surface film conductance (f) which is expressed in the same units as conductance (ie, Btu per hour per square foot of area per °F temperature differential.)

Inside surface film conductance is designated by f_i , and may usually be estimated at 1.60 for walls in still air not exposed to outdoor conditions.

Outside surface film conductance is designated by f_0 , and may be approximated at 6.0 for outdoor walls not exposed to winds in excess of 15 MPH.

PRINCIPLES OF HEAT TRANSMISSION

THERMAL RESISTANCE (R)

Thermal resistance is the resistance of a material to heat flow and is, by definition, the reciprocal of a given heat transfer coefficient (ie, C, f_i , f_o etc.):

$$R = \frac{1}{C}$$

As an example, the conductance (C) of ½ inch plaster board (as obtained from Table 1B) is 2.25 Btu per hour per °F temperature differential per sq. ft. Accordingly, its resistance is:

$$R = \frac{1}{2.25} = 0.449$$
°FTD / sq ft / Btu / hr

This means that a temperature differential of 0.449°F would be required to transfer 1 Btu of heat across 1 square foot of ½ inch plasterboard surface in 1 hour.

The practical significance of resistance (R) is that its values are additive thereby enabling the calculation of overall coefficients of heat transfer for compound structures, ie:

$$R_{Total} = R_1 + R_2 + R_3$$
 (etc.)

OVERALL COEFFICIENT OF HEAT TRANSFER (U)

The overall coefficient of heat transfer of a given material or compound structure with parallel surfaces is commonly known as the U factor, and is expressed in the same units as conductance (ie, Btu per hour per square foot of area per °F temperature differential). It is most generally applied to compound structures such as roofs or walls.

As stated previously, resistance is the reciprocal of conductance and the individual resistances of a structure are additive. Accordingly, it is necessary to determine the overall resistance to heat transfer, and then its reciprocal, to calculate the U factor.

Overall resistance in a compound structure is:

$$R_{Total} = \frac{1}{C} + \frac{X_1}{K_1} + \frac{X_2}{K_2} + \frac{1}{f_1} + \frac{1}{f_0}$$

Where,

- C is the conductance (if it applies.)
- X₁, X₂, etc. are material thicknesses.
- K₁, K₂, etc. are conductivities.
- fi is the inside film conductance.
- fo is the outside film conductance.

The U factor is then calculated as follows:

$$U = \frac{1}{RTotal}$$

An example is useful in illustrating the above. A representative compound structure with parallel surfaces as depicted in Figure A has been selected for this purpose since it is dealt with frequently in refrigeration applications.

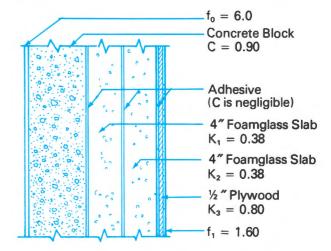


FIGURE A: EXAMPLE CROSS SECTION

In the above example, R_{Total} would equal:

$$R_{Total} = \frac{1}{0.90} + \frac{4}{0.38} + \frac{4}{0.38} + \frac{0.5}{0.80} + \frac{1}{1.60} + \frac{1}{6.0}$$
or,
$$R_{Total} = 23.58$$
and,
$$U_{Overall} = \frac{1}{R_{Total}} = \frac{1}{23.58} = 0.042$$

JOB SURVEY AND LOAD ESTIMATE

JOB SURVEY

Part II of Krack Survey and Load Estimate Form LE-1 is devoted to the job survey. All factors which affect the rate of heat gain must be detailed. It is suggested that each application be thoroughly reviewed with the operating personnel to determine facility operational characteristics, product pulldown requirements, packaging specifics and such other details as are peculiar to a given application.

Particular attention should be given to the means and frequency of product entrance, adjacent area pressure differentials, existing or required ventilation systems, and related operating characteristics which may produce infiltration loading above the norm (the average air changes detailed in Tables 4A and 4B are intended for standard applications only, and should not be used when specialized conditions prevail).

The product entrance rate, condition and type packaging must be determined to assure an accurate product load estimate. If an individual product is treated as a heat exchanger, the product refrigeration load is then

dependent upon its shape, size and type of packaging, as well as the more usual considerations of entering and leaving temperature differential, product type, entrance rate into the cooler, air temperature and velocity over the product and process duration. A prime purpose of the survey, therefore, is to determine the rate of product heat evolution (or rate of heat transfer from the product to the room). Specific examples of various product situations are given in the section devoted to the load estimate.

Part IV of Form LE-1 provides for a sketch of the refrigerated space. All relevant construction features such as column, door and partition locations, ceiling clearances, adjacent area conditions, etc. should be detailed. Supplemental photographs of significant building features are often part of a good survey. Additional survey requirements such as ambient design, room temperature, dimensional data, insulation type & thickness, electrical service and the various miscellaneous loads are self-explanatory.

LOAD ESTIMATE

GENERAL

Part III of Krack Form LE-1 is devoted to calculation of the refrigeration load. Five sources of heat gain must be estimated:

- Wall, floor,& ceiling transmission load
- Solar load
- Infiltration load
- Product load
- Supplemental load

Optimum and efficient equipment selection is dependent upon an accurate determination of each of the above loads.

A brief discussion of each heat gain source follows, with references made where appropriate to factors and data charted in the appendix.

TRANSMISSION LOAD

The heat transmission into a refrigerated space through its ceiling, floor and walls is a function of the outside surface area, the temperature differential between the room and its surrounding area and the thermal conductivity of the insulation utilized.

Table 1A converts thermal conductivity ('K' in Btu / hour / sq ft / °F temperature differential / inch of thickness) to 24 hour heat gain factors for various thicknesses of commonly used insulation materials at temperature differentials from 1 to 130°F. These factors should be inserted where indicated in Part III, Section A of Form LE-1, and multiplied by surface area to obtain the 24 hour transmission heat gain.

For materials other than those tabulated, or for compound structures, refer to Table 1B for the appropriate thermal conductivities and calculate the overall coefficient of heat transfer (U) as illustrated in the foregoing section. This is then converted to a daily heat gain factor by utilizing the following formula:

It is common practice in calculating heat transmission for low temperature rooms to ignore the resistances of both surface films and the building structure proper since their overall effect is quite nominal.

Heat gain factors for various floor designs are tabulated at the bottom of Table 1A. It is the usual practice to assume a factor of 1 Btu / sq ft / °F / 24 hrs for freezer floors with conventional insulation.

SOLAR LOAD

The heat gain through solar radiation is a function of the exposure, type of surface, latitude, altitude, time of year, time of day and other factors. For load estimating purposes, however, this sun effect can be compensated for by adding the degrees shown in Table 2 to the normal temperature differential as indicated in Section A of the load calculation form.

In instances where the refrigerated facility is on (or adjacent to) a highly reflective surface such as sand or water, the allowances shown in Table 2 should be increased by 50%

INFILTRATION LOAD

Infiltration into a refrigerated room will occur when a door is opened as a result of the difference in density between the warm and cold air.

Since door openings vary widely, it the usual practice to estimate infiltration in air changes per 24 hours as shown in Tables 4-A and 4-B. This may then be factored by the room volume and the heat removed in cooling outside air to storage conditions in Btu/cu ft as tabulated in Table 5 to obtain the infiltration load. Space is provided in Part III, Section B of Form LE-1 for computation of this load.

Infiltration may be determined more precisely by calculating the air velocity through the door, the door area and the heat removed in cooling entering air to room conditions, and then estimating the average number of minutes per hour that the door will be open.

The average air velocity in either half of a door 7 feet high at a 60°F temperature differential is 100 feet per minute. Since velocity varies directly with the square root of the doorway height and the square root of the temperature differential across the door, actual air velocity for any set of conditions may be calculated by utilizing the following formula:

Vel fpm =
$$100 \times \frac{\sqrt{H}}{\sqrt{7}} \times \frac{\sqrt{TD}}{\sqrt{60}}$$

or,

Vel fpm =
$$4.88 \times \sqrt{H} \times \sqrt{TD}$$

As an example, the velocity thru a door 8 ft wide and 9 ft high, with a temperature differential of 100°F, is:

$$Vel = 4.88 \times \sqrt{9} \times \sqrt{100}$$

$$Vel = 146.4 \text{ fpm}$$

Were the door in this example open 15 min per hour in a 12 hour shift operation, the 24 hour infiltration would be computed as follows:

Cu ft = Vel fpm
$$\times \frac{\text{Door Area }_{\text{ft}^2}}{2} \times \text{Time Open }_{\text{min}}$$

or,

Cu ft =
$$146.4 \times \frac{(8 \times 9)}{2} \times 180 = 948,672$$

This would then be factored by the heat gain per cu ft from Table 5 in the usual way. An alternate approach is to determine the enthalpy difference between room and entering air from the psychrometric chart, and utilize the following formula:

Heat Gain Btu / 24 hrs =
$$24 \times 4.5^{1} \times \text{Cfm} \times \Delta h$$

or,

Heat Gain Btu / 24 hrs = 108
$$\times$$
 Cfm \times Δ h

In cases where **positive ventilation** is applied to a space, this load would then replace the infiltration load (if greater).

Note 1: Converts Cfm to lbs/hr (refer to Table 48, Pg. 47).

PSYCHROMETRICS

The Psychrometric Chart is utilized to determine the infiltration heat gain for specialized conditions, or for temperature changes not tabulated in Table 5.

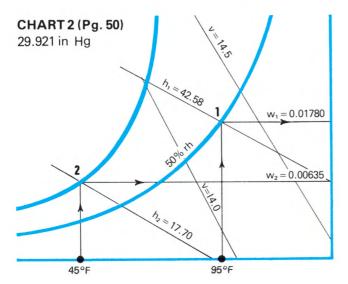
Charts 2 and 3 at the rear of the Appendix are applicable to normal temperature (32°F to 130°F) and low temperature (-40°F to 50°F) conditions, respectively. Both charts are based on a standard atmospheric (or sea level) pressure of 29.921 in Hg , and must be corrected for other altitudes.

For purposes of approximating infiltration loads at higher altitudes, it may be assumed that:

- · Relative humidity (rh) remains constant,
- Enthalpy (h) and humidity ratio (w) increase 2% and 5% respectively per 1000 ft increase in altitude, and,
- Volume (v) for a given dry bulb and humidity ratio is inversely proportional to atmospheric pressure.

Atmospheric pressures at various altitudes are tabulated at the bottom of Chart 3.

An example is useful in demonstrating the use of the psychrometric chart in the calculation of infiltration heat gain. Assuming an infiltration rate of 500 Cfm, an entering air condition of 95°F dbt & 50%rh and a cooler temperature of 45°F, characteristics of the entering and cooled air are first determined as in Figure B:



SCHEMATIC SOLUTION OF EXAMPLE

As indicated in Figure B, the properties of the entering and cooled air are:

$$\begin{split} &h_1=42.58 \text{ Btu} / \text{ Ib of dry air} \\ &w_1=0.01780 \text{ Ib } H_2\text{O} / \text{ Ib of dry air} \\ &v_1=14.25 \text{ Cu ft} / \text{ Ib of dry air} \\ &h_2=17.70 \text{ Btu} / \text{ Ib of dry air} \\ &w_2=0.00635 \text{ Ib } H_2\text{O} / \text{ Ib of dry air} \end{split}$$

Infiltration heat gain may then be calculated as follows:

Heat Gain Btu / hr =
$$4.5 \times \text{Cfm} \times (h_1 - h_2)$$

or,
Q = $4.5 \times 500 \times (42.58 - 17.70) = 55,980 \text{ Btu / hr}$

For an 8 hour shift operation, the 24 hr infiltration heat gain would therefore be 447,840 Btu, and this load would be inserted in the space provided in Part III, Section B of Form LE-1.

The above calculation provides a conservative load estimate since it presupposes that the total heat removed from the entering air is transferred to the evaporated refrigerant. This is not the case in as much as heat leaves the coil box as well via the heat content of the condensate. Accordingly, precise calculation of the refrigeration load in any instance in which entering air is cooled below its dew point would be calculated as follows:

$$Q_{Btu/hr} = 4.5 \times Cfm [(h_1 - h_2) - (w_1 - w_2) h_W]$$

This effect is illustrated by comparing the 1.746 Btu / cu ft $\left(\frac{42.58-17.70}{14.25}\right)$ heat removal indicated

with the 1.710 Btu/cu ft tabulated in Table 5 for comparable conditions.

Additionally, the factor of 4.5 utilized to convert Cfm to lbs / hr incorporates the standard (70°F) dry air conversion factor of 13.33 cu ft / lb. Obviously, therefore, additional safety is built into the sample calculation since utilization of the actual entering volume of 14.25 cu ft/lb would result in a lower mass flow.

It is to be noted that the psychrometric chart is useful in calculating numerous other processes involving the conditioning or mixing of moist air, and that no attempt was made in this manual to fully develop the subject.

PRODUCT LOAD

The heat gain from product loading may consist of one or more of the following:

- · Sensible heat removal above freezing
- Latent heat
- Sensible heat removal below freezing
- Heat of respiration

Sensible heat is calculated by factoring the **daily rate** of product in lbs per 24 hours by the temperature reduction and the product specific heat (the specific heat being the number of Btu's required to lower 1 lb of a substance 1 degree fahrenheit).

Latent heat is calculated by factoring the **daily rate** of product in lbs per 24 hours by the product latent heat of fusion (the latent heat being the number of Btu / lb required to freeze the product).

Applicable formulas are:

QSens
$$Btu / 24 hrs = Daily Rate \times \Delta T \times Sp. Ht.$$

Specific heats (above and below freezing) and the latent heats of fusion for commonly encountered products are detailed in Table 9. Product loads may be figured in the space provided under Part III, Section C of Form LE-1.

As stressed in prior comments relating to the job survey, it is imperative that the rate of product heat evolution be accurately determined. Therein is the significance of **daily rate**, since it is, by definition, the amount of product cooled or frozen per hour multiplied by 24 hours. This may be illustrated by considering two freezers, each of which has been loaded with 10,000 lbs of unfrozen product. In the first instance, eviscerated chickens are to be blast frozen in 2 hours, with the resultant **daily rate** being:

Daily Rate lbs/24 hrs =
$$\frac{10,000}{2} \times 24 = 120,000$$

In the second case, the product is packaged, boxed, and palletized, and therefore requires 16 hours to give up its heat. Accordingly, the **daily rate** is:

Daily Rate lbs/24 hrs =
$$\frac{10,000}{16} \times 24 = 15,000$$

PRODUCT CHILLING

Product chilling is a process wherein product temperatures are rapidly reduced to a level acceptable for processing or shipment. Examples are freshly slaughtered carcasses and recently harvested fruits or vegetables. The benefits of rapid temperature reduction, in each instance, are a reduction in shrinkage and the deterrence of bacterial growth.

The introduction of hot product into a chill room results in the concentration of a significant load segment during the initial cooling period. This initial high rate of product heat evolution is caused by the high temperature and vapor pressure differentials between the product and the room. The effect is illustrated in Figure H, Page 29, wherein temperature reduction versus chill time for hogs is graphically depicted.

Load factors (or chill factors as they are sometimes called) have been developed to compensate for the non-uniform distribution of product load which results. These are utilized to increase the average hourly product load which would otherwise apply. Factors for the products most commonly encountered in chilling applications are charted in Table 10, and should be inserted in the space provided in Part III, Section C of Form LE-1 when applicable. The overall refrigeration requirements for beef and pork chilling rooms are charted in Page 28, Tables 11 and 12, respectively.

As an example, laboratory testing has shown that hogs tend to give up their heat during the initial portion of their chill at a 45% greater rate than is average for the complete period. Accordingly, the load factor indicated is 1.45.

PRODUCT CHILLING (CON'T.)

Failure to apply a load factor to the average hourly load (when applicable) will result in an unacceptably high initial room temperature, and an extension of the chill time required.

The substantial reduction in product load during the latter portion of the chill (15-25% of peak load) makes it mandatory that the refrigeration system be designed for proper function under a wide variance in load condition. Properly staged capacity reduction, in conjunction with evaporator pressure regulating valves, is commonly employed. Other approaches include the application of multi-circuit DX coils, and the combining of other (and more constant) side loads with the basic chill room load to enable high side equipment to stay on line and track the chill load as it tails off.

Suction accumulators and liquid-suction heat exchangers are strongly recommended with close coupled DX halocarbon systems.

PRODUCT CHILLING & HOLDING

Frequently, the same room is utilized to accommodate both the product chilling and long term storage requirements. This is particularly true in the case of apples and pears.

In such rooms, the peak load varies with the duration of the loading period and the maximum percentage loaded on any given day. Normally, however, it is **neither necessary nor advisable** to apply a load factor to the average hourly load since an unacceptable disparity between the peak and holding requirements will result (see Note 5, Table 10).

A common load estimating technique for combined fruit chilling and storage applications is to add the 24-hour pulldown requirement for the last day's loading to the normal room holding load (the apple storage loads charted in Table 16 were computed on this basis).

A prime consideration in this regard is that the on-hand pre-chilled product produces a flywheel effect which minimizes the increase in room temperature which would otherwise result.

Combined chilling and holding facilities may require that existing prechilled product be segregated (either by physical partition or zoned air distribution) from the newly introduced hot product. Otherwise, the significant increase in room relative humidity which results upon the introduction of hot product will produce condensation on the prechilled product. Meat, for example, will sweat and slime, and the bacterial growth rate will be greatly enhanced (meat processed under such conditions would not meet with USDA acceptance).

As is the case with rooms applied for product chilling only, particular attention must be given in the refrigeration plant design to the wide disparity between the peak and normal holding loads. In a fruit storage facility, for example, the winter holding load will approximate 10 to 15% of the peak refrigeration requirement, and the coil TD under holding conditions may, therefore, be only 2-3°F (versus the 15°F and higher TD's experienced under peak pulldown conditions).

Accordingly, flooded or recirculated refrigerant systems are the most frequently utilized since they adapt well to the wide control variance required. When a DX halocarbon system is applied, the comments detailed above under "Product Chilling" apply. Unit coolers with multispeed fans are sometimes utilized, but should be applied with discretion given the necessity for positive air circulation through the load during storage.

As a final consideration, the refrigeration design engineer should remember that his responsibility is confined to the creation and maintenance of a specific room environment. It is neither his function or purpose, nor is it within his capability, to guarantee a given product core temperature within a specified time frame given the many variables (product condition, packaging, wrapping, entrance rate, means of storage, etc).

PRODUCT BLAST FREEZING

Air blast freezing offers an alternative to the conventional contact method wherein the product is placed in direct contact with pipes or plates thru which refrigerant or brine is piped.

Batch freezing is a process wherein the complete product load is placed in the room and frozen in one loading. The resultant load profile approximates that previously described for chill rooms in that a major portion of the load is concentrated during the initial freezing period. Accordingly, a factor of 1.5 is applied to the average hourly load, and the Daily Rate on Form LE-1 is computed by:

$$\text{Daily Rate} = \frac{\text{Product Load}_{\text{lbs}}}{\text{Freezing Period}_{\text{hrs}}} \times 24 \times 1.5$$

The 1.5 factor is **not** to be used when products are frozen over an extended period (these usually being products which are packaged or otherwise not susceptible to significant moisture loss during freezing).

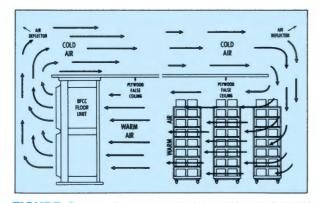


FIGURE C: BATCH FREEZING (FLOOR MOUNT)

Continuous load freezing is a process wherein the product is fed continuously thru the freezer via a conveyor or systemized manual feed. In this type of application, the estimated time of product heat removal has little effect on the total refrigeration load (it does, however, affect room size, conveyor belt size and speed, etc).

Accordingly, **no load factor is applicable** and the Daily Rate is computed by:

Daily Rate =
$$\frac{\text{Product Load }_{\text{lbs}}}{\text{Process Duration }_{\text{brs}}} \times 24$$

Air temperature, air velocity, product loading technique, and space requirements are critical considerations in the design of blast freezing systems (it seems that adequate space for both the equipment and product is never available). Additional comments, and general guidelines, are detailed in the preamble to Example II, Pg. 14.

Figures C, D & E depict typical room layouts for batch and conveyor-fed blast freezers.

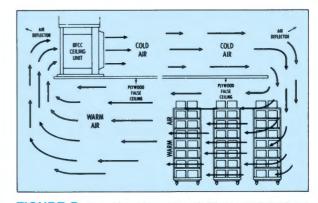
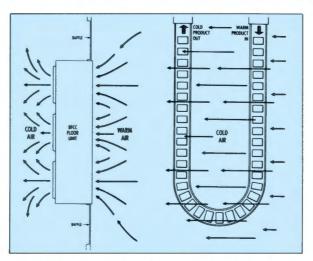


FIGURE D: BATCH FREEZING (CEILING MOUNT)



Note 1: As a product freezes, its outer frozen portion becomes an insulator and its rate of heat evolution decreases accordingly.

FIGURE E: PROCESS BLAST FREEZING

RESPIRATION

Fruits and vegetables are living organisms which continue to respire and carry on certain other life processes after harvesting. The carbon in the product combines with the oxygen in the air with the resulting chemical process being exothermic. This, in turn, results in an additional room heat gain.

The heats of respiration for various products in Btu/lb/24 hrs are tabulated in Table 9 at the temperatures recommended for both long and short term storage. Respiration heat (or reaction heat as it is sometimes called) varies with temperature, and decreases significantly with a reduction in storage temperature. There is no correlation, however, between respiration and relative humidity.

Since living organisms are involved, the temperature in long term storage rooms should be controlled within 1°F; otherwise, the physiology of the product will be affected, and the dormant state in which it has been maintained will be disturbed.

Meats and fish have no continuing life process, and therefore generate no heat in storage.

The respiration heat in controlled atmosphere (CA) storage will be less than the values charted in Table 9 as a result of the reduction in room oxygen content.

SUPPLEMENTAL LOAD

All additional heat dissipated in the refrigerated space must be accounted for in computing the overall load. This includes energy utilized for motors, heaters, lights, people, forklifts and related miscellaneous heat sources. Supplemental loads of this type are computed in Part III, Section D of Form LE-1.

Occupancy loads are tabulated in Table 6. The heat equivalents noted should be increased by 20% if occupancy periods are of short duration. Utilize the average number of personnel in the space.

Heat equivalents for **electric motors** are listed in Table 3 for each possible application (ie, motor and connected load in the refrigerated space, connected load only in the refrigerated space and motor only in the refrigerated space). Equivalent horsepower is determined by multiplying the motor horsepower by the fraction of each hour operated.

Storage room **lighting** may usually be assumed at 1 to 1½ watts/sq ft. Doors, offices and work rooms require 2½ to 3 watts / sq ft. **Forklifts** may be estimated at 4 to 5 hp if more precise data is unavailable, and should be converted to equivalent horsepower as above.

The **defrost heat load** in a refrigerated space varies with the rate and time which heat is required, and, in some cases, with the unit cooler design. In section D of

Form LE-1, 25% of the heat imposed is arbitrarily allocated to room load (the assumption being that this amount is either radiated to the room or retained by the coil mass, with the remainder leaving via the coil condensate.

Charts, trays, racks, pallets, etc. seldom contribute a significant load, but must be accounted for in high volume operations.

Electric energy from any source may be estimated by multiplying the applicable wattage by 82 (24 hrs \times 3.4 Btu / Watt / hr).

HOURLY LOAD CONVERSION

The 24 hour total obtained by adding Sections A thru D of Part III, Form LE-1 is converted to design refrigeration load in Btu/hr by applying time cycle and safety factors.

Time cycle factors for various applications are charted in Table 8. The divisors listed in column 1 represent anticipated operating hours under various frost conditions. The operating times noted are average, and are not applicable to all applications. Some freezers, for example, may require defrosting only once daily (or, in extreme cases, once weekly). The factor selected, therefore, represents a judgment consideration based upon the amount of moisture expected to enter the space from infiltration, product shrinkage, etc.

A safety factor correction of 5 to 10% to the hourly load resulting above is suggested. The figure selected is, again, a judgment consideration. Factors in excess of 10% should not be necessary.

OTHER CONSIDERATIONS

Data herein, and the overall format of Form LE-1, both presuppose a "total load" estimating approach (ie, the combining of sensible and latent loads). Accordingly, evaporative loads such as those resulting from product moisture loss, wash water, etc. have not been considered since they have no net effect on the total room load (the resultant latent heat gains serve as credits to the sensible heat load due to the evaporative cooling effect).

This approach satisfies the requirements of most applications. This is particularly the case with freezers at 15°F or below since variation of the Apparatus Dew Point (ie, the average coil surface temperature) has little or no effect on the sensible heat factor, or the moisture removal capability of the coil.

Further, adherence to the guidelines charted in Tables 17 and 18 for recommended coil TD will produce required room relative humidities in most instances. In those cases where long storage under close humidity control is indicated, however, the possible requirement for reheat or re-humidification must be investigated.

I. FRUIT CHILLING AND STORAGE:

The example below illustrates the load profile for a typical combination chilling/holding facility. Three common product load estimating techniques are shown, with the pre-calculated values charted in Table 16 offering the simplest approach (note that respiration heat is neglected when a load factor is applied to the average hourly pulldown load).

Room design dry bulb varies with product variety. The control temperature for apples, as an example, ranges from 38°F for McIntosh (as shown) to 32°F for Golden Delicious. Relative humidity is maintained at 85% for apples, and 92-95% for pears. Room condition is not significantly affected by daily product loading due to the flywheel affect of the on-hand prechilled fruit. (Note that room temperature only should be guaranteed, and that no commitment as to time required for product pulldown should be made due to the many uncontrollable factors. (ie, type of packaging, position in the load, method of stacking, etc.).

Fruit stored for extended periods (over 3 months) is usually maintained under controlled atmosphere (or C.A.) storage conditions wherein the O_2 concentration is reduced from the normal 20% to a level of 3-7%, with a corresponding increase in the CO_2 level from a trace to 2-5% (the purpose of C.A. storage being to minimize product deterioration during storage). Respiration heat is reduced to a fraction of the normal rate as a result of the low O_2 concentration. C.A. storage facilities are commonly sub-divided into $50' \times 100' \times 20'$

modules to enable product availability in saleable quantities when the room seals are broken. Water defrost and 460V TENV motors are frequently utilized to maximize reliability, and control devices are externally mounted for serviceability given the non-accessible environment.

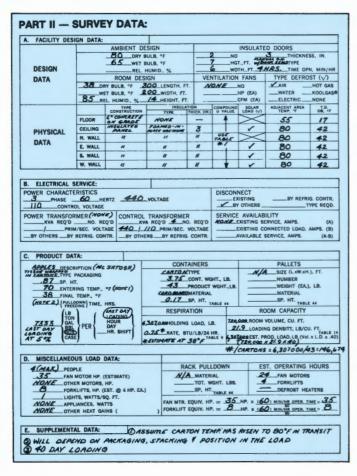
Apples are usually containerized in lug or wood boxes, or in fiber cartons. The fruit may be individually tissue wrapped, or placed in poly-bags. Ungraded fruit is stored in 1000 lb $2\frac{1}{2}$ ' \times 4' \times 4' tote bins. Product loading density averages 25 lb/cu ft.

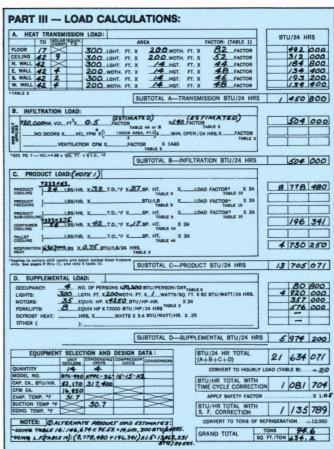
The refrigeration system for a combination chilling/holding facility must be specifically designed for adequate function under the widely divergent pulldown and winter holding loads. Since operational coil TD's will range from 15°F (or higher) during pulldown to 2°F (or less) with the winter holding load, flooded or recirculated systems are the most readily adapted to fruit storage applications.

When a DX system is applied, it must incorporate properly staged capacity reduction in consideration of the wide load variance. Multi-speed fan motors may also be applied, but have an obvious adverse effect on air movement thru the load.

Coils should be selected for a **6-8°F TD** to maintain required humidity. Since all rooms require defrosting, a **4 FPI** coil design is recommended.

Refer to the text, Pg. 10, for more detailed information.





II. BLAST FREEZING:

As illustrated in the example, the load profile of a batch blast freezing process dictates the application of a **load factor** to the average hourly load which would otherwise apply. The result is a refrigeration system properly adapted to the initial high rate of product heat evolution. The usual factor is **1.5**, but a lower number is sometimes applied based on experience. In general, products with high surface-to-weight ratios freeze in 2 to 4 hours, and lower factors are therefor applicable when an extended freezing period is allowed. Note that **no load factor should be applied to conveyor fed blast freezers**, or to rooms equipped with single halocarbon refrigeration systems (in the latter, freezing time should be extended, and the room temperature allowed to rise).

Special design considerations include the provision for room pressure relief, and the consistent problem of obtaining adequate space to accommodate both the equipment and product. Provision for heater pull space must be made with electric defrost units. Utilization of coils with variable fin spacing minimizes the defrost requirement.

The following procedure should be followed in arriving at a blast freezer design:

STEP 1: Determine whether a conveyor or batch loaded freezer is best applied. This judgment is usually based on product test data wherein freezing time with various air temperatures and velocities has been determined. In general, batch loaded freezing is applied with products requiring 1½

hours or more to freeze satisfactorily; products which freeze in less than 1 ½ hours are conveyor fed.

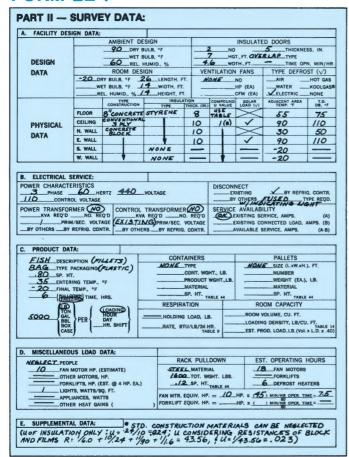
STEP 2: Determine the space limitations of the room (remember that the space initially allocated by others is frequently insufficient to accommodate both the equipment and the product).

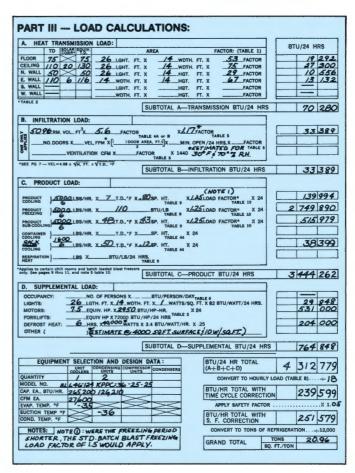
STEP 3: Finalize the room design criteria, keeping in mind that design air velocity and temperature are most critical, and that these factors are the prime considerations in the selection of a blast freezing unit.

STEP 4: Select equipment as dictated by room size and product mass, and which is in conformance with the required air temperature and velocity as finalized in Step 3 (following review of the pilot freezing test results). The equipment employed should be specifically designed for blast freezing application, and should be capable of producing extremely high air velocities and volumes.

STEP 5: The last step is to position the unit in the room. Refer to Figures C & D, Pg. 11, for typical batch loaded blast freezers. Note that the air travels from right to left in these diagrams, passing thru the product and gradually warming up before being returned to the coil. A critical requirement in blast freezing of this type is that product be loaded across the complete room width thereby precluding the cold air bypass which would otherwise destroy the effectiveness of the freezer.

Refer to the text, Pg 10, for further discussion, and to Table 13, pg. 28, for test blast freezing data on selected products.





III. BEEF CARCASS CHILLING:

The load characteristics of a carcass chill room (or the "Hot" cooler, as it is commonly called) are such that the application of a load factor to the average hourly product load is mandatory. The initial rate of heat evolution has been shown by test to exceed the average hourly rate by 50%. Hence the load factor applicable is 1.50. The typical load profile is illustrated in figure H, Page 29, wherein time/temperature curves for Hot Chilling are plotted.

Other specialized design and operational requirements apply. Rail height as dictated by USDA must be 11'2", and a 4 to 5 ft clearance above the rails is required for supporting structure and equipment placement; accordingly ceiling height should be 16 ft at a minimum. BTR units are specifically designed for this application, and should be utilized whenever possible (these units will accommodate 2 rails on either side).

Small plants can present particular problems. Frequently,12 or 14 ft ceiling heights are encountered, as is the placement of structural steel within the envelope. In an application of this type, it is essential that the refrigeration be coordinated with the structure to assure a clear air flow at the discharge of the unit coolers. Hite-saver® or draw-thru type unit coolers must be flush mounted with the ceiling around the periphery of the

An additional USDA requirement is that drain pans be insulated to prevent drippage on the product; stainless enclosures as found on the BTR series are optimum.

Unit coolers should be of 4 FPI coil construction, and be selected for a 10-12°F TD (the initial TD will approach 18-20°F, but will drop rapidly with the fall-off in load). Variable fin spacing (wherein the first 2 rows are of 2 FPI construction) minimizes the defrost requirement, but is not recommended for DXF applications since a 2 fin per inch coil face produces marginal superheat.

Defrost is usually accomplished 4 times daily, with each cycle being of 15 to 20 min duration. Small rooms usually approximate 40 sq. ft. /ton, with large facilities approaching 65-70 sq. ft. /ton. The following guidelines may be applied:

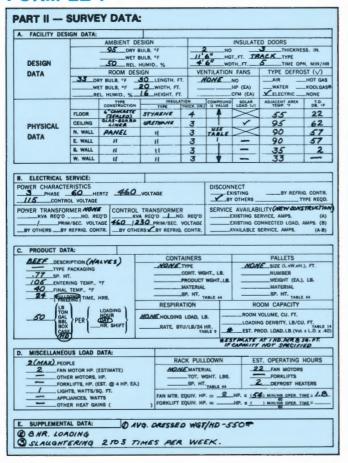
• 5 head per ton

8 sq ft per head

The refrigeration plant should be designed to adapt to the wide load variance. Multiple compressors with unloaders are recommended (a twin unit is illustrated in the example). Improperly applied equipment will short cycle, pump-down the coils, and thereby dry out the product.

As a final consideration, it should be noted that round temperature cannot be pulled down in 18-24 hours. Accordingly, a product load must be estimated for the **holding cooler** which will approximate a 15 degree, 24 hour pull-down of 10% of the carcass weight (utilize 20% of the overall weight for small rooms).

Refer to USDA handbook 191 for detailed meat packing-plant design guidelines, and to tables 11 & 12, Pg. 28, for precalculated chill room loads.



PART III — LOAD CALCULATIONS:
A. HEAT TRANSMISSION LOAD: BTU/24 HRS
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N. WALL 57 57 30 LOHT FT X /6 HGY FT X 59 FACTOR 20 320
E. WALL 67 - 57 20 WOTH. FT. X 16 HGT. FT. X 59 FACTOR 10 880
S. WALL 2 - 2 30 LGHT. FT. X 16 HGT. FT. X 2 FACTOR 960 W. WALL - WOTH. FT. X HGT. FT. X FACTOR
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VEL. 488X VM SX V57 = 124.9 SUBTOTAL B-INFILTRATION BTU/24 HRS 747 759
C. PRODUCT LOAD:
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PRODUCT LBS/HR. X BTU/LB X LOAD FACTOR* X 24
PRODUCT 1 (BS/HR X TD °F X SP HT X LOAD FACTOR® X 24
SUB-COOLING) TABLE 9 TABLE 10
CONTAINER] LBS/HR. X T.D., F X SP. HT. TABLE 44 X 24
PALLET COOLING TABLE 44
RESPIRATION LBS X_BTU/LB/24 HRS.
*Applies to certain chill regers and batch loaded blest frequen
unify. See pages 9 thru 11, and note 5 table 10. SUBTOTAL C—PRODUCT BTU/24 HRS 2 064 562
D. SUPPLEMENTAL LOAD:
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MOTORS:
DEFROST HEAT: HRS. X WATTS X 3.4 BTU/WATT/HR. X .25 (MISLEST)
OTHER ():
SUBTOTAL D-SUPPLEMENTAL BTU/24 HRS 278 400
EQUIPMENT SELECTION AND DESIGN DATA: BTU/24 HR TOTAL
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TIME CYCLE CORRECTION /45 394
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SUCTION TEMP °F 20 BTU/HR TOTAL WITH 145 594
6.1. Connection
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A GREATER FACTOR WITH SMALL ROOMS GRAND TOTAL SO. FT. TON 49.6

IV. BEER STORAGE:

Beer storage facilities are refrigerated for the purpose of maintaining product quality with an extended shelf life (from the usual 90 days, to as much as 180 days at 40°F). The expense is justified by the cyclical nature of industry sales. Storage temperatures vary from 40°F to 76°F, with the control point being adjusted in accordance with the dew point profile of a given area (the reason being that cartoning would otherwise disintegrate upon exposure to ambient conditions). Draught beer (kegs) is stored in a separate cooler since it must be maintained at a constant temperature year-round (the range being from 34°F to 38°F).

The product leaves the brewery's pasteurizer at a maximum temperature of 85°F, with its temperature range prior to arrival at the distribution point increasing (decreasing) 1°F if shipment is by truck, or 1°F per day if shipment is by rail.

Beer is shipped by pallet, with a rail car containing 50 pallets. Car loadings are mixed in accordance with a distributor's sales profile. Kegs may be included with a can or bottle load behind a bulkhead packed with dry ice. Pallets are wood, and vary in weight with location from 36 to 44 lbs. (for cans), to 55 lbs. (for kegs); 42 lbs. is the most common weight encountered with cans or bottles. Dimensions are 32″ × 37″ × 73″.

Pallet refrigeration loads based on a 45°F/24 hour product pulldown are as follows:

TYPE CONTAINER	CASES/ PALLET	BTU/45°F/ 24 HR
 12 oz tray steel can 	98	85,000
 12 oz tray alum. can 	98	84,800
 12 oz Mich¹, N.R. 	56	54,000
• 12 oz N.R., 4/6	77	75,400
 12 oz ret, 24 	49	51,200
 16 oz tray steel can 	77	89,500
 Quart, N.R. 	49	63,200

The following procedure should be followed in estimating the refrigeration load:

STEP 1: Determine facility operational specifics such as method of truck loading (end or side), the percent of presold/scheduled deliveries vs. driver sales, the required number of pallet facings, a 5 year sales projection, the average number of inbound car loads/day, etc.

STEP 2: Following review of the above with operating personnel, define the space to be refrigerated (the primary concern being whether the loading and staging areas should be refrigerated). It is the usual practice to size for expansion planned over a 5 year period.

STEP 3: Determine the distributor's annual sales profile by product category, and compute the average pallet refrigeration load on a weighted average basis.

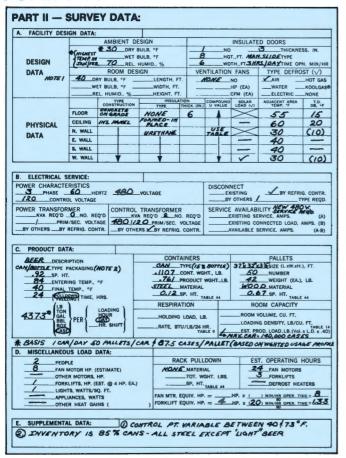
STEP 4: Obtain the area dew point profile, and subsequently establish minimum storage temperature by month.

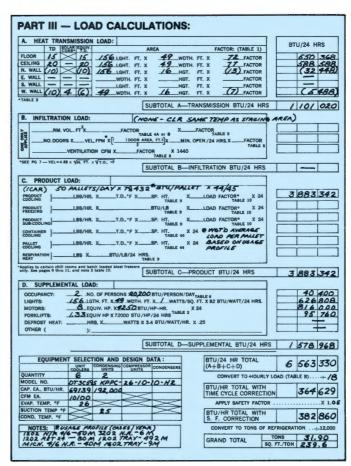
STEP 5: Estimate the heat gain for each of several representative months to determine the peak load. (NOTE: As illustrated in the example, the peak load will occasionally occur during a winter month due to maximum product pulldown requirements).

STEP 6: Review alternate insulation options to those assumed in Step 5 above. A compound U value of .080 is a commonly accepted design, but values as low as .035 are sometimes justified.

STEP 7: Design the refrigeration system for proper function under the load variance determined in Step 5 above. Coil TD is not critical; utilize 6 FPI construction.

See Tables 29 thru 32, Page 37, for additional product load and container data.





V. NUT STORAGE:

Nuts are received from growers during the October thru February harvest season packed in burlap bags. Bag weights vary from 90 lb (for high quality) to 150 lb (for small size, or seedlings); average bag weight is 125 lb, with a truck load being 360 to 400 bags.

Upon receipt at the processing and storage facility, the product is cleaned, sized, and graded, with miscellaneous shells, trash, etc. being removed. It is then segregated into 7 or 8 categories by size, and packed loose in $60'' \times 42'' \times 42''$ wood tote boxes for transfer to storage. Box weights average 170 lbs, with each containing 1800 to 2000 lbs of product. Entrance rate into the cooler is a function of the grading machinery capacity (and **not** the rate of inbound shipments from growers).

Tote boxes are generally stacked 4 high (or 20 ft). The box bottoms and sides are perforated with small holes, and these, in combination with the loosely packed nature of the product, enable adequate air movement thru the load.

Customer orders are filled from storage, with the appropriate size and grade nuts being transferred to the plant area where shelling, cutting and repackaging for customer shipment occur.

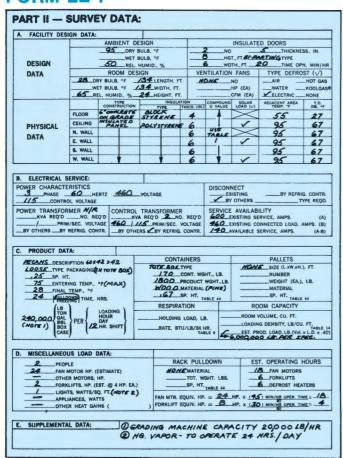
Proper storage room design is 28°F to 32°F with a 65% relative humidity; maintainance of constant humidity is critical. Processing and plant areas are not usually air condi-

tioned. Since the product enters storage during the fall and winter months, the peak pulldown, transmission and infiltration loads are not coincident (note that incoming product during the summer months usually represents inter-warehouse transfer, and is pre-refrigerated).

The usual practice, therefore, is to estimate the load on the basis of the maximum transmission, infiltration and miscellaneous loads only, with the product load neglected. An alternate load estimating technique is to compute the product load based on 24 hr pulldown at the maximum entrance rate, and add the usual transmission, infiltration and miscellaneous loads recomputed for a lower design ambient (were the example refigured on this basis with a 75°F outdoor design, the net effect would be to reduce the transmission and infiltration loads to 1.8 million and 1.6 million Btu/24 hrs, respectively, with the overall load becoming slightly overstated at 60 tons).

Coils should be selected for a 12°F TD, and may be of 4 or 6 FPI construction. Multiple compressors are recommended to adapt to the widely divergent peak and holding loads.

Provision for reheat is usually necessary to assure maintenance of constant humidity under light load conditions. The simplest approach is to de-energize one refrigeration system while continually operating all unit fans, lights, and a predetermined number of defrost heaters (the net effect being to false load the operative refrigeration unit). This approach requires the addition of a humidistat and humidity relay (the function of the latter being to de-energize the required refrigeration circuitry and to activate the defrost heaters).



	SMISSION	LOAD:						BTU/24 HRS
	ORR T.D.		- 1	REA		FACTOR: (
	× 27	134 LG			VDTH. FT. X		_FACTOR	520 72
N. WALL 67		134 10			VDTH. FT. X		_FACTOR	1 418 62
		/34 LG		24		69	_FACTOR	205 82
		/34 LG		24		64	_FACTOR	205 82
W. WALL 67 .	4 7/	134 W	OTH. FT. X	24	IGT. FT. X	69	FACTOR	22/ 90
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VEL . + 488			.s [s	UBTOTAL B	—INFILTRA	TION BTU	/24 HRS	3 027 73
C. PRODUCT								
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				TABLE 1				
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788 m						TAB	DE 10	
(35×)	LBS/HR.	x47_T.	D. F X.6			CONT. 240	000	7// 98
CONTAINER -24	LBS/HR.			ZSP. HT.	X 24 W	CONTO 240	800#	7// 98
CONTAINER 24	LBS/HR.	XT.I), F X	ZSP. HT. YABLE -SP. HT. YABLE	X 24 W	CONTO 240	000	7// 98
CONTAINER 2000LING PALLET COOLING RESPIRATION	LBS/HR. LBS/HR.	XT.(LB/24 HRS. TAE	ZSP. HT. YABLE -SP. HT. YABLE	X 24 W	CONTO 240	800#	7// 98
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COOLING PALLET COOLING PALLET	LBS/HR. LBS/AWI. LBS X. rooms and batch 11. and note 9 NTAL LOAD 2. NO. 1/3-4 LGT 1/8 LGQ 4. LGQ 6. HRT): CONUMER CONUMER 6. CONUMER CONUMER CONUMER CONUMER 6. CONUMER CONUMER CONUMER 6. CONUMER CONUMER CONUMER CONUMER	STU/Ush loaded blast table 10. OF PERSON HI. FT. X / Z UIV HP. X Z X X X X X X X X X X X X X X X X X	LB/24 HRS. VAI I freeters S IS X22502 WIDTH, FT WIDTH, FT WATTS X 300 S DESIGN E COMPRESSO	ZSP. HT. TABLE 4 SSP. HT. TABLE 4 LLE 9 UBTOTAL C D STU/PERSON X. 1. WATT HP-HR. YAMA A STU/WATT, UBTOTAL D WATA: CONDENSERS	PRODUC PRODUC I/DAYTABLE 6 S/90, FT. X 8 A X 24 HR. X .25	T BTU/24 T BTU/24 T BTU/24 T BTU/24 T BTU/24 T BTU/24	HRS 1/24 HRS. TU/24 HRS.	3 53/ 98 (NOTE!) 45 40 / 177 2 59 / 1836 00 288 00 / 185 20
COOLING PALLEY P	LBS/HR. LBS/HR. LBS X rosems and batch I and mote 5 INTAL LOAD I AND I A	STU/Ch loaded blass table 10. OF PERSON IN. FT. X 1.5 UIV. HP. X	LB/24 HRS. VAI I freeters S IS X22502 WIDTH, FT WIDTH, FT WATTS X 300 S DESIGN E COMPRESSO	ZSP. HT. TABLE 4 SSP. HT. TABLE 4 LLE 9 UBTOTAL C D STU/PERSON X. 1. WATT HP-HR. YAMA A STU/WATT, UBTOTAL D WATA: CONDENSERS	# X 24 #F	T BTU/24 T BTU/24 Z BTU, WATT	HRS TU/24 HRS. TOTAL TO HOURLY TO HOURLY TAL WITH	3 53/ 98 (NOTE!) 45 60 1 47 2 59 28 8 00 1 1 8 5 20 5 4 8 2 5 19
D. SUPPLEME! D.	LBS/HR. LBS X LBS X reserve and before 3 NTAL LOAD 1.3 4 LOAD 4 EQU 4 EQU 6 HRI 004 FR 004 FR 0075 FF 98604	STU/Ush loaded blast table 10. OF PERSON HI. FT. X / Z UIV HP. X Z X X X X X X X X X X X X X X X X X	LB/24 HRS. VAI I freeters S IS X22502 WIDTH, FT WIDTH, FT WATTS X 300 S DESIGN E COMPRESSO	ZSP. HT. TABLE 4 SSP. HT. TABLE 4 LLE 9 UBTOTAL C D STU/PERSON X. 1. WATT HP-HR. YAMA A STU/WATT, UBTOTAL D WATA: CONDENSERS	# X 24 #F	T BTU/24 T BTU/24 Z BTU, WATT	HRS TU/24 HRS. TOTAL TO HOURLY	3 53/ 98 (NOTE!) 45 60 1 47 2 59 28 8 00 1 1 8 5 20 5 4 8 2 5 19
COULDING PALLET OF THE PARTY OF	LBS X. LBS X. LBS X. NTAL LOAD 2. NO. 11. and held 5. 11. and held 5. 12. A. LOT 2. NO. 4. EQU 4. EQU 4. EQU 4. EQU 6. HRI 7. SELECTI 0.0017 5. 0.75C 75. 78. EQU 6. A. R.	STU/Ch loaded blass table 10. OF PERSON IN. FT. X 1.5 UIV. HP. X	LB/24 HRS. VAI I freeters S IS X22502 WIDTH, FT WIDTH, FT WATTS X 300 S DESIGN E COMPRESSO	ZSP. HT. TABLE 4 SSP. HT. TABLE 4 LLE 9 UBTOTAL C D STU/PERSON X. 1. WATT HP-HR. YAMA A STU/WATT, UBTOTAL D WATA: CONDENSERS	# X 24 #F	T BTU/24 T BTU/24 AENTAL B U/24 HR MBH C+O COMPRETE COMPRETE	HRS TU/24 HRS. TOTAL TO HOURLY TO HOURLY TAL WITH	3 53/ 98 (NOTE!) 45 60 (17.2 59 / 836 00 288 00 1 16.5 20 1 16.5 20 LOAD (TABLE 8)
COOCHINE COO	LBS X. LBS X. LBS X. NTAL LOAD 2. NO. 11. and held 5. 11. and held 5. 12. A. LOT 2. NO. 4. EQU 4. EQU 4. EQU 4. EQU 6. HRI 7. SELECTI 0.0017 5. 0.75C 75. 78. EQU 6. A. R.	STU/Ch loaded blass table 10. OF PERSON IN. FT. X 1.5 UIV. HP. X	LB/24 HRS. VAI I freeters S IS X22502 WIDTH, FT WIDTH, FT WATTS X 300 S DESIGN E COMPRESSO	ZSP. HT. TABLE 4 SSP. HT. TABLE 4 LLE 9 UBTOTAL C D STU/PERSON X. 1. WATT HP-HR. YAMA A STU/WATT, UBTOTAL D WATA: CONDENSERS	A 24 PRODUC PRODUC (/DAY_ABLE 6 BY/50, FT. X 8 A 2 X 24 HR. X 25 SUPPLEN BT	T BTU/24 T U/47 T T U/47 T T U/47 T T U/47	HRS TU/24 HRS TOTAL TO HOURLY TAL WITH CORRECTIC TETY FACTOR TAL WITH	3 53/ 98 (NOTE!) 45 6 00 288 00 1 183 26 1
COOLING PALLEY COOLING PALLEY	LBS //R. LBS X LBS X TOTAL LOAD 1. sed rate 3 NTAL LOAD 1. Sed rate 3 NTAL LOAD 1. Sed rate 3 Sed rate 3 Sed rate 4 Sed r	STU/ STU/ STU/ STU/ STU/ STU/ STU/ STU/	DESIGN ECOMPRESSO	ZSP. HT. TABLE 4 SP. HT. TABLE 4 UBTOTAL C DETU/PERSON X. L. WATTH-HR. 7/24 HRS YABLE UBTOTAL D WATA: CONDENSERS 30-4/2	X 24 X 25 X 24 X 27 X 24 X 27 X 26 X 3 X 3 X 3 X 3 X 3 X 3 X 3 X	T BTU/24 T BTU/24 T BTU/24 IENTAL B' U/24 HR BH C+0 CONVERT U/HR TO' ME CYCLE APPLY SAM U/HR TO' F, CORRI	HRS TU/24 HRS. TOTAL TO HOURLY TO HOURLY TAL WITH CORRECTIC FETY FACTOR AL WITH CCTION	3 53/ 98 (NOTE!) 4 620 / 47 2 59 / 83 6 00 28 8 00 1 18 3 20 1 18 3 20
COOCHINE COO	LBS/MR. LBS/MR	STU/ STU/ STU/ STU/ STU/ STU/ STU/ STU/	DESIGN ECOMPRESSON	ZSP. HT. TABLE 4 SP. HT. TABLE 4 UBTOTAL C DETU/PERSON X. L. WATTH-HR. 7/24 HRS YABLE UBTOTAL D WATA: CONDENSERS 30-4/2	PRODUC PRODUC A/DAY, ABLE 6 B/BQ, FT, X	T BTU/24 T BTU/24 T BTU/24 IENTAL B' U/24 HR BH C+0 CONVERT U/HR TO' ME CYCLE APPLY SAM U/HR TO' F, CORRI	HRS TU/24 HRS. TOTAL TO HOURLY FACTOR CETY FACTOR CETY FACTOR COTONS OF F	3 53/ 98 (NOTE!) 46 60 /47 2 59 /33 6 00 28 8 00 1 18 3 20 1

VI. DISTRIBUTION CENTERS:

The refrigeration load in a food distribution facility differs substantially from that common to holding rooms utilized for the extended (or, long term) storage of seasonal and process foods. Product movement, and the activity level in general, is high, with the result being significantly increased infiltration and supplemental heat gains.

The produce cooler depicted in the example is illustrative of the application in general. Rooms of this type are maintained at 32-35°F with high humidity, and open into a staging or loading area most frequently controlled at 50-55°F. There is a significant infiltration heat gain resulting from the high frequency of product movement (it is not uncommon for the entrance doors to be open 50% or more of the time). Vestibule and air doors, or strip curtains, appreciably reduce this load, but are often not employed. Consequently, the infiltration load can approach 2 to 2.5 tons per door. An additional characteristic of this type room is the significant product load resulting from reaction heat; this load may usually be estimated at .003 to .004 tons/sq ft, and the room load overall will generally fall between 150 and 200 sq ft/ton. Proper equipment application dictates unit coolers selected for a 6-9°F coil T.D., with face velocities not in excess of 600 FPM for wet coil operation, or 700 FPM for light frosted operation. The over-riding design consideration in these rooms is the prevention of product damage from shrinkage, drying, or mold growth.

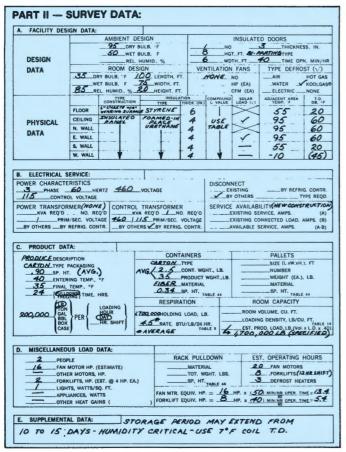
Deli coolers are generally maintained at a slightly lower temperature (30-33°F), and represent an even more severe

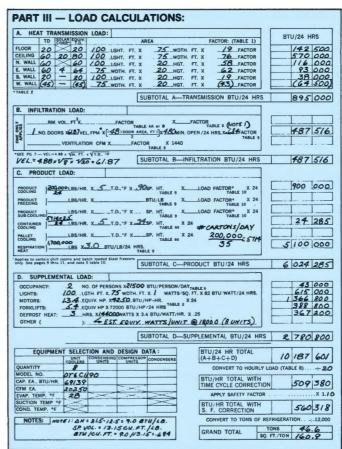
application from the standpoint of infiltration. In many rooms, the doors are never closed, with the resulting infiltration gain being 3.5 to 4 tons/door. The overall room load usually approximates 200 to 225 sq ft/ton.

The load in **holding freezers** is dependent in large measure on the condition of the inbound product. Frequently, a 10 to 15°F pulldown load is imposed, and, since movement is heavy, this load is significant. Infiltration can be estimated at 2 tons/door. A load estimating guideline of 200 to 300 sq ft/ton applies due to the wide variance in product load.

The refrigeration requirements for **loading docks** are difficult to estimate. The activity level is high (personnel, forklifts, etc.), as is the rate of infiltration. Dock seals may be either worn or damaged, or not adaptable to certain trailer cavities. Forced ventilation is sometimes utilized to evacuate exhaust fumes, and, when present, will supplant the usual infiltration load (if greater). Docks are maintained at 35 to 55°F, with the lower temperatures affording the dual advantage of increased flexibility and decreased load imposition on adjacent rooms. Unit coolers should have face velocities under 650 FPM, and be placed such that they blow toward and above the doors to create an air curtain effect. The load range is **150 to 175 sq ft/ton.**

Ripening rooms are usually located at the rear of the loading area, and may be of ½, 1 or 2 car capacity. The load range is 3 to 12 tons per room, and is accommodated most effectively with individual halocarbon systems specifically designed for this application. Since the full complement of rooms are seldom (if ever) in simultaneous service, a load diversity factor of .75 can be applied if a central refrigeration plant is utilized.





VII. WALK-IN COOLERS:

40

Pre-fabricated walk-in coolers and freezers are utilized for a wide variety of refrigerated storage, chilling and freezing applications, the most common of which is the point-of-sale holding room.

Since standard configurations with an extensive experience factor are involved, loads may be precalculated and charted as a matter of convenience.

A brief description of the precalculated walk-in cooler data included herein is as follows:

TABLE NO. DESCRIPTION

- Tabulates transmission, infiltration, lighting, occupancy and related miscellaneous loads for 8' and 10' prefabricated coolers in the 40 most common configurations. Note that product load is excluded for the purpose of enabling greater applicational flexibility. Loads are based on:
 - 95°F ambient design
 - Average usage
 - Indoor installation
 - 3" urethane (or equivalent) insulation
 - 18 hour compressor operation

Correction factors are noted for other ambients, and for light or heavy usage situations.

- 41 Tabulates average product loads by room volume. Data is based on actual Hussmann experience with field applications, and is intended for use with holding rooms only when the specific product loading is unknown.
- Tabulates specific product loads on the basis 42 of 24 hour pulldown with 18 hour operation. This table should be used for all pulldown coolers and freezers, or when the specific product entering rate and condition is known. Note: batch blast freezing, and certain other specialized applications such as ice cream hardening, require adjustment of the 24 hr pulldown data. The applicable formula is:

$$Q_{Btu/24 \, hrs} = \frac{Charted \, Value \times 24}{Pulldown \, or \, Freezing \, Time_{hrs}}$$

43 Tabulates additional infiltration loads for glass display doors.

Additionally. Table 32 tabulates the total capacity reguirements for walk-in beer storage coolers.

Product loads not tabulated in Table 42, or loads for specialized applications, may be estimated in the usual manner utilizing Form LE-1.

SPECIFIC EXAMPLES:

- I. Cooler Average Product Load:
 - 10'W × 12'L × 8'H@36°F
 - 95°F ambient design
 - · Refrig. load less product Average product load (Table 41) 1,800 Btu/hr

- II. Milk Cooler Specific Product Load:
 - 10'W × 12'L × 8'H@35°F
 - 300 gal/day entering @ 45°F
 - 10 hour pulldown
 - 80°F ambient design (air cond. space)
 - (3) 30" × 66" glass display doors

• Refrig. load less product (Table 40) 7125 × 0.75 (C.F. @ 80°F) 5,444 Btu/hr

Product load (Table 42)

456 Btu/hr /100 gal $\times \frac{300}{100} \times \frac{24}{10} \dots 3,283$ Btu/hr

Display door infiltration (Table 43)

960 × 3 2,880 Btu/hr Total refrig. load 11,607 Btu/hr

III. Holding/Pulldown Freezer:

- 16'W × 32'L × 10'H@ 20°F
- 2000 lbs fish/day entering @ 35°F
- 100°F ambient design
- Product packaged & boxed
- 16 hour pulldown
- Refrig. load less product (Table 40)

26,600 Btu/hr × 1.10 (C.F. @ 100°F)......29,260 Btu/hr

• Product load (Table 42)

817 Btu/hr/100 lbs $\times \frac{2000}{100} \times \frac{24}{16} \dots 24,510$ Btu/hr

Total refrig. load 53,770 Btu/hr

IV. Ice Cream Hardening/Storage Freezer:

- 30'W × 30'L × 10'H@ 20°F
- Soft mix @ 28°F
- Assume maximum daily capacity
- 100% overrun; wgt/gal = 4.6 lbs
- 95°F ambient design
- Refrig. load less product

Assuming 3.3 gal/sq ft (see Table 7, Note 7), the no. of gal to be hardened is:

 $900 \text{ sq ft} \times 3.3 \text{ gal/sq ft} = 2970 \text{ gal,}$

and the product load based on a 10 hr hardening time is therefore:

3284 Btu/hr/100 gal × 2970/100 ×

24/10......234,083 Btu/hr Total refrig. load 271,083 Btu/hr

V. Beer Cooler:

- 12'W × 20'L × 10'H@35°F
- 900 case capacity with 20% daily turn
- Product entering temp. of 50°F
- 95°F ambient design
- · Refrig. load less product assuming heavy usage (Table 40)

 $11,100 \times 1.15$

(C.F. @ heavy usage)........12,765 Btu/hr

Product load (Table 42)

2670 Btu/hr/100 Cases ×

900 5 × 100

Total refrig. load 17,571 Btu/hr

TAE	BLE 1	Α		HEAT GAI	N FACTOR	S IN BTU/	SQ FT /24	HRS FOR	соммо	N
					DIFFERENC		BIENT LESS	STORAGE	TEMPERATU	JRE)
	K Factor	Inches	1 10 20	30 35 40	45 50 55	60 65 70	75 80 85	90 95 100	105 110 115	120 125 130
SLASS	20	3 4 5 6 7	3.85 39 77 2.28 23 46 1.82 18 36 1.52 15 30 1.30 13 26	116 135 154 68 80 92 55 64 72 46 53 61 39 46 52	173 193 212 103 114 125 82 91 100 68 76 84 59 65 72	232 250 270 136 148 160 110 118 128 92 99 106 78 85 92	288 308 327 171 184 194 137 144 155 114 122 129 98 104 110	206 217 228 164 173 182 136 144 152 118 124 130	239 250 262 191 200 209 160 168 175 137 144 150	272 285 296 220 228 236 184 190 198 156 163 170
FOAMGLASS	.38	8 9 10 11 12	1.14 11 23 1.01 10 20 0.91 9 18 0.83 8 17 0.76 7.6 15	34 40 46 30 35 40 27 32 36 25 29 34 23 27 30	51 57 63 45 50 55 41 46 50 37 42 46 34 38 42	68 74 80 61 65 71 54 59 64 50 54 58 46 49 54	86 92 97 76 81 86 68 72 77 62 68 71 57 60 65	102 106 114 91 96 101 82 86 91 74 79 83 68 72 76	120 126 131 106 111 116 96 100 105 87 92 95 80 84 87	136 143 148 121 126 131 108 114 118 100 104 108 91 95 99
OARD	20	3 4 5 6 7	2.40 24 48 1.80 18 36 1.44 14 28 1.20 12 24 1.03 10 20	72 84 96 54 63 72 42 50 58 36 42 48 30 35 41	108 120 132 81 90 99 65 72 79 54 60 66 46 52 57	144 156 168 108 117 126 87 94 101 72 78 84 62 67 72	180 192 204 135 144 153 108 115 122 90 96 102 77 82 88	216 228 240 162 171 180 130 137 144 108 114 120 93 98 103	252 264 276 189 198 207 151 159 166 126 132 138 108 113 118	288 300 312 216 225 234 173 180 188 144 160 176 124 129 134
CORKBOARD	.30	8 9 10 11 12	0.90 9 18 0.80 8 16 0.72 7 14 0.66 6.5 13 0.60 6 12	27 32 36 24 28 32 21 25 29 19.5 23 26 18 21 24	41 45 50 36 40 44 32 36 40 30 33 36 27 30 33	54 59 63 48 52 56 43 47 50 40 43 46 36 39 42	68 72 77 60 64 68 54 58 61 50 53 56 45 48 51	81 86 90 72 76 80 65 68 72 60 63 66 54 57 60	95 99 104 84 88 92 76 79 83 69 73 76 63 66 69	108 113 118 96 100 104 86 90 94 79 82 86 72 75 78
NDED YRENE RGLASS	EXPANDED POLYSTYRENE OR FIBERGLASS	1 2 3 4 5	5.76 58 115 2.88 29 58 1.92 19 38 1.44 14 29 1.15 11 23	173 201 230 86 101 115 58 68 77 43 50 58 34 40 46	260 290 320 130 144 158 86 96 106 65 72 79 51 58 63	173 187 202 115 125 135 86 94 101 68 75 80	216 231 245 145 154 163 108 115 123 86 92 98	260 274 288 173 182 192 130 137 144 102 109 115	303 202 212 221 151 159 166 121 126 132	231 240 251 173 181 188 136 143 150
EXPAN POLYST OR FIBEI		6 7 8 9 10	0.96 9.6 19 0.84 8.4 17 0.72 7.2 14 0.64 6.4 13 0.58 5.8 12	29 34 38 25 29 34 22 25 29 19 22 26 17 20 24	43 48 53 38 42 46 32 36 39 29 32 35 26 29 32	58 62 68 50 55 59 43 46 50 38 42 44 34 38 40	72 77 82 63 68 72 54 57 61 48 52 54 44 48 49	87 91 96 76 80 84 65 69 72 58 61 64 52 55 58	101 106 111 88 92 97 76 80 83 67 70 74 61 64 67	115 120 125 101 105 109 86 90 93 76 80 84 69 73 75
EXTRUDED POLYSTYRENE	.185	1 2 3 4	4.44 44 89 2.22 22 44 1.48 15 30 1.11 11 22	133 155 178 67 78 89 44 52 60 34 39 45	200 222 244 100 111 122 67 74 81 50 56 61	266 289 311 133 145 156 89 96 104 67 73 78	333 167 177 189 111 118 126 84 89 95	200 211 222 133 141 148 100 106 111	233 244 255 155 163 170 117 122 128	266 278 289 178 185 192 133 139 145
EXTRI	.105	5 6 7 8	0.89 9 18 0.74 7.4 15 0.63 6.3 13 0.56 5.6 11	27 31 36 22 26 30 19 22 25 17 19 23	40 45 49 33 37 40 28 32 35 25 28 31	54 58 62 44 48 52 38 41 44 34 37 39	67 71 76 56 59 63 47 50 53 42 45 48	80 85 89 67 70 74 57 60 63 50 53 56	93 98 102 78 81 85 66 69 72 59 61 64	107 111 116 89 92 96 76 79 82 67 69 72
ANE- LACE ANELS	.16	1 2 3	3.84 38 77 1.92 19 38 1.28 13 26	115 134 154 58 67 77 38 45 51	173 192 211 87 96 106 58 64 71	230 250 268 115 124 135 77 83 90	288 307 326 144 154 163 96 102 109	173 183 192 115 122 128	202 212 221 135 141 147	231 240 249 154 160 167
SLAB URETHANE- FOAMED IN-PLACE URETHANE PANELS	.10	4 5 6	0.96 9.6 19 0.75 7.5 15 0.64 6.4 13	29 34 38 23 26 30 19 22 26	43 48 53 34 38 41 29 32 35	58 63 68 46 49 52 38 42 45	72 76 82 56 60 64 48 51 54	87 91 96 68 71 75 57 61 64	101 106 111 79 83 86 67 70 74	115 119 125 90 94 98 77 80 83
SLA! FOAN URET	.13	3 4 5	1.04 10 21 0.78 7.8 16 0.62 6.2 12	31 36 42 23 27 32 19 22 24	47 52 57 35 38 43 28 31 34	62 68 73 46 51 55 37 40 43	78 83 88 59 63 66 47 50 53	94 99 104 70 74 78 56 59 62	109 114 120 82 86 89 65 68 71	125 130 135 94 98 101 74 78 8
ING	Single Glass Double Glass Triple Glass	s	27 270 540 11 110 220 7 70 140	810 330 385 440 210 245 280	495 550 600 320 350 390	660 715 770 420 454 490	825 880 935 525 560 595	990 630 665 700	740 770 810	840 875 910
BUILDING MATERIALS	6" Conc. on Gr 8" Conc. ' & 4" Extrud. Styrene 8" Conc' & 6" E		4.8 48 96 1.08 11 22	144 32 38 43	49 54 59	65 70 76				
	8" Conc' & 6" Es Styrene or 4" Un 8" Conc' & 8" Expand. Styrene	ethane	0.96 9.6 19 0.71 7.1 14	28 33 38 21 25 28	43 48 53 32 36 39	57 62 67 43 46 50	53 57 60	64		

Note 1: 4" sub floor & 4" wearing surface enclosing intermediate insulation slab.

TA		EAT TR	ANSMISSIO ING AND BU		ENTS FOR (OTHER	
	MATERIAL	DENSITY LB/CU FT	MEAN TEMP °F	CONDUCTIVITY K	CONDUCTANCE C	RESISTANCE PER IN	R OVERALL
BUILDING	Asbestos-Cement Board Plaster Board, 1/2" Plywood Insulating Board, Sheathing, 1/2" Sound Deadening Board,1/2" Hardboard, Siding 7/16" Particleboard, Med. Dens.	120 50 34 22 15 40 50	75 75 75 75 75 — 75	4.0 — 0.80 — — — 0.94	2.25 - 0.82 0.74 1.49	0.25 - 1.25 - - - 1.06	- 0.45 - 1.22 1.35 0.67
BUILDING	Vapor, Permeable Felt Vapor, Seal, 2 Layers of Mopped 15 lb Felt Vapor, Seal, Plastic Film	_ _ _	75 75 75	-	16.70 8.35	 	0.06 0.12 Negl.
FLOORING	Carpet & Fiber Pad Carpet & Rubber Pad Cork Tile, 1/8" Terrazzo, 1" Tile, Asphalt Vinyl or Linoleum Wood Subfloor, 25/32" Wood Flooring	1111111	75 75 75 75 75 75		0.48 0.81 3.60 12.50 20.00 1.05 1.45	- - - - -	2.08 1.23 0.28 0.08 0.05 0.95 0.69
INSULATION	Blanket, Fiberglass Blanket, Mineral Wool Loose Fill, Perlite, Expanded Loose Fill, Glass Fiber Loose Fill, Vermiculite, Exp. Insulating Roof Deck, 2" Mineral Fiber Board, Accoustical Tile Roof Insulation, 2" (Note 1)	1.0 0.5 5.0-8.0 2.5 7.0-8.2 — 23	75 75 75 75 75 75 75	0.29 0.32 0.37 0.28 0.47	 0.18 0.19	3.45 3.12 2.70 3.46 2.12 — 2.38	5.56
MISC.	Sawdust Snow Soil Water		75 — — —	0.45 1.2-3.6 7.2-12.0 4.2	- - - -	2.22 0.83-0.27 0.14-0.08 0.24	- - - -
MASONRY	Brick, Common Brick, Face Concrete (Sand & Gravel) Concrete Block (Sand & Gravel — 8") Concrete Block, Cinder, 8" Concrete Block, Cinder, 12" Gypsum Plaster (Sand) Stone, Lime or Sand Tile, Hollow 2 Cell, 6"	120 130 140 — — — 105 —	75 75 - 75 75 75 75 75	5.0 9.0 12.0 — — — 5.6 12.50	 0.90 0.58 0.53 0.66	0.20 0.11 0.08 - - 0.18 0.08	- - 1.11 1.72 1.89 - - 1.52
ROOFING	Asphalt Roll Roofing Roofing, Built-Up, 3/8" Shingles, Asbestos Cement Shingles, Asphalt	70 70 120 70	75 75 75 75		6.5 3.0 4.76 2.27	- - - -	0.15 0.33 0.21 0.44
SIDING	Asphalt Insul. Siding, 1/2" Wood, Bevel, 1/2" × 8" Lapped Aluminum or Steel (Sheathed) Insulating-Board Backed, 3/8"	- - -	75 75 —	_ _ _	0.69 1.23 1.61 0.55		1.46 0.81 0.61 1.82
WOOD	Hardwoods (Maple, Oak) Softwoods (Fir, Pine) Softwoods (Fir, Pine), 3/4"	45 32 32	75 75 75	1.10 0.80 —	_ _ 1.06	0.91 1.25 —	 0.94

TA	TABLE 2 SOLAR RADIATION ALLOWANCE									
	SURFACE	°F TO BE ADDED TO NORMAL T.D. (NOTE 1)								
	TYPE		South Wall	West Wall	Flat Roof					
DARK	Slate Roofing Tar Roofing Black Paints	8	5	8	20					
MEDIUM	Unpainted Wood Brick Red Tile Dark Cement Red, Grey, or Green Paint	6	4	6	15					
LIGHT	White Stone Light Colored Cement White Paint	4	2	4	9					

Notes: 1. The F degrees noted are to be added to the normal
temperature difference to compensate for sun effect in
calculating transmission heat gain.

TABLE 3	MOTOR EQUIVALENCIES					
	BTU PE	RHORSEPOWER	-HOUR			
HORSE- POWER	Connected Load And Motor In Refrigerated Space (Note 1)	Connected Load Only In Refrigerated Space	Motor Only In Refrigerated Space			
1/8 to ½	4250	2545	1700			
3/4-3	3700	2545	1150			
5-20	2950	2545	400			

Note 1: Use for forced circulation unit coolers.

TABLE 4	TABLE 4A AVERAGE AIR CHANGES PER 24 HRS FOR MED. TEMPERATURE (ABOVE 32°F) ROOMS DUE TO INFILTRATION AND DOOR OPENINGS									
VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR			
200	44.0	1000	17.5	6000	6.5	30000	2.7			
300	34.5	1500	14.0	8000	5.5	40000	2.3			
400	29.5	2000	12.0	10000	4.9	50000	2.0			
500	26.0	3000	9.5	15000	3.9	75000	1.6			
600	23.0	4000	8.2	20000	3.5	100000	1.4			
800	20.0	5000	7.2	25000	3.0	200000	0.9			

Note: For heavy usage, multiply above values by 2. For long storage, multiply the above values by 0.60. Not valid if ventilating ducts or grilles are used.

TABLE 4	TABLE 4B AVERAGE AIR CHANGES PER 24 HRS FOR LOW TEMPERATURE (BELOW 32°F) ROOMS DUE TO INFILTRATION AND DOOR OPENINGS									
VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR	VOLUME CU FT	AIR CHANGES PER 24 HR			
250	29.0	1000	13.5	5000	5.6	25000	2.3			
300	26.2	1500	11.0	6000	5.0	30000	2.1			
400	22.5	2000	9.3	8000	4.3	40000	1.8			
500	20.0	2500	8.1	10000	3.8	50000	1.6			
600	18.0	3000	7.4	15000	3.0	75000	1.3			
800	15.3	4000	6.3	20000	2.6	100000	1.1			

Note: For heavy usage, multiply above values by 2. For long storage, multiply the above values by 0.6. Not valid if ventilating ducts or grilles are used.

Tables 2, 3, 4A & 4B from 1972 ASHRAE Handbook of Fundamentals — Reprinted by Permission

^{2.} Not to be used for air conditioning design.
3. Add 50% to charted values for buildings adjacent to highly reflective surfaces such as sun, water, or heat-repellent glass.

	TEMPERATURE OF OUTSIDE AIR, °F											
STORAGE ROOM TEMP. °F	8	5	9	90		15	100					
	RELATIVE HUMIDITY, PERCENT											
	50	60	50	60	50	60	50	60				
65 60 55 50	0.32 0.58 0.80 1.01	0.52 0.78 1.00 1.21	0.58 0.83 1.05 1.26	0.81 1.06 1.28 1.49	0.85 1.10 1.32 1.53	1.12 1.37 1.59 1.79	1.15 1.39 1.61 1.82	1.46 1.70 1.92 2.13				
45 40 35 30	1.20 1.37 1.54 1.78	1.40 1.57 1.74 2.01	1.45 1.62 1.78 2.05	1.68 1.85 2.01 2.31	1.71 1.88 2.04 2.33	1.98 2.15 2.31 2.64	2.00 2.17 2.33 2.65	2.31 2.48 2.64 3.00				
	1		TEM	IPERATURE C	FOUTSIDE AI	R, °F						
STORAGE ROOM TEMP.	4	10	50 90			10	100					
°F	RELATIVE HUMIDITY, PERCENT											
	70	80	70	80	50	60	50	60				
30 25 20 15 10	0.21 0.37 0.52 0.66 0.80	0.26 0.43 0.58 0.72 0.85	0.55 0.71 0.86 1.00 1.13	0.62 0.78 0.93 1.07 1.20	2.05 2.20 2.33 2.46 2.58	2.31 2.46 2.60 2.72 2.84	2.65 2.79 2.93 3.05 3.17	3.00 3.14 3.28 3.40 3.52				
5 0 - 5 - 10 - 15	0.92 1.04 1.15 1.26 1.37	0.97 1.09 1.20 1.31 1.42	1.25 1.36 1.47 1.58 1.69	1.32 1.43 1.55 1.65 1.76	2.69 2.80 2.90 3.00 3.10	2.95 3.06 3.16 3.26 3.36	3.28 3.38 3.48 3.58 3.68	3.63 3.74 3.84 3.93 4.03				
20 25 30	1.47 1.57 1.67	1.52 1.62 1.72	1.79 1.89 1.99	1.86 1.96 2.06	3.19 3.29 3.38	3.46 3.55 3.64	3.77 3.86 3.95	4.12 4.21 4.30				

From 1972 ASHRAE Handbook of Fundamentals — Reprinted by Permission

TABLE 6						
ROOM TEMPI °F	ERATURE	HEAT PER PERSON BTU/24 HRS				
50 40 30)	17,300 20,200 22,800				
20 10 0 - 10)	25,200 28,800 31,200 33,600				

Derived from 1972 ASHRAE Handbook of Fundamentals — Reprinted by Permission

TABLE 8 TIME	CYCLE FA	CTORS				
	RECOMMENDED FACTORS					
APPLICATION	24 HOUR (DIVIDE BY)	HOURLY (MULTIPLY BY				
Coil Temp. Above 32°F — No Frost Accumulation	24	1.0				
Light Frost With Positive Defrost Systems	22	1.1				
Med. Temp. With Positive Defrost Systems	20	1.2				
Low Temp. With Positive Defrost Systems	18	1.3				
Off Cycle Defrost, 35°F or Higher Storage Temp., With Evap. Temp. Below 32°F	16	1.5				

Note: Factors noted are for average frosting. For heavier frost, or lower than normal evap. temps., use 1-2 hrs less oper. time.

TABLE 7	CE CREAM DATA
PERCENT OF	HARDENING LOAD
OVERRUN	BTU/GAL ICE CREAM
60	532
70	500
80	470
90	447
100	425
110	405
120	386

Notes:

- 1. % overrun = $\frac{(wgt /gal \text{ of mix}) (wgt /gal \text{ ice cream})}{wgt /gal \text{ of ice cream}}$
- 2. Values based on entering temp of 25°F (30% frozen).
- 3. Formula: Product Load (Btuh) = $\frac{\text{no of gal } \times \text{Btu/gal}}{\text{hardening time (hrs.)}}$
- 4. 8-10 hr hardening time should be used with forced air circulation; adjust the calculated load for 18-20 hr compressor operation.
- See Table 42 for prefigured 24 hr hardening loads at 28°F ent. temp. & 18 hr comp. operation (the values charted in Table 42 must be adjusted for the desired hardening time — i.e., 8 or 10 hrs).
- 6. At 100% overrun, avg. wgt/gal is 4.6 lb with 60% water content.
- Estimate hardening rooms at a peak daily production rate of 3.3 gal/sq ft and for a storage capacity of 10 gal/sq ft, if sized to stock all flavors.
- 8. Estimate storage rooms @ 25 gal/sq ft when stacked solid 6 ft high (including aisles).

Extracted from 1971 ASHRAE Guide & Data Book - Reprinted by Permission

TABLE 9	TABLE 9 PROPERTIES AND STORAGE DATA FOR PERISHABLE PRODUCTS											
	SP. HEAT B		LATENT ²	HIGHEST			ORTSTORA			LONG ST		
PRODUCT	ABOVE FREEZE POINT	BELOW FREEZE POINT	HEAT OF FUSION BTU/LB	FREEZE POINT °F	WATER CONTENT %	TEMP °F	RH% MIN-MAX	RESPIRATION HEAT BTU/LB/24 HR	TEMP °F	RH% MIN-MAX	RESPIRATION HEAT BTU/LB/24 HR	APPROX. STORAGE LIFE
DAIRY PRODUCTS Butter Cheese	.64	.34	(Se	e Tables 2	1-28 for add	itional M	ilk / Cheese 75-80	Data)	-5 to -10	80-85		6 Mo
American Limburger Roquefort Swiss	.64 .70 .65 .64	.36 .40 .32 .36	79 86 79 79	17.0 19.0 3.0 15.0	55.0 60.0 55.0 55.0	40 ⁸ 40 ⁸ 45 ⁸ 40 ⁸	75-80 80-85 75-80 75-80		32 ⁸ 32 ⁸ 30 ⁸ 32 ⁸	75-80 80-85 75-80 75-80	- - -	12 Mo 2 Mo 2 Mo 2 Mo
Cream Eggs Crated Frozen Whole Solid	.85 .75 _ .22 .75	.40 .42 .42 .21	90 96 96 4 89	28.0 30.0 ⁴ 30.0 ⁴ - 28.0	55.0 66.0 — 3.0 61.0	35 40 ⁸ 40 ⁸ -15	80-85 - 80		-5 to -10 31° -5 to -10 40° -15	85-88 — 80	-	4 Mo 12 Mo 18 Mo 12 Mo 3-4 Mo
Milk Fluid Whole Condensed Evaporated Dried Oleo	.92 .42 .72 .22	.48 - - - - .25	125 40 106 4 22	31.0	88.0 28.0 74.0 3.0 15.5	35 40 - - 45	- - - - 60-70	1111	 40 Rm Temp 50 35	 80 60-70		5 Day: 3 Mo: 12 Mo: 3 Mo: 8 Mo:
FRUIT Apples Apricots Avocados Bananas • Green • Ripe	.87 .88 .81	.45 .46 .45 .42	121 122 118 108 108	29.3 30.1 31.5 30.6 30.6	84.1 85.4 82.0 74.8 74.8	35 ⁶ 35 50 ⁶	85-88 ⁸ 80-85 85-90 ⁸ 90-95	.72 .96 —	30 ⁶ 31 45 ⁶ —	85-88 ⁸ 80-85 85-90 ⁶ — 85-90	.48 .48 - -	3-8 Mc 2 Wks 3 Wks
Berries (Gen) Cherries Coconuts Cranberries Currants Dates (Cured)	.88 .86 .58 .90 .88	.45 .45 .34 .46 .45	120 116 67 124 120 29	30.0 28.8 30.4 30.4 30.2 3.7	84.0 80.4 46.9 87.4 84.7 20.0	35 35 35 40 36 35 ⁶	80-85 80-85 80-85 85-90 85-90 65-75	2.90 1.35 - .48 -	31 31 32 36 32 28 ⁶	80-85 80-85 80-85 85-90° 85-90 65-70	2.90 .75 - .48 -	8 Day 2 Wk 2 Mod 3 Mod 2 Wk
Dried fruit Figs (Fresh) Grapefruit Grapes (Calif) Lemons Limes	.42 .82 .91 .86 .91	.28 .43 .46 .44 .47 .45	39 112 126 116 127 118	27.6 30.0 28.1 29.4 29.7	28.0 78.0 88.8 81.6 89.3 82.9	35 40 45 35 55 ⁵ 45	50-60 65-75 85-90 80-90 85-90 ⁸ 85-90 ⁸	- .48 .48 1.44 1.44	32 32 32 31 55 45	50-60 65-75 85-90 ⁸ 85-90 ⁸ 85-90 ⁸ 85-90 ⁸		12 Mo 12 Day 6 Wks 5 Mo 3 Mo 8 Wks
Melons Olives (Fresh) Oranges Peaches Pears	.94 ³ .80 .90 .90	.48 ³ .42 .46 .46 .45	120 ³ 108 124 124 118	30.0 29.4 30.6 30.3 29.2	87.0 ³ 75.2 87.2 89.1 82.7	45 50 40 ⁶ 35 35 ⁶	85-90 85-90 85-90 80-85 90-95	1.68 - .72 .96 .72	40 45 32 ⁶ 32 30 ⁶	85-90 85-90 85-90° 80-85° 90-95°	.96 - .48 .48 .48	3 Wk 5 Wk 3-12 W 2-4 W 2-7 Mc
Pineapples • Green • Ripe Plums Prunes Quinces	.88 .88 .88 .88	.45 .45 .45 .45 .45	122 122 118 118 122	30.2 30.0 30.5 30.5 28.4	85.3 85.3 82.3 82.3 85.3	50 40 40 40 40 35	85-90 ⁸ 85-90 ⁸ 80-85 80-85 80-85	- 1.44 1.44 .72	- 31 31 31	80-85 ⁸ 80-85 ⁸ 80-85 ⁸	 .72 .72 .48	4 Wk 3 Wk 2-6 Wi 2-6 Wi 2-3 Mc
Raisins (Dried) Raspberries Strawberries Tangerines	.47 .84 .92 .90	.33 .44 .42 .46	45 122 129 125	30.0 30.6 30.1	80.6 89.9 87.3	45 31 31 40	85-90 85-90 85-90 85-90	2.40 1.80 1.63	40 - - 32	85-90 — — 85-90	- - - 1.14	3-6 Me 3 Day: 5-7 Day 2-4 Wi
MEAT Bacon (Cured) Beef	.43	.29	39	_	28.0	55	55-65	_	_	_	_	15 Day
 Dried Fresh Brined	 .77 	- .42 -	99 —	30.0 ³	70.0 —	34 ⁸ 40	85-90 80-85 ¹¹	_ _ _	55 32 ⁸ 32	65-70 85-90 80-85 ¹¹		6 Mo 3 Wk 6 Mo
Liver/Tongue Ham/Shoulder • Fresh	.77 .61	.44	102 80	- 30.0³	72.0 54.0	34 34 ⁸	85-90 85-88	_	32 28 ⁸	85-90 85-88	_	3 Wk
• Smoked Hides	.56	.33	64	_		55 —	55-65 —	_	55 34	55-65 55-70	1	6 Mos 3-5 Y

Footnote references above may be found at conclusion of Table on Page 26.

TABLE 9	PROPERTIES AND STORAGE DATA FOR PERISHABLE PRODUCTS											
IABLE 9	SP HEAT B				TORAC		ORT STORAG		SHAB	LE PRO		<u> </u>
PRODUCT	ABOVE	BELOW	HEAT OF	HIGHEST FREEZE	WATER	TEMP	RH%	RESPIRATION	TEMP	RH%	RESPIRATION	APPROX.
	FREEZE POINT	FREEZE POINT	FUSION BTU/LB	POINT	CONTENT %	°F	MIN-MAX	HEAT BTU/LB/24 HR	°F	MIN-MAX	HEAT BTU/LB/24 HR	STORAGE LIFE
Lamb ^a	.76	.45	100	28.0 ³	70.0	34	85-90	_	28	85-90	-	2 Wks
Lard Pork ^s	.53	.32	60	28.0³	0 42.0	45 34	75-80 85-90	_	32	75-80 —	_	6-8 Mos 15 Days
Sausage • Fresh	.87	.56	92	26.0 ³	65.0	35	85-90 ⁸			_	_	7 Days
Smoked	.83	.54	87	29.0 ³	61.0	40	80-85	_	32	70-75	_	6 Mos
Veal ^s Frozen Meats	.75	.40 .42³	98	28.0³	65.0	34	85-90 —	_	28 - 10	85-90 90-95	_	15 Days 9 Mos
POULTRY								V				
Chicken Game	.80 .80	.42 .42	106 114	27.0 ³ 27.0 ³	74.0 77.0	28 28	85-90 85-90	_	_	_	_	10 Days 10 Days
Goose Turkey	.58 .66	.35 .38	69 82	28.0	48.0 57.0	28 28	85-90	_	_	_	- 1	10 Days
Frozen Fowl	.00	.36 .40 ³	- 02	28.0 27.0 ³	57.0	- 5	85-90 85-90	_	- 10	85-90		10 Days 10 Mos
SEA FOOD Clams												
• In Shell	.84	.44	115	27.0	80.0	32	_	_	_	-	-	15 Days
Shucked Crabs	.90	.46	125	27.0	87.0	32	70-75	_	_	_	-	10 Days
(Boiled) Fish	.83	.44	115	_	80.0	25	80-90	-	-		-	10 Days
Fresh	.80³	.43³	110³	28.0 ³	80.0 ³	30	80-95 ⁸		_	-	_	15 Days
• Frozen • Smoked	.70	.43³ .39	92	_	_	5 45	_ 50-60	_	- 10 40	_ 50-60	_	8 Mos 6 Mos
Lobsters	.83	.44	113	_	79.0	25	80-90	_	-	30-00	-	10 Days
Oysters • In Shell	.84	.44	115	27.0	80.0	32	_	-	_		_	15 Days
• Shucked Shrimp/	.90	.46	125	27.0	87.0	32	70-75	_	_	_	_	10 Days
Scallops	.83	.45	119	28.0	75.0	32	70-75	_	_		_	7-10 Days
VEGETABLES Artichokes	.87	.45	120	29.9	83.7	40	90-95	7.24	31	90-95	5.07	1-2 Wks
Asparagus Beans	.94	.48	134	30.9	93.0	32	85-90	.84	32	85-90°	.84	3-4 Wks
Green	.91	.47	128	30.7	88.9	45	85-90	4.80	45	85-90°	4.80	7-10 Days
• Lima Beets	.73	.40	94	31.0	66.5	40	85-90	7.20	32	85-90 ⁸	4.80	1-2 Wks
Bunch	.90	.46	126	31.3	87.6	40	85-90	2.40	32	95 ⁸	1.44	10-14 Days
Topped Broccoli	.90 .92	.46 .47	126 130	30.1 30.9	87.6 89.9	40 40	85-90 90-95	2.40 2.40	32 32	85-90 90-95	1.44	3 Mos 9-12 Days
Brussel Sprouts Cabbage	.88 .94	.46 .47	130 132	30.9 30.4	89.9 92.4	40 35	90-95 90-95	2.40 2.40	32 32	90-95 ⁸ 90-95 ⁸	1.44 1.44	3-5 Wks 3-4 Mos
Carrots												
Bunch Topped	.86 .90	.46 .46	126 126	29.5 29.5	88.2 88.2	40 40	85-90 85-90	1.92 1.92	32 32	85-90 ⁸ 95	1.20 1.20	10-14 Days 4-5 Mos
Cauliflower Celery	.93 .95	.47 .48	132 135	30.6 31.1	91.7 93.7	35 35	85-90 85-90	2.40 2.40	32 32 32	85-90° 90-95°	1.44 1.44	2-4 Wks 3-4 Mos
Collards	.90	-	-	30.6	86.9	35	85-90	2.40	32	90-958	1.44	2 Wks
Corn (Fresh) Cucumbers	.82 .97	.42 .49	106 137	30.9 31.1	73.9 96.1	35 50	85-90 85-95	4.08 4.32	32 45	85-90° 85-95	0.96 2.40	4-8 Days 10-14 Days
Egg Plant	.94	.48	132	30.6	92.7	50	85-90	_	45	85-90	_	7 Days
Endive Garlic (Dry)	.94 .69	.48 .40	132 89	31.9 30.5	93.3 61.3	35 35	90-95 85-90	4.80	32 32	90-95° 65-70	3.60	2-3 Wks 6 Mos
Greens (Leafy) Kale	.90³	.46	126³	31.1 ³ 31.1	86.0 ³	35	90-95 90-95	2.40	32	90-95 90-95 ⁸	1.44	10-14 Days
Lettuce	.89 .96	.48	136	31.7	86.6 94.8	35 35	90-95	7.92	32 32	90-95 ⁸	6.00	10-14 Days 2-3 Wks
Leeks (Fresh) Mushrooms	.88 .93	.46 .47	126 130	30.7 30.4	85.4 91.1	35 32	90-95 90	.96 3.05	32	90-958	.48	2-3 Mos 3-4 Days
Mushroom (Grain Spann)	_	_	-	_	-	40	75-80	-	32	75-80	-	2 Wks
Okra	.92	.46	128	28.7	89.8	50	90-95	9.00	45	90-95	6.50	7-10 Days
Onions Parsley	.90 .88	.46 .45	124 122	30.6 30.0	87.5 85.1	50 35	70-75 90-95	.96 2.40	32 32 32	65-70 90-95	.48 1.44	4-8 Mos 1-2 Mos
Parsnips	.84	.44	112	30.4	78.6	35	90-95	1.68	32	90-95	1.20	4-5 Mos
Peas, Green Peppers	.79 .94	.42 .47	106 132	29.2 30.7	82.7 92.4	35 50	85-90 90-95	6.00 3.25	32 45	85-90 ⁸ 90-95	4.80 2.80	1-3 Wks 2-3 Wks
Potatoes • Irish	.85	.44	116	30.9	81.2	50	85-90	1.44	38	85-90 ⁸	.72	
• Sweet*	.83	.42	100	29.7	68.5	55°	85-90	2.40	55°	85-90 ⁸	2.40	4-6 Mos
Pumpkins Radishes	.92 .95	.47 .48	130 134	30.5 30.7	90.5 93.6	55 35	70-75 90-95	_	50 32	70-75 90-95	_	2-3 Mos 2-4 Mos
Rhúbarb Rutabagas	.96 .91	.48 .47	134 127	30.3 30.1	94.9 89.1	35 35	95 95	_	32 32 32	95 95	_	2-4 Wks 2-4 Mos
Sauerkraut	.92	.52	128	26.0	89.2	45	75-80	_	32	75-80	_	4-5 Mos
(In Kegs)												

TABLE 9	Р	ROPER	TIES A	AND S	TORAG	E DA	TA FOR	PERIS	HABL	E PROD	UCTS	
	SPHEATE	BTU/LB/°F1	LATENT ²	HIGHEST		SI	HORT STORA	AGE		LONG S	TORAGE	
PRODUCT	ABOVE FREEZE POINT	BELOW FREEZE POINT	HEAT OF FUSION BTU/LB	FREEZE POINT °F	WATER CONTENT %	TEMP °F	RH% MIN-MAX	RESPIRATION HEAT BTU/LB/24 HR	TEMP °F	RH% MIN-MAX	RESPIRATION HEAT BTU/LB/24 HR	APPROX. STORAGE LIFE
Spinach Squash	.94	.48	132	31.5	92.7	35	90-95 ⁸	4.80	32	90-95 ⁸	2.88	10-14 Days
Acorn Summer Winter Tomatoes	.92 .95 .91	.47 .48 .47	131 135 127	30.5 31.1 30.3	90.5 94.0 88.6	50 50 55	70-75 85-95 70-75	1 1 1	45 32 50	70-75 85-95 70-75		6-8 Wks 5-14 Days 4-6 Mos
 Green Ripe Turnips Vegetable Seed Vegetables (Mixed) 	.95 .94 .93 .29 .92³	.48 .48 .47 .23 .47³	134 134 130 16 130 ³	31.0 31.1 30.1 — 30.0 ³	93.0 94.1 91.5 12.0 ³ 92.0 ³	55 50 35 45 35	85-90 85-90* 90-95 55-65 90-95	3,12 .72 1,20 2,40 ³	55 32 32 32 32	85-90 90-95* 50-60 90-95	3.12 .96 1.60³	3-4 Wks 5-7 Days 4-5 Mos — —
MISCELLANEOUS Beer • Metal Keg • Wood Keg Bread Candy Chocolate (Coatings)	.92 .92 .74 .93	- .34 -	129 129 53 -	28.0 28.0 20.0 —	90.2 90.2 34.0³	40 40 0 34	85-9011 	1111	35 35 0 0	85-90 ¹¹ 40-50		3 Mos 3 Mos 3 Mos 6 Mos
Canned Foods				30.0				_		40-50		6 Mos
Cocoa	_	_	_	_		60 40	70 70		32 32	70 50	_	1 Yr 1 Yr
Coffee (Green)	.30	.24	20	_	15.0	37	80-85	_	35	80-85	- 4	3 Mos
Dried Foods Flour	.38	.28	_	_	14.0	70 82	40-50 60-65	_	32 78	40-50 60-65	_	1 Yr 6 Mos
Flowers			able 15 fo	r Data on (, Bulbs, and			00 03		O IVIOS
Frozen Pack Fruits & Vegetables	_	_	_	_	_	0	_	_	- 10	-	_	12 Mos
Furs &	_	_	_	_	_	40	45-55 ¹²	_	34	45-5512	_	Yrs
Fabrics Honey Hops	.35	.26 —	26 —		18.0 —	40 32	60-70 50-60	_	31 29	60-70 50-60	_	1 Yr 3 Mos
Maple Sugar Maple Syrup Nursery Stock	.24 .48	.21 .31	7 51	Ξ	5.0 35.5	45 45	65-70 65-70	_	31 31	65-70 65-70	_	4 Mos 4 Mos
Nuts				See Ta	ble 15 For V	arious V	arieties					
In Shells Shelled	.25 .30	.22 .24	8 ³ 10 ³	_	6.0 ³ 8.0 ³	40-45 40-45	65-75 65-75		28-32 28-32	65-75 65-75	_	10 Mos 8 Mos
Oil (Vegetable) Oleo Orange Juice (Chilled)	- .32 .91	.25 .47	22 128		0 15.5 89.0	70 45 35	75-80 		70 35 30	70-75 —	=	1 Yr 6 Mos 6 Wks
Popcorn (Unpopped)	.31	.24	19	_	13.5	40	85	-	32	85	_	-
Precooked Frozen Food	-	-	_	_	_	0	_	_	- 10	_	-	10 Mos
Seed (Vegetable) Serums/	.29	.23	16 —	_	12.0³ —	50 45	55-65 70	_	32 40	50-55 70	= 1	_
Vaccines Yeast (Compressed Bakers)	.77	.41	102	-	70.9	35	80-85	-	31	75-80	-	-

Notes: 1. Specific heats for products not listed may be estimated as follows: Specific heat above freezing = $0.20 + (0.008 \times \% \text{ water})$ Specific heat below freezing = $0.20 + (0.003 \times \% \text{ water})$

3. Average value.

4. Eggs with weak albumen freeze just below 30°F.

5. Lemons in terminal markets are customarily stored @ 50-55°F; sometimes, 32°F is used

7. Permissable storage period varies widely with variety. See USDA handbook #66.

8. Room design conditions critical.

11. High humidity required with wood kegs to prevent drying and resulting leaks.

12. Constant humidity desirable.

Latent heats of fusion for products not listed may be estimated as follows: Heat of fusion = % water × 143.4 Btu/lb

Optimum storage temperature varies widely with variety and/or section where grown. Recommended temperatures
for apples, as an example, range from 32°F (Golden Delicious) to 38°F (McIntosh). See USDA handbook #66.

Sweet potatoes must be cured for 10 to 14 days @ 85°F & 85-90% rh for successful storage.
 Relative humidity is left blank (—) in cases where the product is sealed from the air, or the rh % is otherwise non-critical.

TABLE 10			Р	RODUCT	CHILLING DATA	4			
	TEMP	ERATURE ³	CHILLING	GDATA		TEMPE	RATURE	CHILLING	DATA
PRODUCT	ENT. °F	FINAL °F	TIME, HRS	LOAD FACTOR	PRODUCT	ENT. °F	FINAL °F	TIME, HRS	LOAD FACTOR
DAIRY					Lamb	100	35	8	1.35
Eggs (crated)	45	30	10	1.20	Liver	90	35	18	1.44
Eggs (frozen)	40	0	24	1.50	Poultry	85	35	6	1.00
Ice Cream					Sausage	70	35	2	1.00
(5 gal cans)	28	- 10	10	1.38	Smoked	70	35	2	1.00
Milk (cartons)	45	35	10	1.20	(small cuts)	,,,	00	_	
FRUIT					Tongue	90	35	18	1.44
Apples	80	35	24	1.50	Weiners	70	35	2	1.00
Apricots	80	35	22	1.50	Veal	100	35	7	1.36
Avocados	80	46	22	1.50	VEGETABLES				
Berries	80	35	22	1.50		60	34	24	1.12
Grapes	70	34	20	1.27	Asparagus Beets ²	00	34	24	1.12
Grapefruit	75	35	22	1.45	(with tops)	70	34	24	1.26
Lemons	75	56	20	1.05	Broccoli	80	34	24	1.26
Limes	75	52	20	1.13	Brussel				
Oranges	75	33	22	1.45	Sprouts	80	34	24	1.26
Peaches	85	35	24	1.60	Cabbage	70	34	24	1.26
		35	24	1.25	Cantaloupes	80	45	24	1.10
Pears	70		3	1.50	Carrots ²				
Pineapples	85	42	20	1.50	(with tops)	70	34	24	1.26
Plums	80	35	20	1.20	Cauliflower	70	34	24	1.26
Prunes Quinces	80 80	35 33	20	1.50	Corn	70	34	24	1.26
	80	33	24	1.50	Cucumbers	70	50	24	1.00
MEAT					Onions	70	34	24	1.26
Bacon	105	28	24	1.00	Parsnips	70	34	24	1.26
Beef¹	100	35	18	1.40	Peas	78	34	22	1.45
(carcass)	100	35	24	1.50	String Beans	80	45	22	1.45
Ham	105	38	18	1.00	Tomatoes	80	55	40	1.00
Hogs¹	100	35	18	1.40	Turnips	70	34	24	1.26
(carcass)	100	35	24	1.50	Turnips	//	34	27	1.20

Notes: 1. See Tables 11 & 12 for data on typical beef and pork chilling rooms.

- 2. Load factor of beets or carrots withouts tops is 1.
- 3. Design room temperatures at the completion of the chilling process are generally 2°F below the final product temperature.
- The following factors apply to any blast freezing operation: batch freezing-1.5; continuous process (ie, conveyor fed) freezing-1.0.
- 5. Important: Utilization of load factors results in sufficient refrigeration capacity to accommodate the high initial rates of product heat evolution; room temperature rise is thereby minimized. It is to be noted, however, that the application of load factors necessitates a system design compatible with the diverse pulldown & holding requirements. These factors are not to be applied to: (1) small rooms, (2) rooms loaded over an extended period of time, & (3) rooms equipped with single rooftop halocarbon systems. In cases (1), (2) & (3) above, the chill period should be extended, and the room temperature allowed to rise. (See Page 9 for a more detailed discussion of this subject).

TABLE 11	TABLE 11 BEEF CHILLING • • MINIMUM REFRIGERATION REQUIREMENTS IN TONS ¹											
TOTAL ROOM	FLOOR AREA	18 HOUR C	HILL TIME ²	24 HOUR CHILL TIME								
CAPACITY - HEAD	SQ. FT.	4 HR LOADING	8 HR LOADING	4HR LOADING	8 HR LOADING							
75	650	23.2	18.2	17.9	15.6							
100	800	31.0	24.2	23.8	20.8							
250	2000	77.5	60.5	59.5	52.1							
450	3600	139.5	109.0	107.2	93.8							

Notes: 1. Refrigeration tonnages noted allow for normal room heat gain and defrosting, and are based upon a 65°F temperature pulldown of 550 lb cattle.

^{2.} An 18 hour chill time requires additional air circulation and lower than normal room temperatures (32-34°F).

TABLE 12	TABLE 12 PORK CHILLING • • MINIMUM REFRIGERATION REQUIREMENTS IN TONS											
TOTAL ROOM	FLOOR AREA	18 HOUR C	HILL TIME ²	24 HOUR CHILL TIME								
CAPACITY - HEAD	SQ FT	4 HR LOADING	8 HR LOADING	4 HR LOADING	8 HR LOADING							
75	200	7.9	6.3	6.2	5.5							
100	250	10.5	8.4	8.2	7.3							
250	625	26.2	20.9	20.6	18.3							
450	1125	47.2	37.8	37.0	33.0							

Notes: 1. Refrigeration tonnages noted allow for normal room heat gain and defrosting, and are based upon a 65°F temperature pulldown of 200 lb hogs.

^{2.} An 18 hour chill time requires additional air circulation and lower than normal room temperatures (32-34°F).

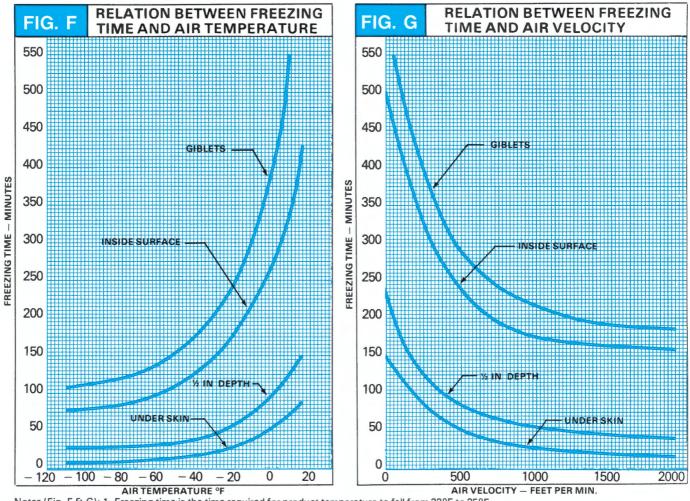
TABLE 13	ВІ	AST FREEZ	ING • • PR	ODUCT LO	AD ESTIMATES		
	SUPP	LYAIR	PRODUCT	TEMP., °F	HEAT REMOVED	ESTIMATED TIME	
PRODUCT	TEMP, °F	VELOCITY, FPM	ENTERING	LEAVING	BTU/LB	OF HEAT REMOVAL HOURS: MINUTES	
4 Oz. Hamburger Patties (unwrapped)	– 17	400	55	25	119	0:22	
2 Oz. Hamburger Patties (unwrapped)	- 18	400	40	16	112	0:13	
6 Lbs. Ground Beef In Plastic Wrapper (not lean)	- 20	1250	39	0	119	9:00	
1 Oz. Fresh Pork Sausage (unwrapped)	- 13	1000	41	15	101	0:20	
12 Oz. — 1¼ "Thick Strip Steak In Plastic Wrapper	- 20	1000	40	0	119	1:03	
1 Lb. — 6 Oz. Cooked Chop Suey In Plastic Container	- 21	800	64	0	147	2:13	
16 Lb. Fresh Turkey In Plastic Wrapper	- 24	2600	44	0	130	5:24	
12 — 1 Lb7 Oz. Containers Of Bar-B-Que Beef In Cardboard Box	- 21	1450	78	0	158	10:00	

Notes: 1. For a continuous loading operation such as a conveyor or systemized manual feed, the product load in Btu per 24 hrs equals:

 $\mathbf{QBtu/24\,hrs} = \mathbf{Btu/lb} \times \frac{\mathbf{Product\,per\,Shift\,lbs}}{\mathbf{Shift\,time\,hrs}} \times \mathbf{24} \; ; \; \text{this equation does not apply to "batch loading"}.$

 $^{2. \} The \ usual \ transmission, in filtration, lighting, motor \ and \ defrosting \ loads \ must be \ added \ to \ the \ product \ loads \ listed.$

^{3.} In continuous loading operations, the rate of product heat evolution has a negligible effect on the refrigeration load (it does, however, affect room sizing, conveyor size and speed, etc).



Notes (Fig. F & G): 1. Freezing time is the time required for product temperature to fall from 32°F to 25°F.

2. Fig. F based on 5-8 lb chickens with an initial temperature of 32-35°F, and an air velocity of 450-550 ft./min. 3. Fig. G based on 5-8 lb chickens with an initial temperature of 32-35°F, and an air temperature of -20°F

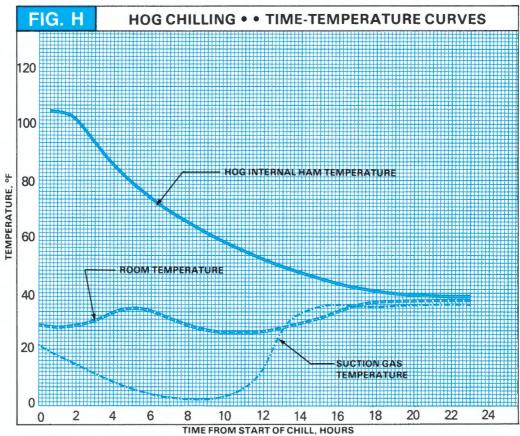


Fig. F, G & H from ASHRAE 1971 Applications Guide & Data Book — Reprinted by Permission

TABLE 14	FHISICAL	DATA OF PERISHABLE CONTAINER DATA		CONTA	INEKS	
			Ī	X. WEIGHTS -	LPC	LOADING
	TYPE	OUTSIDE DIMENSIONS ³ H×W×L—INCHES	PRODUCT	CONTAINER	TOTAL	LB/CUF
DAIRY PRODUCTS Cheese Cheese Cheese, Swiss Eggs, Shell Eggs, Frozen Milk, Condensed	Hoops Wood Box (Export) Wheels Wood Cases Cans Barrels	13 × 16 × 16 14 × 17 × 17 7 × 32 ½ × 32 ½ 13 × 26 × 12 12 ½ × 10 × 10 35 × 25 ½ × 25 ½ ee Table 23 for Data on Milk Cartons and Bottl	78 76 171 45 30 600	6.0 11.0 — 10.0 2.0 70.0	84.0 87.0 171.0 55.0 32.0 670.0	40.5 32.5 40.0 19.1 41.5 45.6
FROZEN FRUITS, JUICES & VEGETABLES Asparagus Beans (Green) Blueberries Broccoli Citrus Concentrates Peaches	24/12 oz Carton 36/10 oz Carton 24/12 oz Carton 24/12 oz Carton 48/6 oz Fiber Carton 24/1 lb Carton	8¼ × 13½ × 11¾ 8 × 12½ × 11 8 × 12 × 11½ 8½ × 12½ × 11½ 7½ × 13 × 8¾ 7½ × 13½ × 11¼	18 22.5 18 15 26 24	3.0 3.0 2.0 3.5 1.0 3.0	21.0 25.5 20.0 18.5 27.0 27.0	23.8 35.3 28.2 21.2 52.7 36.4
Peas Peas Spinach Strawberries Strawberries Strawberries	6/5 lb Carton 48/12 oz Carton 24/14 oz Carton 30 lb Can 24/1 lb Carton 450 lb Barrel	9½ × 17 × 11 12½ × 21½ × 8½ 8¼ × 12½ × 11 12½ × 10 × 10 8 × 13 × 11 35 × 25 × 25	30 36 21 30 24 450	2.0 2.0 3.0 2.0 4.0	32.0 38.0 24.0 32.0 28.0	28.2 27.2 31.0 41.5 36.2 35.5
FRUIT Apples Eastern Western General General General Apricots Avocados	Lug Box Wood Box Fiber Tray Carton Fiber Bulk Carton Tote Bin Box Box	11 % × 14 ½ × 18 % 12 % × 19 ½ × 11 13 % × 20 ½ × 12 ½ 13 × 19 × 12 ½ 2 ½ × 4 × 4 5 ½ × 13 × 17 ½ 4 ¼ × 14 × 17 ½	59 42 43 41 1000 22 13	5.0 8.0 3.8 3.8 3.8 150.0 3.0	64.0 50.0 46.8 44.8 1150.0 25.0 16.0	31.4 27.8 21.9 22.9 25.0 30.4 19.3
Berries (Gen.) Coconut (Shredded) Cranberries Dried Fruit • Dates • Raisins, Prunes, Figs	Crate (24 qt) Bags Fiber Carton Fiber Carton Fiber Carton	11% × 11% × 24 8 × 38 × 18½ 10½ × 15% × 11% 11 × 14 × 14 7 × 15 × 11	36 100 24 30 30	4.0 1.0 2.0 2.0 2.0	40.0 101.0 26.0 32.0 32.0	18.8 30.7 22.2 24.0 44.9
Figs (Fresh) Grapes • Eastern • Western Grapefruit Lemons Oranges • California	Box Wood Lug Box Wood Lug Box Box Box Box	2½ × 11½ × 17½ 7¼ × 14 × 17½ 6½ × 15 × 18 12¼ × 12 × 26 10¼ × 13½ × 27 12¼ × 12 × 26	6 28 28 68 72 76	2.0 3.5 3.0 7.0 6.0	8.0 31.5 31.0 75.0 78.0 82.0	20.6 27.3 29.2 30.4 32.9 34.0
Plorida California Ilorida Peaches Pears Plums & Prunes Quinces	Bruce Box Fiber Carton Fiber Carton Wood Lug Box Wood Box Crate Bushel	12% × 12% × 26 10% × 16% × 10% 8 × 19% × 12% 5% × 18% × 11% 8% × 18 × 11% 5% × 16% × 17% See Note 2	82 37 37 23 48 20 48	6.0 3.0 8.0 3.0 4.0 5.0 3.0	88.0 40.0 45.0 26.0 52.0 25.0 51.0	33.5 35.2 33.9 33.1 47.1 22.4 18.3
ICE CREAM ⁵ Can, Welded Can, Welded Can, Welded Pressboard, Waxed Pressboard, Waxed	Standard — 8 qt Standard — 10 qt Standard — 20 qt Tall — 1 qt Tall — 2 qt	6 % Diam. × 14 % 8% Diam. × 10 % 8% Diam. × 20 % 3 % Diam. × 7 % 4 % Diam. × 8 %	9.2 11.5 23.0 1.2 2.3	5.5 8.0 12.0 0.1 0.2	14.7 19.5 35.0 1.3 2.5	24.8 24.1 25.2 25.9 24.4
Pressboard, Waxed Pressboard, Waxed Pressboard, Waxed Pressboard, Waxed	Squat — 2 qt Squat — 4 qt Squat — 10 qt Squat — 20 qt	7 Diam. × 4 7 Diam. × 7 ¼ 9 ½ Diam. × 9 ½ 9 ½ Diam. × 19 ½	2.3 4.6 11.5 23.0	0.3 0.4 0.4 0.5	2.6 5.0 11.9 23.5	20.3 22.4 25.1 24.5
MEAT Beef • Boneless • Fores • Hinds Lamb, Boneless	Fiber Carton Loose Loose Fiber Box	6 × 28 × 18 — — 5 × 20 × 15	140 _ _ 53	6.0 - - 4.0	146.0 - 57.0	80.0 22.2 22.2 61.0
Pork Bellies Loins, Regular Loins, Boneless Veal, Boneless	Bundles Wood Box Fiber Box Fiber Carton	7 × 23 ½ × 10 ½ 10 × 28 × 10 5 × 20 × 15 5 × 20 × 15	57 54 52 53	 6.0 5.0 4.0	57.0 60.0 57.0 57.0	57.0 33.3 59.9 61.0

Notes: 1. Loading density for products packaged in bushel baskets, bushel hampers, or barrels is computed on the basis of actual warehouse cubage utilized.

^{2.} Approximate weights and dimensions of bushel baskets, and hampers are as follows:

4. Bushel Basket — Wgt: 2 lb; 14½ in top diam. × 11½ in bottom diam. × 10 in high

5. Bushel Basket — Wgt: 3 lb; 18 in top diam. × 14 in bottom diam. × 12 in high

6. Bushel Hamper — Wgt: 3 lb; 16 in top diam. × 10 in bottom diam. × 20 in high

6. 1½ Bushel Hamper — Wgt: 5 lb; 17 in top diam. × 12 in bottom diam. × 24 in high

TABLE 14	PHYSICAL	DATA OF PERISHABLE		CONTAI	INERS	1
		CONTAINER DAT	1		1.50	LOADING
	TYPE	OUTSIDE DIMENSIONS ³ H × W × L – INCHES		CONTAINER	TOTAL	LB/CU FT
POULTRY, FRESH Fryers (Whole: 24-30) Fryers (Parts)	Crate Crate	7 × 24 × 10 12½ × 17¾ × 10	60 50	5.0 4.0	65.0 54.0	25.4 38.9
POULTRY, FROZEN Ducks, 6 to Pkg. Fowl, 6 to Pkg. Fryers, Cut Up, 12 to Pkg. Roasters, 8 to Pkg.	Fiber Carton Fiber Carton Fiber Carton Fiber Carton	4 × 22 × 16 5 ½ × 20 ¾ × 18 4 ¼ × 17 ¼ × 15 ¾ 5 ½ × 20 ¾ × 18	31 31 28 30	1.5 2.5 2.5 2.5	22.5 33.5 30.5. 32.5	38.0 26.1 41.7 25.2
TURKEYS 3-6 lb, 6 to Pkg.	Fiber Carton	6½ × 21 × 17	27	3.0	30	20.1
6-10 lb, 6 to Pkg. 10-13 lb, 4 to Pkg. 13-16 lb, 4 to Pkg. 16-20 lb, 2 to Pkg. 20-24 lb, 2 to Pkg.	Fiber Carton Fiber Carton Fiber Carton Fiber Carton Fiber Carton	7 × 26 × 21 ½ 7 ½ × 26 ½ × 16 9 × 29 × 18 ½ 9 × 17 × 16 9 ½ × 19 × 16 ½	48 46 62 36 44	4.5 4.0 5.5 3.0 3.5	52.5 50.0 67.5 39.0 47.5	21.2 25.0 22.2 25.4 25.5
SEA FOOD — FROZEN Blocks Fillets	4/13 ½ lb Carton 4/16 ½ lb Carton 12/16 oz Carton 10/5 lb Carton 5/10 lb Carton	6% × 20% × 12% 11% × 19% × 10% 3 ½ × 12% × 8% 14 × 14% × 10 14 × 14% × 10	54 66 12 50 50	2.0 2.0 1.5 2.3 2.2	56.0 68.0 13.5 52.3 52.2	55.0 47.8 49.6 42.7 42.7
Fish Sticks Panned Fish Portions Round Ground Fish	12/8 oz Carton 24/8 oz Carton None (Glazed) 2, 3, 5 or 6 lb Cartons None (Glazed)	3 % × 11 × 8 ½ 4 % × 16 % × 8 % Wood Boxes Custom Packing Stacked Loose	6 12 	0.9 1.8 - -	6.9 13.8 - - -	29.3 32.9 35.0 29-33 33-35
Round Halibut Round Salmon Shrimp Steaks	None (Glazed) None (Glased) 2 ½ or 5 lb Cartons 1, 5 or 10 lb Packages	Wood Box, Loose Stacked Loose Stacked Loose Custom Packing Custom Packing			_ _ _ _	30-35 38.0 33-35 35.0 50-60
VEGETABLES Asparagus Beans Beets (Topped) Broccoli Cabbage Carrots (Topped)	Crate Bushel Bushel Crate Hamper (1 ½ bu) Bushel	11½ × 9½(top) × 12½(bot.) × 17½ See Note 2 See Note 2 13¾ × 19 × 24½ See Note 2 See Note 2	32 32 53 48 50 50	6.5 3.0 3.0 10.0 5.0 3.0	38.5 35.0 56.0 58.0 55.0 53.0	25.0 14.2 23.6 13.0 17.7 22.2
Cauliflower Celery Corn (Green) Cucumbers Lettuce (Head) Melons • General	Crate Crate Bushel Bushel Fiber Carton Crate	14 ½ × 16 × 25 ½ 9% × 20 % × 16 See Note 2 See Note 2 9 ½ × 20 ½ × 13 ½ 13 × 12 % × 23 ½	55 55 35 46 35	9.0 5.0 3.0 3.0 2.5	64.0 60.0 38.0 49.0 37.5	16.0 30.0 15.6 20.4 25.2 26.7
Cantaloupe Honeydew Onions (Dry) Onions Peas (Unshelled) Potatoes	Crate Crate Sack Bushel Bushel Bushel	5 %s × 14 % × 23 % 7 % × 16 % × 23 % — See Note 2 See Note 2 See Note 2	27 42 50 50 30 60	4.0 6.0 1.5 3.0 3.0 3.0	31.0 48.0 51.5 56.0 33.0 63.0	25.7 24.4 — 22.2 13.3 26.7
Sweet Potatoes Tomatoes • General • California • Florida • Texas	Bushel Fiber Box Lug Box Crate Lug Box	See Note 2 10 % × 19 × 10 % 7 % × 17 ½ × 14 11 1% × 18 % × 11 1% 6 % × 17 ½ × 14	55 40 30 60 30	3.0 4.0 4.0 4.0	58.0 43.0 34.0 64.0 34.0	24.4 31.0 27.3 38.7 31.9
MISCELLANEOUS Beverages* Lard (2/28 lb) Nuts • Almonds (In Shell) • Almonds (Shelled) • English Walnuts (In Shell)	Wood Box (Export) Sacks Cases Sacks	7% × 18 × 13% 33 × 24 × 15 6% × 23% × 11 31 × 25 × 11	56 90 28 100	8.0 1.5 4.0 3.0	64.0 91.5 32.0 103.0	52.5 13.1 27.7 20.3
English Walnuts (Shelled) Peanuts (Shelled) Pecans (In Shell) Pecans (Shelled) Pecans (In Shell)	Fiber Carton Burlap Bag Burlap Bag Fiber Carton Tote Box	10 × 14 × 14 35 × 10 × 15 35 × 22 × 12 11 × 13 × 13 60 × 42 × 42	25 125 125 30 1800	2.0 2.0 1.5 2.0 170.0	27.0 127.0 126.5 32.0 1970.0	22.0 38.6 23.4 27.9 29.4

Notes: 3. Tabulated figures are the true dimensional characteristics of the various containers when empty, and make no allowance for bulging tops or sides when filled.

^{4.} Weights of various products at point of sale holding facilities may vary substantially from the figures noted due to moisture loss during processing or storage.

^{5.} Ice cream assumed at 100% overrun and 4.6 lb/gal.6. Refer to Table 29 for beer and soda data.

	STORAGE	CONDITIONS	APPROXIMATE	METHOD OF	HIGHEST FREEZE
	TEMP., °F	REL. HUM., %	STORAGE LIFE	HOLDING	POINT, °F
CUT FLOWERS					
Calla lily	40	90-95	1 week	Dry pack	_
Camellia	45	90-95	3-6 days	Dry pack	30.6
Carnation	32-36	90-95	1 month	Dry pack	30.8
Chrysanthemum	32-35	90-95	3-6 weeks	Dry pack	30.5
Daffodil (Narcissus)	32-33	90-95	1-3 weeks	Dry pack	31.8
Dahlia	40	90-95	3-5 days	Dry pack	
Gardenia	32-33	90-95	2-3 weeks	Dry pack	31.0
Gladiolus	35-40	90-95	1 week	Dry pack	31.4
Iris, tight buds	31-32	90-95	2 weeks	Dry pack	30.6
Lily, Easter	32-35	90-95	2-3 weeks	Dry pack	31.1
Lily-of-the-Valley	31-32	90-95	2-3 weeks	Dry pack	_
Orchid	45-50	90-95	2 weeks	Water	31.4
Peony (tight buds)	32-35	90-95	2 weeks 4-6 weeks	Dry pack	30.1
Rose (tight buds)		10.00			
	32	90-95	1-2 weeks	Dry pack	31.2
Snapdragon	31-32	90-95	3-4 weeks	Dry pack	30.4
Sweet peas	31-32	90-95	2 weeks	Dry pack	30.4
Tulips	31-32	90-95	4-8 weeks	Dry pack	-
GREENS					
Asparagus (plumosus)	32-40	90-95	4-5 months	Polylined cases	26.0
Fern (dagger and wood)	30-32	90-95	4-5 months	Dry pack	28.9
Holly	32	90-95	4-5 weeks	Dry pack	27.0
Huckleberry	32	90-95	1-4 weeks	Dry pack	26.7
Laurel	32	90-95	1-4 weeks	Dry pack	27.6
Magnolia	35-40	90-95	1-4 weeks	Dry pack	27.0
Rhododendron	32	90-95	1-4 weeks	Dry pack	27.6
Salai	32	90-95	1-4 weeks	Dry pack	26.8
BULBS					
Amaryllis	38-45	70-75	5 months	Dry	30.8
Crocus	48-63	70-73	2-3 months	Diy	30.0
Dahlia	40-45	70-75	5 months	D	28.7
				Dry	
Gladiolus	38-50	70-75	8 months	Dry	28.2
Hyacinth	55-70	_	2-5 months	_	29.3
Iris, Dutch, Spanish	80-85	70-75	4 months	Dry	_
Lily					
Gloriosa	63	70-75	3-4 months	Poly liner	_
Candidum	31-33	70-75	1-6 months	Poly liner & peat	
• Croft	31-33	70-75	1-6 months	Poly liner & peat	_
					20.0
• Longiflorum	31-33	70-75	1-10 months	Poly liner & peat	28.9
Speciosum	31-33	70-75	1-6 months	Poly liner & peat	_
Peony	33-35	70-75	5 months	Dry	_
Tuberose	40-45	70-75	4 months	Dry	_
Tulip	31-32	70-75	5-6 months	Dry	27.6
NURSERY STOCK					
Trees and Shrubs	32-36	80-85	4-5 months		
	32-36	85-95	4-5 months	Baro rented	_
Rose Bushes	32	85-95	4-5 months	Bare rooted	_
Strawberry Plants	30-32	80-85	8-10 months	with poly liner Bare rooted	29.9
				with poly liner	20.0
Rooted Cuttings	33-40	85-95	_	Poly wrap	_
Herbaceous Perennials	27-28 or	80-85	_		-
	33-35				
	22-32	80-85	6-7 weeks		

Note: Refer to USDA Handbook No. 66 for additional data relating to flower and nursery stock storage.

TABLE 16	APPLE ST	ORAGE C	APACITY	REQUIRE	MENTS (@ 35°F							
ENTERING FRUIT	MAXIMUM (NOTE 3)	BTU PER 24 HR PER BOX (NOTES 1, 5 & 8)											
TEMPERATURE, °F	RESPIRATION	PERCENTAGE LOADED ON LAST DAY											
TENN ENATORE, T	BTU/LB/24 HRS	5	10	15	20	25	30						
100	9.0	164.6	298.6	432.8	576.9	701.1	835.3						
95	7.5	154.0	277.7	401.4	525.1	648.9	772.6						
90	6.5	143.5	256.8	370.1	483.4	596.6	709.9						
85	5.5	133.1	235.9	338.7	441.6	544.4	647.2						
80	4.9	122.6	215.0	307.4	399.8	492.2	584.6						
75	4.4	112.2	194.1	276.1	358.0	439.9	445.3						
70	3.8	101.7	173.3	244.7	316.2	387.7	459.2						
65	3.3	91.4	152.6	213.8	275.0	336.1	397.3						
60	2.6	81.0	131.7	182.4	233.2	283.9	334.6						
55	2.0	70.5	110.8	151.1	191.4	231.6	271.9						
50	1.5	60.1	89.9	119.7	149.6	179.4	209.2						
45	1.1	49.6	69.0	88.4	107.8	127.1	146.6						
40	0.8	39.2	48.1	57.0	65.0	74.9	83.9						

Notes: 1. The Btu's noted per box represent product load only. The usual transmission, infiltration, and miscellaneous loads must be added.

- 2. One box equals one bushel: gross weight 50 lbs; net weight 42 lbs.
- 3. Respiration heat at 35°F: 0.72 Btu/lb/24 hrs; at 30°F: 0.48 Btu/lb/24 hrs.
- 4. Sp. heats: apples: 0.88 Btu/lb/°F; boxes: 0.60 Btu/lb/°F; weighted average: 0.835 Btu/lb/°F.
- 5. Loads will be less under C. A. storage conditions.
- 6. See Table 10 and Text, Page 9, for applications involving chilling only.
- 7. Example: 10000 box storage with ent. temp. of 95° F and last day loading of 15 percent: Product Load = $10000 \times 401.4 = 4,014,000$ Btu/24 hrs.
- 8. Apply a 0.95 factor to charted loads if containers are 3.75 lb cardboard cartons in lieu of 8 lb wood boxes.
- 9. Hydrocoolers generally pre-cool the fruit to 40°F or 45°F.

TABLE 17	RECOMMEN	DED COILT	BY PRODUC	CT CLASS						
COILTYPE	TEMPERATURE DIFFERENTIAL - °F									
	CLASS 1	CLASS 2	CLASS 3	CLASS 4						
FORCED AIR GRAVITY	6 to 9 12 to 16	9 to 12 14 to 18	12-20 16-22	20-25 20-25						

- Class 1 Includes products which require very high relative humidities in order to minimize moisture loss during storage. Examples of this category include unpackaged cheese or butter, eggs, and most vegetables if held for comparatively long periods.
- Class 2 Includes products which require reasonably high relative humidities (but not as high as those included in Class 1). Examples of this category include fruits & cut meats in retail storage¹.
- Class 3 Includes products which require only moderate relative humidities, and includes such products as mushrooms, carcass meats, hides, smoked fish, and fruits such as melons having tough skins.
- Class 4 Includes products which are either unaffected by humidity, or which require specialized storage conditions in which the maximum relative humidity is limited thru use of a reheat system. Examples of the first group are furs, woolens, milk, beer (steel or aluminum kegs), bottled beverages, canned goods & similar products having a protective coating; nuts and chocolates are good examples of the second group.

Note 1: Some supermarket fixtures for cut meat display are designed to operate with lower TD's.

TABLE	E 18	(COMMERCI	AL ESTIM	ATING GU	IDELINES ¹
AF	PPLICATION	TEMP, °F	CEILING HEIGHT, FT	COIL TD, °F	SQ FT /TON	COMMENTS
NTER	Storage Cooler	28-40	16-24	Dry Room 9-15 Wet Room 6-9	150-250	Maximum face velocity for light frosted application is 700 fpm; for wet coil operation, face velocity should not exceed 600 fpm; centrifugal or propeller fans are applicable.
ON CE	Storage	- 10	16-24	10-15	200-300 7000-10000	Maximum fin spacing of 3-4 fpi; propeller fan units with high face yelocities and long air throw are
5	Freezer	-10	24-40	10-13	cu ft/Ton	normally used.
DISTRIBUTION CENTER	Loading 40-55 Dock		16-20	10-12	150-175	Low face velocity units (under 650 fpm) are required. Units should blow toward and above the doors to create an air curtain effect. Between-the-rail units are ideal for narrow docks.
MEAT CHILL COOLER	Hogs²	28-34	16-20	10-12	25-40 10-16 hd/ton	Coil face velocity should not exceed 750 fpm. Between-the-rail units are
M H O O	Beef ³	20-34	10-20	10-12	30-45 3-5 hd/ton	specifically designed for this application and should be used whenever possible.
	Work Rooms Cutting & Grinding Rooms		10-12	15-25	125-175	Units with low noise level which distribute air with low velocity or in an umbrella pattern optimize worker comfort.

Notes: 1. Above guidelines are for budgeting purposes only, and should not be used as the sole design criteria.

- 2. Hog chill rooms average 2-2.5 sq ft per head.
- 3. Beef chill rooms average 6-8 sq ft per head.

TABLE 19		BANAN	A ROOM	DESIGI	N PARA	METERS		
ROOM	NO OF	WEIGH	IT, LBS	EVAPO	DRATOR	REFRIGERATION4.5	HEATING	
SIZE	BOXES	GROSS	NET	T.D.	CFM	LOAD-BTU/HR	LOAD-KW	
½ Car	432	20304	18144	15	6000	36,000	4	
1 Car	864	40608	36288	15	12000	72,000	8	

Notes: 1. Evaporator fan should have ½ "ext. static pressure capability.

- 2. Weights per box: gross-47 lb; net-42 lb.
- 3. Specific heats: bananas-0.8 Btu/lb/°F; cartons-0.4 Btu/lb/°F.
- 4. To calculate load, assume pulldown of 1°F per hour, and peak respiration of 12 Btu/lb/24 hr.
- 5. Tabulated loads represent total heat removal.
- 6. Heat is required only to warm a cold load and may not be required.

TABL	E 20		U VALUE REVISIONS									
SECT PROPE	TION	REVISED U VALUE AT ADDITIONAL RESISTANCE OF										
U	R	4	6	8	12	16	20	24				
1.00	1.00	0.20	0.14	0.11	0.08	0.06	0.05	0.04				
0.90	1.11	0.20	0.14	0.11	0.08	0.06	0.05	0.04				
0.80	1.25	0.19	0.14	0.11	0.08	0.06	0.05	0.04				
0.70	1.43	0.19	0.13	0.11	0.07	0.06	0.05	0.04				
0.60	1.67	0.19	0.13	0.10	0.07	0.06	0.05	0.04				
0.50	2.00	0.18	0.13	0.10	0.07	0.06	0.05	0.04				
0.40	2.50	0.16	0.12	0.10	0.07	0.05	0.05	0.04				
0.30	3.33	0.14	0.11	0.09	0.07	0.05	0.04	0.04				
0.20	5.00	0.11	0.09	0.08	0.06	0.05	0.04	0.03				
0.10	10.00	0.06	0.06	0.06	0.05	0.04	0.04	0.03				
0.08	12.50	0.06	0.06	0.05	0.04	0.04	0.03	0.03				

Example: Given an existing structure with a U value of 0.50, determine the revised U following the addition of insulation having a resistance of 12: enter Column 1 at 0.50 and move horrizontally to the column headed by 12; the revised U value may then be read at 0.07.

TAI	BLE 21	FC	OOD STOP	RAGE EST	FIMATING	GUIDELIN	IES			
		AVER	AGE HEAT CON	TENT		RECOMMENDED STORAGE CONDITIONS				
	PRODUCT	SP HT	SP HT	LATENT	HIGHEST	TEMPERA	RELATIVE			
	CATEGORY	ABOVE FREEZING	BELOW FREEZING	HEAT BTU/LB	FREEZING POINT, °F	SHORT TERM				
	Butter	.64	.34	15	30	40	-5	80-85		
DAIRY	Cheese, Cream, Eggs, Milk	.85	.40	100	31	35-40	33-35	70-85		
	Bananas (Ripe)	.80	.42	108	30.6	56	56	85-90		
	Dried Figs/Raisins	.41	.29	36	- 4	40-50	40	60		
FRUIT	Avocados	.76	.41	101	30	50-55	45-50	85-90		
E	Citrus	00	40	400	00	50-55	32	85-90		
	Apples/Apricots/Pears	.90	.46	123	30	35	30-38	85-90³		
	Bacon (Cured)	.43	.29	39	27	55	34-40	55-65		
MEAT	Fresh Game	.80	.42	114	27	34	28	85-90		
Σ	Beef, Ham, Lamb, Pork Sausage, Veal	.76	.40	95	29	34	28-32	85-90		
٨	Chicken	.79	.42	106	20	34	00	05.00		
FOWL	Turkey	.63	.36	78	30	34	28	85-90		
FOOD	Boiled Lobsters or Crabs	.84	.44	14	_	25	-	85-90		
w E	All Other (Fresh)	.84	.44	14	28	32	-	85-95		
VEGETABLES	Beans (Green), Cucumbers, Eggplant, Garlic (Dry), Melons, Okra, Onions (Dry), Peppers, Potatoes, Pumpkins, Squash (Hard Shell), Sweet Potatoes, Tomatoes (Ripe)	.94	.47	136	31	50	50	80		
	Most Other	.94	.47	136	31	35	31-32	90-95		

Notes: 1. Values are averages by product group, and may be used for estimating rooms in which the exact product loading is unknown.

^{3.} Pears require a relative humidity of 92-95%.

TABLE 22		RECOMMENDED INSULATION THICKNESS											_					
	TEMPE						RATURE DIFFERENCE (ROOM LESS AMBIENT), °F											
INSULATION TYPE AND 'K' VALUE		COOLER								HOLD	NG FF	REEZER	3			SHAR	PFRE	EZER
		50	55	60	65	70	75	80	85	90	95	100	105	110	115	120	125	130
Foamglass	.38	3	4	5	6	6	7	8	8	9	9	9	10	11	11	12	12	12
Corkboard	.30	3	4	4	4	5	5	5	6	6	7	7	8	9	9	10	10	10
Expanded Polystyrene	.24	2	3	3	3	4	4	4	5	5	6	6	6	7	7	8	8	8
Fiberglass	.24	2	3	3	3	4	4	4	5	5	6	6	6	7	7	8	8	8
Extruded Polystyrene	.185	2	3	3	4	4	5	5	5	6	6	6	6	6	6	7	7	7
Slab Urethane	.16	2	3	3	3	3	3	4	4	4	4	5	5	5	6	6	6	6
Foamed-In- Place Urethane	.13	2	2	2	3	3	3	3	3	42	42	42	42	42	4	5	5	5

Notes: 1. Thicknesses shown are for general guidance only. Requirements for a given installation will vary in accordance with operating versus first cost projections.

^{2.} Refer to Table 9 for specific properties and storage requirements of individual products.

^{2. 3} inch foamed-in-place urethane is adequate for short term walk-in freezer applications.

TABLE 23				MIL	к со	NTAINE	R DA	TA			
•	CAP	CAPACITY DIMENSIONS, IN.			CONTAINER DATA			BOTTLES	LIQUID	BTU REQ'D	
TYPE CONTAINER	oz	GAL	LENGTH	WIDTH OR MAX. DIAM.	HEIGHT	WEIGHT LBS	SP. HT. B/LB/°F	MATERIAL	CARTONS PER CASE	WEIGHT LBS	TO COOL 1°F WHEN FULL
Carton Quart Half Gallon Gallon	32 64 —	- - 1		2.81 3.81 5.56	9.00 9.375 9.50	0.075 0.142 0.245	0.50 0.50 0.50	Paper Paper Paper	-	2.15 4.30 8.60	2.06 4.11 8.20
Bottle Half Pint Pint Quart	8 16 32	_		2.375 3.00 4.00	5.375 7.75 9.75	0.500 0.810 2.000	0.20 0.20 0.20	Glass Glass Glass	_	0.537 1.075 2.15	0.61 1.18 2.42
Cases³ Quart Cartons Half Gal Cartons Gallon Cartons	- - -	_ _ _	13.0 13.0 13.0	13.00 13.00 13.00	11.00 11.00 11.00	7.0 7.0 7.0	0.12 0.12 0.12	Steel Steel Steel	16 9 4	34.40 38.70 34.40	33.80 37.92 33.80
Half Pint Bottles Pint Bottles Quart Bottles			18.5 18.5 18.5	14.50 14.50 14.50	6.75 8.50 10.50	11.0 14.0 16.0	0.60 0.60 0.60	Wood Wood Wood	30 20 12	16.11 21.50 25.80	24.90 32.00 38.70
Cans 5 Gallon 10 Gallon		5 10		10.50 13.00	19.50 25.00	15.0 26.0	0.12 0.12	Steel Steel	_	43.00 86.00	42.20 84.00

Notes: 1. Sp. Ht.: 0.94; weight per quart - 2.15 lbs ; weight per gallon - 8.60 lbs.

2. Storage areas may be estimated on the basis of 70 lb of milk in glass bottles or 100 lb of milk in paper quart cartons per sq ft, with 1/3 additional area being allowed for aisles. Cases are usually stacked 5 high.

Extracted in part from ASRE (now ASHRAE) Applications are also shown as the contraction of the basis of 70 lb of milk in glass bottles or 100 lb of milk in paper quart cartons per sq ft, with

3. Weights for cases empty (no bottles included).

Extracted in part from ASRE (now ASHRAE) Application Data Section. Some data obtained by actual weighing & measuring.

TABLE	24 CHEES	E MAKE	& CUR	E DATA
CHEESE	PART OF PROCESS	TEMP.	RELATIVE HUMIDITY %	TIME
Blue	Form Room Curing Room Holding Room	68-72 48-50 40-45	80-90 95 70	3-5 90 30-180
Cheddar	Curing Room	32-34 38-40 45-55 55-70	70 70 85-90 85-90	12-18(mos) 8-10(mos) 60 indeterminate
Swiss	Salting Room Cool Room Warm Room Curing Room Holding Room	50-54 40-45 68-77 60 35-40	In Brine 70 80-85 80-85 70	4-6 10-14 14 14-28 60-180

ABLE 26	THER CH	IEESE CURE	DATA			
CHEESE	CURE	RELATIVE	CURE			
	TEMP.	HUMIDITY	TIME			
	°F	%	DAYS			
Brick	60-65	90	60			
Limburger	60-65	95	42			
Camembert	53-59	90	21			
Cream Cottage Neufchatel	53-59 90 21 No Cure					

TABLE 25		SPECIFIC HEATS¹ OF MILK AND MILK DERIVATIVES TEMPERATURE, °F 32 59 104 140 0.978 0.976 0.974 0.972 0.940 0.943 0.952 0.963 0.920 0.938 0.930 0.918 0.750 0.923 0.899 0.900								
	TEMPERATURE, °F									
PRODUCT	32	59	104	140						
Whey Skim Milk Whole Milk 15% Cream 20% Cream	0.940 0.920	0.943 0.938	0.952 0.930	0.963 0.918						
30% Cream 45% Cream 60% Cream Butter Milk Fat	0.673 0.606 0.560 0.512 0.445	0.983 1.016 1.053 0.527 0.467	0.852 0.787 0.721 0.556 0.500	0.860 0.793 0.737 0.580 0.530						

Note 1: Sp. heat in Btu/lb/°F

TABLE 27 CHEE	SE FREEZE POINTS				
CHEESE	FREEZE POINT, °F				
Brick	16.3				
Cheddar	8.8				
Cottage	29.8				
Limburger	18.7				
Process American	16.6				
Process Swiss	17.5				
Roquefort	3.7				
Swiss, Domestic	14.0				
Swiss, Imported	14 7				

TABLE 2	.8 c	HEESE ST	TORAGE TEMP	ERATUR	ES
CHEESE	OPTIMUM STORAGE TEMP., °F	MAXIMUM STORAGE TEMP., °F	CHEESE	OPTIMUM STORAGE TEMP., °F	MAXIMUM STORAGE TEMP., °F
Brick	30-34	50	Process American	40-45	75
Camembert	30-34	50	Process Brick	40-45	75
Cheddar	30-34	60	Process Limburger	40-45	75
Cottage	32- 34	45	Process Swiss	40-45	75
Cream	32-34	45	Roquefort	30-34	50
Limburger	30-34	50	Swiss	30-34	60
Neufchatel	32-34	45	Cheese Foods	40-45	55

								_			
TABLE 29				BEVEF	RAGE	CONT	AINER	DATA			
	CAP	ACITY	C	DIMENSIONS, IN	I,	CC	ONTAINER D	ATA	BOTTLES		
TYPE CONTAINER	FLUID OZ	GAL	LENGTH	WIDTH OR MAX. DIAM.	HEIGHT	WEIGHT LBS	SP. HT. BTU/LB/°F	MATERIAL	OR CANS PER CASE	LIQUID WEIGHT LBS	TO COOL 1°F WHEN FULL
Bottles Beer, Tall, Ret. Beer, Squat, N.R. Beer, Quart, N.R. Coca Cola Soda- 6 Soda- 7 Soda- 8 Soda- 9 Soda- 12 Soda-32	12 12 32 6 6 7 8 9 12 32	111111111	11111111	2.50 2.60 3.63 2.37 2.50 2.37 2.50 2.25 2.67 3.67	9.50 5.75 11.25 7.75 7.75 7.87 7.25 9.13 9.75 11.50	0.75 0.40 1.03 0.85 0.88 0.88 0.88 0.88 1.00	0.20 0.20 0.20 0.20 0.20 0.20 0.20 0.20	Glass		0.76 0.76 2.03 0.38 0.38 0.44 0.50 0.56 0.75 2.03	0.91 0.84 2.24 0.55 0.56 0.62 0.68 0.74 0.96 2.41
Cans 12 oz. Beer, Steel 12 oz. Beer, Alum. Pint Beer, Steel	12 12 16	-	-	2.63 2.55 2.63	4.59 4.59 6.22	0.111 0.047 0.134	0.12 0.214 0.12	Steel Alum. Steel	one due	0.76 0.76 1.02	0.77 0.77 1.03
Cases Beer Tall, 12 oz, Ret. Tall, 12 oz, Ret. Squat, 12 oz, N.R. Quart, N.R. Can, 12 oz Tray Coca Cola Soda 6 oz 8 oz 12 oz Quart	-		15.87 16.19 17.31 15.94 16.00 18.50 14.50 18.00 16.67	10.63 10.63 11.56 12.00 10.50 12.13 11.00 11.75 12.25	10.06 9.69 6.50 10.63 4.75 8.25 8.25 7.75 10.25 12.50	1.81 3.19 1.38 1.81 0.27 5.25 6.90 6.50 9.25 8.00	0.34 0.40 0.34 0.34 0.60 0.60 0.60 0.60	Corr. Paper Fiber ³ Corr. Paper Corr. Paper Corr. Paper Wood Wood Wood Wood	24 24 24 12 24 24 24 24 24 24 12	18.26 18.26 18.26 24.34 18.26 9.12 9.12 12.00 18.00 24.00	22.48 23.14 20.65 25.16 18.67 12.27 13.26 15.90 23.55 28.80
Kegs — Wood V _s ¼ ½ Full Kegs — Insulated Steel ½ ½		4 8 15 31 8	-	13.5 17.0 20.0 24.0 16.0	16.0 21.0 24.0 31.0 17.25 23.5	22 35 65 105 33 60	0.60 0.60 0.60 0.60 0.12	Wood Wood Wood Wood Steel	-	33 70 130 260 62 124	41 80 155 300 60 120
Kegs — Cast Aluminum '/s '/4 '/4	-	4 8 16	_ _ _ _	13.0 16.0 19.25	15.0 17.25 23.5	22 32 70	0.12 0.21 0.21 0.21	Aluminum Aluminum Aluminum	_ _ _	31 62 124	35 64 130

Notes: 1. Specific heats of beer and carbonated beverages estimated at 1 Btu/lb/°F.

- 2. Storage areas may be estimated on the basis of 24 cans per one half cubic foot, and 24 bottles per 2 cubic feet; one third additional area should be allowed for aisles.
- 3. Fiber is utilized for returnable bottle cartons in southern climates.
- 4. Case weights include partitions, but no bottles or cans.

TABL 30	_	NFILT OAD BEER	S W	HENS		ING
SIZE OF CONTAINE	(OU	MPER ITSIDE STOR	TEMP	PERAT	UREN	IINUS
	60	55	50	45	40	35
Full keg Half keg Quarter keg Case 24-12 oz.	3200 2600 2200	2600 2100 1900	2100 1700 1600	1700 1400 1300	1400 1100 1000	1100 900 800
bottles	2100	1800	1500	1200	900	700

Note 1: Loads are in Btu/24 hr. Multiply the number of kegs delivered per day by the appropriate load per keg, and utilize the resultant number as the total 24 hr infiltration heat gain in Part III B, Form LE-1

TYPE AND SIZE		TEMPERATURE REDUCTION, °F										
OF CONTAINER	65	50	40	30	20	15	10	5				
Keg — Wood One Keg Half Keg Quarter Keg Eigth Keg	-	-	12000 5600 3200 1640	9000 4650 2400 1230	6000 3100 1600 820	4500 2325 1200 615	3000 1550 800 410	1500 775 400 205				
Keg — Aluminum Half Keg Quarter Keg Eigth Keg	=	-	5200 2560 1400	3900 1920 1050	2600 1280 700	1950 960 525	1300 640 350	650 320 175				
Keg — Steel Half Keg Quarter Keg	-		4800 2400	3600 1800	2400 1200	1800 900	1200 600	600 300				
Bottles 6 oz² 7 oz² 8 oz² 9 oz² 12 oz²	32 37 42 47 60	27 31 35 38 50	22 25 28 30 40	16 20 21 23 30	10.8 12.4 14.0 15.2 20.0	8.1 9.3 10.5 11.4 15.0	5.4 6.2 7.0 7.6 10.0	2.1 3.1 3.1 5.1				
Cases 12 Oz Tray, Can Tall, 12 Oz, Ret. Squat, 12 Oz, N.R.	1214.2 1502.8 1341.6	934.0 1156.0 1032.0	746.8 924.8 826.0	560.4 693.6 619.2	373.4 462.4 413.0	280.2 346.8 309.6	186.7 231.2 206.5	93.4 115.6 103.2				

Notes: 1. Specific heat of beer estimated at 1 Btu/lb/°F. 2. Tabulated values may be utilized for carbonated beverages.

TABLE 32		WALK-IN BEER C	OOLER STO	RAGE LOADS	
WALK-IN	CAPACITY	TOTAL LOAD	WALK-IN	CAPACITY	TOTAL LOAD INCLUDING PRODUCT IN BTU/HR
COOLER	CASES OF 24 —	INCLUDING PRODUCT	COOLER	CASES OF 24 —	
SIZE	12 OZ BOTTLES	IN BTU/HR	SIZE	12 OZ BOTTLES	
6' × 6'	110	5400	10' × 14'	470	13960
6' × 8'	150	6470	10' × 16'	540	15400
6' × 10'	190	7450	10' × 18'	610	16820
6' × 12'	230	8520	10' × 20'	680	18150
8' × 10'	260	9080	12' × 16'	650	17500
8' × 12'	315	10330	12' × 18'	740	19260
8' × 14'	370	11880	12' × 20'	820	20800
8' × 16'	425	13130	12' × 30'	1240	28690

Note: Loads are based on 10' cooler heights, 35°F holding temp., 20°F product temp. reduction and a 75°F environment, and have been adjusted for 18 hr compressor operation. A 20% daily inventory turn was assumed.

TABLE 33		DOM	ESTIC (OUTDOOR DESIG	N DAT	A¹	
LOCATION	DBWB °F °F	LOCATION	DBWB °F °F	LOCATION	DBWB °F °F	LOCATION	DBWB °F °F
Alabama		Illinois		Montana		South Dakota	
Birmingham	97 79	Champaign	96 79	Billings	94 68	Rapid City	96 72
Mobile	95 80	Chicago	94 78	Helena	90 65	Sioux Falls	95 77
Montgomery	98 80	Springfield	95 79	Nebraska		Tennessee	
Tuscaloosa	98 81	Indiana		Omaha	97 79	Chattanooga	97 78
Alaska		Evansville	96 79	Nevada		Knoxville	97 80
Anchorage	73 63	Fort Wayne	93 77	Las Vegas	108 72	Memphis	98 80
Fairbanks	82 64	Indianapolis	93 78	Reno	94 64	Nashville	97 79
Juneau	75 66	Terre Haute	95 79	New Hampshire		Texas	00.70
Arizona		Iowa		Concord	91 75	Amarillo	98 72
Douglas	100 70	Cedar Rapids	92 78	New Jersey		Corpus Christi	95 81
Phoenix	108 77	Des Moines	95 79	Newark	94 77	Dallas	101 79
Tucson	105 74	Kansas		Trenton	92 78	El Paso	100 70
Arkansas		Dodge City	99 74	New Mexico		Galveston	91 82
Fort Smith	101 79	Topeka	99 79	Albuquerque	96 66	Houston	96 80
Little Rock	99 80	Wichita	102 77	Santa Fe	90 65	San Antonio	99 77
California	33 00	Kentucky		New York		Utah	07.07
	100 70	Lexington	94 78	Albany	91 76	Salt Lake City	97 67
Bakersfield	103 72	Louisville	96 79	Buffalo	88 75	Vermont Burlington	88 74
Blythe	111 78	Louisiana		New York	94 77	Virginia	00 /4
Fresno	101 73	Baton Rouge	96 81	Rochester	91 75	Norfolk	94 79
Los Angeles	94 72	New Orleans	93 81	Syracuse	90 76	Richmond	96 79
Oakland	85 65	Shreveport	99 81	North Carolina		Roanoke	94 76
Sacramento	100 72		33 01	Asheville	91 75	Washington	0170
San Francisco	80 64	Maine	00 75	Charlotte	96 78	Seattle	81 67
Colorado		Portland	88 75	North Dakota	00 70	Spokane	93 66
Denver	92 65	Maryland		Bismarck	95 74	Yakima	94 69
Connecticut		Baltimore	94 79		92 76	West Virginia	
Hartford	90 77	Hagerstown	94 77	Fargo	92 /6	Charleston	92 76
New Haven	88 77	Massachusetts		Ohio		Parkersburg	93 77
Delaware		Boston	91 76	Cincinnati	94 78	Wisconsin	
Wilmington	93 79	Springfield	91 76	Cleveland	91 76	Green Bay	88 75
	33 /3	Worcester	89 75	Dayton	92 77	Madison	92 77
Dist. Of Columbia	04.70	Michigan		Oklahoma		Milwaukee	90 77
Washington	94 78	Detroit	92 76	Oklahoma City	100 78	Wyoming	
Florida		Grand Rapids	91 76	Lawton	103 78	Caspar	92 63
Jacksonville	96 80	Lansing	89 76	Tulsa	102 79	Cheyenne	89 63
Miami	92 80	Larioning	00 70	7 4.04	102 70	Canada	
Orlando	96 80	Minnesota		Oregon		Calgary	87 66
Tallahassee	96 80	Duluth	85 73	Portland	91 69	Edmonton	86 69
Tampa	92 81	St. Paul	92 77	Pennsylvania		Goose Bay	86 69
Georgia		Minneapolis	92 77	Erie	88 76	Halifax	83 69
Atlanta	95 78	Mississippi		Philadelphia	93 78	Hamilton	91 77
Savannah	96 81	Jackson	98 79	Pittsburg	90 75	Montreal	88 76
Hawaii		Missouri		Rhode Island		Ottawa	90 75
Honolulu	87 75	Kansas City	100 79	Providence	89 76	Toronto	90 77
Idaho		St. Louis	96 79	South Carolina	00 ,0	Vancouver	80 68
Boise	06 60			Charleston	05 01		90 75
DOISE	96 68	Springfield	97 78	Charleston	95 81	Winnipeg	30 /5

Tables 33 & 34 extracted from 1972 ASHRAE Handbook of Fundamentals - Reprinted by Permission

TABLE 34	.,	INTERNA	ATIONA	L OUTDOOR DE	SIGN D	ATA¹	
LOCATION	DBWB °F °F	LOCATION	DBWB °F °F	LOCATION	OBWB °F °F	LOCATION	DBWB °F °F
Afghanistan		Cuba		Indonesia		Pakistan	
Kabul	98 66	Havana	92 81	Djakarta	90 80	Chittagong	93 82
Algeria		Denmark		Makasser	90 80	Kaachi	100 82
Algiers	95 77	Copenhagen	79 68	Iran		Panama & Canal Z	
Argentina		Dominican Repub	lic	Abadan	116 82	Panama City	93 81
Buenos Aires	91 77	Santo Domingo	92 81	Meshed	99 68	Paraguay	
Tucuman	102 76	Ecuador		Tehran	102 75	Asuncion	100 81
Australia		Guayaquil	92 80	Iraq		Peru	de ex
Adelaide	98 72	Quito	73 63	Baghdad	113 73	Lima	86 76
Brisbane	91 77	El Salvador		Ireland		Philippines	
Melbourne	95 71	San Salvador	98 77	Shannon	76 65	Manila	94 82
Perth	100 76		90 //	Israel		Puerto Rico	
Sydney	89 74	Ethiopia	04.00	Tel Aviv	96 74	San Juan	89 81
Austria		Addis Ababa	84 66	Italy		Saudi Arabia	
Vienna	88 71	Finland		Naples	91 74	Dhahran	111 86
Bahamas		Helsinki	77 66	Rome	94 74	Riyadh	110 78
Nassau	90 80	France		Japan		South Africa	
Belgium		Marseilles	90 72	Sapporo	86 76	Capetown	93 72
Brussels	83 70	Paris	89 70	Tokyo	91 81	Johannesburg	85 70
Bermuda		Germany		Jordon		Spain	
Kindley AFB	87 79	Berlin	84 68	Amman	97 70	Barcelona	88 75
Bolivia		Hamburg	80 68	Kenya		Madrid	93 71
La Paz	71 58	Munich	86 68	Nairobi	81 66	Sweden	
Brazil		Ghana	00 00	Lebanon	01 00	Stockholm	78 64
Brasilia	89 76	Accra	91 80	Beirut	93 78	Syria	
Porto Alegre	95 76		31 00		33 70	Damascus	102 72
Rio de Janeiro	94 80	Greece	00.70	Libya		Thailand	102 72
Salvador	88 79	Athens	96 72	Bengasi	97 77	Bangkok	97 82
Sao Paulo	86 75	Greenland		Malaysia		Tunisia	37 02
British Honduras		Narssarssuaq	66 56	Penang	93 82	Tunis	102 77
Belize	90 82	Guatemala		Singapore	92 82		102 //
Burma		Guatemala City	83 69	Mexico		Turkey	04 60
Mandalay	104 81	Guyana		Guadalajara	93 68	Ankara Istanbul	94 68 91 75
Cambodia		Georgetown	89 80	Merida	97 80		
Phnom Penh	98 83	Haiti		Mexico City	83 61	United Arab Reput	
Ceylon		Port Au Prince	97 82	Monterrey	98 79	Cairo	102 76
Colombo	90 81	Honduras		Vera Cruz	91 83	United Kingdom	
Chile		Tegucigalpa	89 73	Netherlands		Belfast	74 65
Santiago	90 71	Hong Kong	00 70	Amsterdam	79 65	Birmingham	79 66
Valparaiso	81 67	Hong Kong	92 81	New Zealand		London	82 68
Colombia			92 01	Auckland	78 67	Uraguay	
Bogota	72 60	Iceland	F0 F4	Wellington	76 66	Montevideo	90 73
Cali	87 73	Reykjavik	59 54		70 00	Venezuela	
Medellin	84 70	India		Nicaragua	04.04	Caracas	84 73
Congo		Bombay	96 82	Managua	94 81	Puerto Ordaz	95 82
Kinasha	92 81	Calcutta	98 83	Nigeria		Maracaibo	97 84
Stanleyville	92 81	New Delhi	110 83	Lagos	92 82	Valencia	95 80

Note 1: Design temperatures shown in Tables 33 & 34 are equalled or exceeded during 1% of summer months.

TABLE 35					SI METR
		Α	RE	=	A
Acre	× 4.0	147E +	03	=	Metre ² (m ²)
ft ²					Metre ² (m ²)
in ²					Metre ² (m ²)
mi ²			-		Metre ² (m ²)
yd²	× 8.3	361E —	01	=	Metre ² (m ²)
		EN	EF	?	GY
Btu					Joule (j)
Calorie					Joule (j)
Kilocalorie					Joule (j)
kw-h w-h					Joule (j) Joule (j)
ENE	RG	V PI	FR		UNITTIME
Btu/(ft²•s)				_	Watt Per Metre ² (w / m ²)
Btu/(ft2 min)			-		Watt Per Metre ² (w/m²)
Btu/(ft²•h)					Watt Per Metre ² (w/m ²)
Cal/(cm² • min)					Watt Per Metre ² (w/m²)
w/cm²					Watt Per Metre ² (w/m ²)
w/ft²					Watt Per Metre ² (w/m ²)
w/in²			-		Watt Per Metre ² (w/m ²)
		Н	E	4	Т
Heat Density:				_	
Btu/ft ²					Joule Per Metre ² (j/m ²)
Cal/cm ²	× 4.	187E +	04	=	Joule Per Metre ² (j/m ²)
Heat Flux Density:					
Btu / (ft2 • h)	× 3.	155E +	00	=	Watt Per Metre ² (w / m ²)
Cal/(cm ² s)	× 4.1	187E +	04	=	Watt Per Metre ² (w / m ²)
Heat Transfer Coefficie	ent (U):				
Btu/(h oft2 o oF)	× 5.	678E +	00	=	Watt Per Metre ² - Kelvin [w/(m ² • K)]
Btu/(seft2e oF)	× 2.	044E +	04	=	Watt Per Metre ² - Kelvin (w/(m ² • K))
Specific Enthalpy (Late					
Btu/lb					Joule Per Kilogram (j / kg)
Cal/g	× 4.	18/E +	U3	==	Joule Per Kilogram (j / kg)
Specific Heat (C):					
Btu/(lb • °F)					Joule per Kg ● Kelvin [j / (kg ● K)]
Cal/(g • °C)		18/E +	03	=	Joule per Kg ● Kelvin [j / (kg ● K)]
Thermal Conductivity (2045	00		W B . M
(Btu • Ft)/(h • ft² • °F)					Watt Per Metre — Kelvin [w/(m • K)]
(Btu • In)/(S • ft² • °F)					Watt Per Metre — Kelvin [w/(m • K)]
(Btu • In)/(h • ft² • °F) Cal / (cm • s • °C)					Watt Per Metre — Kelvin [w/(m • K)] Watt Per Metre — Kelvin [w/(m • K)]
Thermal Diffusivity:					
ft²/h	× 2.	581E -	05	=	Metre ² Per Sec (m ² /s)
Thermal Resistance (R	:				
(°F•h•ft²)/Btu	× 1.	761E —	01	==	Kelvin — Metre²/Watt {(K • m²) / w}
		LE	NC	3	TH
ft					Metre (m)
in					Metre (m)
micron					Metre (m)
	. 0	2445	04		Adam Ind
yd					Metre (m) Metre (m)

	LIGHT
Footcandle	× 1.076E + 01 = Lux (lx)
Footlambert	\times 3.426E + 00 = Candela/Metre ² (cd/m ²)
Todambert	A STEEL 1 SO SUITOR HIS SOUTH
	MASS
Gram	× 1.000E - 03 = Kilogram (kg)
Ounce (Avoir)	\times 2.835E $-$ 02 $=$ Kilogram (kg)
Pound (Avoir)	\times 4.536E $-$ 01 $=$ Kilogram (kg)
Tonne	\times 1.000E + 03 = Kilogram (kg)
Ton (long, 2240 lb)	× 1.016E + 03 = Kilogram (kg)
Ton (Metric)	× 1.000E + 03 = Kilogram (kg)
Fon (short, 2000 lb)	× 9.072E + 02 = Kilogram (kg)
M	ASS PER UNIT TIME
b/h	× 1.260E - 04 = Kilogram Per Second (kg/s)
lb/min	\times 7.560E $-$ 03 = Kilogram Per Second (kg/s)
lb/sec	\times 4.536E $-$ 01 $=$ Kilogram Per Second (kg/s)
b/(hp•h)	\times 1.690E $-$ 07 $=$ Kilogram Per Joule (kg/j)
	DENSITY
g/cm³	× 1.000E + 03 = Kilogram Per Metre ³ (kg/m ³)
Oz (Avoir) / Gal	× 7.489E + 00 = Kilogram Per Metre ³ (kg/m ³)
b/ft³	× 1.602E + 01 = Kilogram Per Metre ³ (kg/m ³)
b/in³	× 2.768E + 04 = Kilogram Per Metre ³ (kg/m ³)
b/gal	× 1.198E + 02 = Kilogram Per Metre ³ (kg/m ³)
/yd³	× 5.933E - 01 = Kilogram Per Metre ³ (kg/m ³)
	POWER
Btu/h	× 2.931E - 01 = Watt (w)
Btu / min	\times 1.758E + 01 = Watt (w)
Cal./m	\times 6.978E - 02 = Watt (w)
hp[550ft • lbf/s]	\times 7.457E + 02 = Watt (w)
hp (boiler)	\times 9.810E + 03 = Watt (w)
har falantain)	\times 7.460E + 02 = Watt (w)
np (electric)	7 OFFF . DO 18/ (.)
	\times 7.355E + 02 = Watt (w)
hp (metric)	× 7.355E + 02 = Watt (w) × 3.517E + 03 = Watt (w)
hp (metric)	
hp (metric) ton of refrig.	× 3.517E + 03 = Watt (w)
hp (metric) ton of refrig. Atmosphere	× 3.517E + 03 = Watt (w) PRESSURE
hp (metric) ton of refrig. Atmosphere Cm of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa)
hp (metric) ton of refrig. Atmosphere Cm of Hg Cm of Water	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa)
np (metric) ton of refrig. Atmosphere Cm of Hg Cm of Water Ft of Water	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa)
Atmosphere Cm of Hg Cm of Water It of Hg In of Hg In of Water It of Water In of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa)
Atmosphere Cm of Water to of Water n of Hg n of Hg of Water n of Hg n of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.889E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa)
Atmosphere Cm of Hg Cm of Water In of Hg In of Water In of Hg In of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa)
Atmosphere Cm of Hg Cm of Water In of Hg In of Water In of Hg In of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.889E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa)
hp (metric) ton of refrig. Atmosphere Cm of Hg Cm of Water Ft of Water In of Hg In of Water Mm of Hg Psi'	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.889E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa)
Atmosphere Cm of Hg Cm of Water Ft of Water In of Hg In of Hg Mm of Hg Psi	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 → 1.8 = °C
Atmosphere Cm of Hg Cm of Water Ft of Water In of Hg In of Water Mm of Hg Psi'	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 + 1.8 = °C × 1.8 + 32 = °F
°F	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 + 1.8 = °C × 1.8 + 32 = °F + 459.67 + 1.8 = Kelvin
Atmosphere Cm of Hg Cm of Water Ft of Water In of Hg In of Hg In of Hg Cm of Gate Cm of Hg Cm of Gate Cm of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 + 1.8 = °C × 1.8 + 32 = °F + 459.67 + 1.8 = Kelvin × 1.8 - 459.67 = °F
Atmosphere Cm of Hg Cm of Water Ft of Water In of Hg In of Hg On o	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 + 1.8 = °C × 1.8 + 32 = °F + 459.67 + 1.8 = Kelvin × 1.8 - 459.67 = °F + 273.15 = Kelvin
trong (metric) on of refrig. Atmosphere on of Hg on of Water of Hg on of Hg on of Hg on of Hg or of Hg	× 3.517E + 03 = Watt (w) PRESSURE × 1.013E + 05 = Pascal (pa) × 1.333E + 03 = Pascal (pa) × 9.806E + 01 = Pascal (pa) × 2.989E + 03 = Pascal (pa) × 3.386E + 03 = Pascal (pa) × 2.490E + 02 = Pascal (pa) × 1.333E + 02 = Pascal (pa) × 6.895E + 03 = Pascal (pa) TEMPERATURE - 32 + 1.8 = °C × 1.8 + 32 = °F + 459.67 + 1.8 = Kelvin × 1.8 - 459.67 = °F

Notes:

- 1. No equivalents for the abbreviations "Psia" and "Psig" are utilized in the SI System (if necessary to so designate a given pressure, it would be defined as "an absolute pressure of 50kpa", or "25 kpa (Gage)", etc.
- 2. All factors have been rounded off to 4 significant digits and are, therefore, by SI definition "approximate."
- 3. The "E" notation is utilized for convenience in electronic data processing, and has no other significance.
- 4. SI equivalents are always shown as a number greater than 1 and less than 10. Examples: 1.055E + 03 joule per Btu (rather than 1055); 1.000 E 03 kg per gram (rather than 0.001), etc.

TABLE 36	WEIGHT EQUIVALENCY OF COMMON MEASURES							
Product	Measure	Weight - Lbs						
Apples Bananas Beef, Dressed	Bushel Or Box Barrel Bunch Head (Carcass)	50 125 50 550						
Butter Calves, Dressed Hogs, Dressed Ice	Tub Head (Carcass) Head (Carcass) Bushel	60 150 200 50						
Lamb, Dressed Peaches/Pears Potatoes	Head (Carcass) Bushel Bushel	45 55 60						

			METRIC N FACTORS
Btu Cubic Feet Cubic Feet	×	252 = 28.32 = 472 =	Liters Cubic Centimeters
Per Minute Cubic Inches Cubic Meters		16.39 = 35.31 = 264.2 =	
	×	1000 =	Liters
Cubic Yards Drams	×	764.6 = 1.772 =	Grams
Feet Per Second		30.48 = 1.097 =	Centimeters Kilometers per Hour
Gallons Grams		3.785 =	Liters
Grams Per Cubic Centimeter			Pounds per Cubic Foot
Grams Per Liter Grams Per	×		Pounds per
Square Centimeter Horsepower (English)	×	1.014 =	
Horsepower Inches	×	641.1 = 2.54 =	Centimeters
Inches Of Mercury	×	34.53 =	Grams per Sq. Centimeter
Kilograms Kilograms Per	×	2.205 =	Pounds
Square Centimeter		28.96 = 14.22 =	Inches of Mercury Pounds per Sq In
Kilocalories	×	3.97 =	Btu
Kilometers Kilowatts Liters	×	3281 = 860.5 = 1.057 =	Kilocalories per Hour
Meters	×	3.281 =	Feet
Ounces (Avoir) Ounces (Troy)		28.35 = 31.10 =	
Pounds Pounds Per	×	453.6 = 16.02 =	Grams
Cubic Foot			Cubic Meter Cubic Centimeters
Quarts Square Feet	×	929 =	Square Centimeters
Square Inches Square Meters	×	6.45 = 10.76 =	
Tons (Short) Tons (Metric)	×	907.2 = 1.102 =	Kilograms
Watts	×	860.5 =	

TABLE 38 ENGLIS	Н	CONV	ER	SION FACTORS
Atmospheres Acres Barrels Bushels Bushels Cubic Feet	×	43,560 31.5 1.245	=	Square Feet Gallons Cubic Feet
Cubic Feet Cubic Yards Cubic Yards Gallons Grains (Avoir) Horsepower	× × ×	7.48 27 202 231 1.0 2547	= = = =	Gallons (U.S. Liq.) Cubic Inches
Horsepower Kilowatts Kilowatts Kilowatts Ounces (Avoir) Ounces (Fluid)	×××××	3413 1.34 1000 437.5	= =	Watts Btu/hr Horsepower Watts Grains Cubic Inches
Ounces (Troy) Ounces (Troy) Pounds Per Sq In Pounds Per Sq In Pounds Pounds		1.097 27.686 2.307 7000	= = =	Grains Ounces (Avoir) Inches of Water Feet of Water Grains Ounces (Avoir)
Pounds Pounds Pounds (Troy) Pounds (Troy) Pounds (Troy) Pounds (Troy) Pounds Per Sq In	×	1.22 5760 13.17	= =	Pounds (Troy) Grains Ounces (Avoir)
Quarts (Liquid) Square Feet Square Yards Tons (Short) Tons (Long) Tons Of Refrigeration Watts	× × ×	57.75 144 1296 2000 1.12 12000 3.41	= = = =	o quaro monos

TABLE 39	M	ETRIC CO	N۱	ERSION FACTORS
Atmospheres	×	76	=	Centimeters of Mercury
Centimeters	×	10	=	Millimeters
Cubic Meters	X	1,000,000	=	Cubic Centimeters
Cubic Meters	X	1,000	=	Liters
Dekagrams	X	10	=	Grams
Dekaliters	×	10	=	Liters
Dekameters	×	10	=	Meters
Grams	×	1,000	=	Milligrams
Kilocalories	×	1,000	=	Calories
Kilograms	×	1,000	=	Grams
Kiloliters	×	1,000	=	Liters
Kilometers	×	1,000	=	Meters
Kilowatts	×	860.5	=	Kilocalories per Hour
Liters	×	1,000	=	Cubic Centimeters
Meters	×	100	=	Centimeters
Meters	×	1,000	=	Millimeters
Milliliters	×	1.0	=	Cubic Centimeters
Square				
Centimeters	×	100	=	Square Millimeters
Square Meters	×	10,000	=	Square Centimeters
Watts	×	860.5	=	Calories per Hour

OUTSIDE AREA, ROOM VOLUME AND REFRIGERATION LOADS TABLE 40 FOR WALK-IN COOLERS AND FREEZERS AT 95°F AMBIENT3 8 FT HEIGHT² 10 FT HEIGHT² ROOM CAPACITY REQUIREMENTS LESS CAPACITY REQUIREMENTS LESS OUTSIDE ROOM ROOM OUTSIDE SIZE PRODUCT LOAD-BTU/HR PRODUCT LOAD-BTU/HR AREA VOLUME AREA VOLUME OUTSIDE SQ FT CU FT SQ FT CU FT - 20°F - 10°F 28°F - 20°F - 10°F 28°F W×L 6× 6 6× 8 6 × 10 6 × 12 8 × 10 8 × 12 8 × 14 8 × 16 10×10 10 × 12 10 × 14 10 × 16 10×18 10 × 20 12 × 14 12×16 12×18 12 × 20 12×30 14×16 14 × 20 14 × 24 14×28 14 × 32 16 × 16 16×20 16 × 24 16 × 28 16 × 32 16 × 36 20 × 20 20 × 24 20×28 20×32 20 × 36 20 × 40 30×20 30×24 30×30 40 × 30 40 × 40

Notes: 1. Ratings based on 3" foamed-in-place urethane, average usage, indoor installation & 18 hour compressor operation

2. Heights represent internal clearance. Overall heights with floor: 8'6" & 10'6"

3. Correction Factors — Other Ambients: 80°F — 0.75; 100°F — 1.10; 115°F — 1.35

^{4.} Correction Factors — Other Usage: Light (Long-Term Storage) — 0.80; Heavy — 1.15-1.40

^{5.} IMPORTANT: Utilization of charted values requires application of properly rated equipment.

ROOM	CO	OLERS	FREE	ZERS	ROOM	COO	LERS	FREE	ZERS
CU FT	LBS/DAY	PRODUCT LOAD BTU/HR	LBS/DAY	PRODUCT LOAD BTU/HR	CU FT	LBS/DAY	PRODUCT LOAD BTU/HR	LBS/DAY	PRODUCT LOAD BTU/HR
250	850	567	300	112	7000	15800	10500	3800	1425
500	1600	1067	600	225	7500	16100	10700	4000	1500
1000	3000	2000	1000	375	8000	16500	11000	4200	1575
1500	4200	2800	1400	525	8500	18000	12000	4400	1650
2000	5100	3400	1700	637	9000	21000	14000	4600	1725
2500	6900	4600	1900	713	9500	22500	15000	4900	1840
3000	8500	5700	2100	787	10000	24000	16000	5100	1910
3500	9800	6500	2250	844	15000	31000	20700	7600	2850
4000	11100	7400	2400	900	20000	40000	26700	9400	3525
4500	12000	8000	2500	938	30000	54000	36000	15000	5625
5000	12900	8600	2900	1090	40000	65000	43200	18000	6750
5500	13700	9100	3200	1200	60000	108000	72000	26000	9750
6000	14600	9700	3400	1275	80000	150000	100000	35000	13100
6500	15200	10100	3600	1350	100000 & up	190000 & up	127000 & up	53000 & up	19500 & up

Notes: 1. Values have been adjusted for 18 hour compressor operation, and apply to holding rooms only with entering product at 15°F above the refrigerator temperature.

2. This table is not to be used for unusual product loads, or if product specifics are known.

	DAILY PRODUCT	PRODUCT	FINAL PRODUCT TEMPERATURE - °F								
PRODUCT	QUANTITY	ENTERING TEMP. °F	60	40	35	32	0	-10	-20	-30	
Bakery Goods	100 Lbs	80 55 36	82 - -	164 34	185 82 4	197 95 16	545 443 365	564 462 384	583 480 403	60 500 42	
Beef	1000 Lbs	100 55 34	1667 - -	2500 625	2708 833	2833 958 83	9194 7319 6444	9422 7547 6672	9649 7774 6899	987 800 712	
Lamb & Veal	1000 Lbs	100 55 34	1824 - -	2736 684	2964 912	3100 1049 91	9477 7435 6477	9726 7674 6716	9965 7913 6955	1020 815 719	
Pork	1000 Lbs	100 55 34	1178	1766 441	1914 589	2002 677 59	6106 4781 4104	6283 4958 4281	6461 5136 4459	663 531 463	
Beer & Soda	100 Cases	80 60 50	3555 - -	7110 3555 1775	8000 4440 2670	8530 4980 3200		-	-	-	
Frozen Food	1000 Lbs	10	_	-	-	_	278	556 278	833 556	111	
Ice Cream ³	100 Gal • Soft Mix • Pre-Hardened	28 10	-	-	-	-	2667 364	2962 606	3284 793	363 116	
Milk	100 Gal	45	-	228	456	547	-	-	-	-	
Poultry & Fresh Game	1000 Lbs	55 50 35	=	658 439	879 658	1009 790 132	7747 7528 6870	7980 7761 7103	8214 7995 7337	844 822 757	
Pizza Meat Pies & TV Dinners	100 14 Oz Units	80 60 35	73 - -	146 73	164 91 -	175 102 11	611 537 446	630 557 466	649 576 485	66 59 50	
Sea Food	100 Lbs	70 50 35	47	141 47 -	165 71 -	179 85 14	933 838 768	957 862 792	982 887 817	100 91 84	
Vegetables	1000 Lbs	90 75 55 35	1500 750 	2500 1750 750	2750 2000 1000	2900 2150 1150 150	10409 9659 8659 7659	10666 9916 8916 7916	10922 10172 9172 8172	1117 1047 947 847	

Notes: 1. Values are for 24 hour pulldown and have been adjusted for 18 hour compressor operation.

2. For shorter pulldown periods, or for continuous blast freezing operations, utilize the following formula:

Product Load Btu/hr= Charted Value × 24

Pulldown or Shift Timehrs

3. Ice cream loads must be modified for the preferred hardening period (usually 8-10 hrs) to prevent crystalization.

TABLE		GLASS DISPLAY DOOR LOADS IN BTU/HR FOR WALK-IN COOLERS AND FREEZERS							
NO. OF	COOLE	R@35°F	FREEZER						
DOORS1	75°F AMBIENT	90°F AMBIENT	80°F TD4	90°F TD4	110°F TD4				
2 to 4 5 to 7 8 to 12	960 890 820	1200 1100 1000	1800 1550 1440	2100 1600 1500	2600 2100 2000				
13 to 16 16 to 20	630 550	800 700	1330 1240	1400 1300	1800 1600				

Notes: 1. Values are per door, and are based on standard 30" × 66" double glazed cooler, and triple glazed freezer, doors. Factors for other standard door sizes: 30" × 72": 1.11; 30" x 80": 1.26.

- 2. Values do not apply to reach-in refrigerators.
- Unit coolers should be placed opposite and above the doors (blowing toward the doors) to create an air curtain effect.
- 4. T D represents the difference between box and room temperatures.

TABLE 44		PR	OPERTIES OF SOLID	os	
					EMISSIVITY
MATERIAL DESCRIPTION	SPECIFIC HEAT BTU/LB/°F	DENSITY LB/CU FT	THERMAL CONDUCTIVITY BTU • FT/HR/SQ FT/°F	RATIO	SURFACE CONDITION
Aluminum (alloy 1100)	0.214	171	128.00	0.09 0.20	Commercial sheet heavily oxidized
(76% Cu, 22% Zn, 2% A1) Alundum (aluminum oxide) Asbestos:	0.09 0.186	517	58.00		
pfiber pinsulation Ashes, wood Asphalt	0.25 0.20 0.20 0.22	150 36 40 132	0.097 0.092 0.041 [122] 0.43	0.93	"Paper"
Bakelite Bell metal Bismuth tin Brick, building Brass:	0.35 0.086 [122] 0.040 0.2	81 123	9.70 37.60 0.40	0.93	
red (85% Cu, 15% Zn) yellow (65% Cu, 35% Zn)	0.09 0.09	548 519	87.0 69.0	0.030 0.033	Highly polished Highly polished
Bronze Cadmium Cardon (gas retort) Cardboard Cellulose Cement (Portland clinker)	0.104 0.055 0.17 0.34 0.32 0.16	530 540 3.4 120	17 [32] 53.70 0.20 [2] 0.04 0.033 0.017	0.02 0.81	
Chalk Charcoal (wood) Chrome Brick Clay Coal Coal Tars	0.215 0.20 0.17 0.22 0.3 0.35 [104]	143 15 200 63 90 75	0.48 0.03 [392] 0.67 0.098 [32] 0.07	0.34	About 250 F
Coke (petroleum powdered) Concrete (stone) Copper (electrolytic) Cork (granulated) Cotton (fiber) Cryolite (AIF3 • 3NaF)	0.36 [752] 0.156 [392] 0.092 0.485 0.319 0.253	62 144 556 5.4 95 181	0.55 [752] 0.54 227.00 0.028 [23] 0.024	0.072	Commercial, shiny
Diamond Earth (dry and packed) Felt	0.147	151 95 20.6	27.00 0.037 0.03	0.41	
Fireclay brick Flourspar (CaF₂) German Silver (nickel silver)	0.198 [212] 0.21 0.09	112 199 545	0.58 [392] 0.63 19.00	0.75 0.135	At 1832 F Polished
Glass: crown (soda-lime) flint (lead) pyrex "wool"	0.18 0.117 0.20 0.157	154 267 139 3.25	0.59 [200] 0.59 [200] 0.022	0.94	Smooth
Gold	0.0312	1208	172.00	0.02	Highly polished
Graphite: powder 'Karbate" (impervious) Gypsum Hemp (fiber) Ice:	0.165 0.16 0.259 0.323	117 78 93	0.106 75.00 0.25	0.75 0.903	On a smooth plate
• [32 F] • [-4 F]	0.487 0.465	57.5	1.30 1.41	0.95	
ron: cast wrought Lead Leather (sole) Limestone	0.12 [212] 0.0309 0.217	450 485 707 62.4 103	27.60 [129] 34.90 20.10 0.092 0.54	0.435 0.94 0.28 0.36 to 0.90	Freshly turned Dull, oxidized Gray, oxidized At 145 to 380 F
Linen Litharge (lead monoxide) Magnesia:	0.055	490	0.05		
Magnesia: • powdered • light carbonate Magnesite brick Magnesium	0.234 [212] 0.222 [212] 0.241	49.7 13 158 108	0.35 [117] 0.034 2.20 [400] 91.00	0.55	Oxidized

Note: Values are for room temperature unless otherwise noted in brackets.

TABLE 44		PF	OPERTIES OF SOI	IDS	
					EMISSIVITY
MATERIAL DESCRIPTION	SPECIFIC HEAT BTU/LB/°F	DENSITY LB/CU FT	THERMAL CONDUCTIVITY BTU • FT/HR/SQ FT/ °F	RATIO	SURFACE CONDITION
Marble Nickel Paints:	0.210 0.105	162 555	1.50 34.40	0.931 0.045	Light gray, polished Electroplated, polished
White lacquer White enamel Black lacquer Black shellac Flat black lacquer Aluminum lacquer		63	0.15	0.800 0.910 0.800 0.910 0.960 0.390	On rough plate "Matte" finish On rough plate
Paper Paraffin Plaster Platinum Porcelain Pyrites (Copper)	0.320 0.690 0.032 0.180 0.131	58 56 132 1340 162 262	0.075 0.14 [32] 0.43 [167] 39.90 1.30	0.920 0.910 0.054 0.920	Pasted on tinned plate Rough Polished Glazed
Pyrites (Iron) Rock Salt Rubber: • Vulcanized (soft) • Vulcanized (hard) Sand Sawdust Silica	0.136 [156] 0.219 0.480 0.191 0.316	310 136 68.6 74.3 94.6 12 140	0.08 0.092 0.19 0.03 0.83 [200]	0.860 0.950	Rough Glossy
Silver Snow Freshly fallen At 32°F Steel (mild) Stone (quarried) Tar: pitch	0.0560 0.120 0.200 0.59	654 7 31 489 95	245.00 0.34 1.30 26.20	0.020	Polished and at 440 F Cleaned
• bituminous		75	0.41		
Tin Tungsten Wood: • Hardwoods: (Most woods vary between) • Ash, white • Elm, American	0.0556 0.032 0.450/0.650	455 1210 23/70 43 36	37.50 116.00 0.065/0.148 0.0992 0.0884	0.060 0.032	Bright and at 122 F Filament at 80 F
Hickory Mahogany Maple, sugar Oak, white Walnut, black	0.570	50 34 45 47 39	0.075 0.108 0.102	0.900	Planed
Softwoods: Fir, white Pine, white Spruce Wool: Fiber	0.650 0.670 0.325	22/46 27 27 26 82	0.061/0.093 0.068 0.063 0.065		
• Fabric		6.9/20.6	0.021/0.037		
Zinc: • Cast • Hot-rolled • Galvanizing	0.092 0.094	445 445	65.00 62.00	0.050 0.230	Polished Fairly bright

Note: Values are for room temperatures unless otherwise noted in brackets.

ABLE 45 PROPERTIES OF WATER1							
Specific Heat of Water	=	1 Btu/lb/°F 1 Cal/Gram/°C					
Specific Heat of Ice	=	0.5 Btu/lb/°F 0.5 Cal /Gram/°C					
Latent Heat of Vaporization	=	970 Btu/lb @ 212°F & 1 ATM 540 Cal/Gram @ 100°C & 1 ATM					
Latent Heat of Fusion	=	144 Btu/lb 80 Cal/Gram					
One Cubic Foot	=	62.4 Pounds 7.48 Gallons					
One Gallon	=	8.33 Pounds 3.77 Kilograms					

Note: Water @ 39.2°F

TABLE 46	PROPERTIES OF AIR1					
One Pound of One Cubic Foot	of Air = 0.075 Pounds					
One Cubic Fo Per Minute (Ci						

Note: Standard Dry Air @ 69.8F° and 1 Atmosphere Pressure.

TABLE 47	PROPERTIES OF LIQUIDS											
	NORMAL BOILING	ENTHALPY OF VAPORIZATION BTU/LB	SPECIFIC HEAT, Cp		VISCOSITY		ENTHALPY	SPECIFIC GRAVITY OR DENSITY (P)		THERMAL ² CONDUCTIVITY		FREEZING
NAME OR DESCRIPTION	POINT °F AT 1 ATM		BTU/LB/°F	TEMP °F	LB/(HR) (FT)	TEMP °F	OF FUSION BTU/LB	LB/CU FT	TEMP °F	к	TEMP °F	POINT °F
Acetaldehyde Acetic Acid Acetone Alcohol	69.44 245.3 133.2	245.1 174.1 228.9	0.522 0.514	79-203 37-73	0.558 2.956 0.801	68 68 68	84.0 42.1	48.9 65.49 49.4	64.4 68 68	0.099 0.102	68 86	- 192.3 61.9 - 139.6
Allyl Allyl Amyl Ethyl Isobutyl Methyl	206.6 280.6 173.3 226.4 148.9	294.1 216.3 367.5 249 473.0	0.655 0.680 0.116 0.601	70-205 32-208 68 59-68	3.298 9.686 2.889 9.450 1.434	68 73.4 68 68 68	48.0 46.4 42.7	53.31 51.06 50.0 49.27 49.40	68 59 68 68 68	0.104 0.094 0.082 0.105 0.124	77-86 86 68 68 68	- 200.2 - 110.2 - 162.4 - 179.1 - 144.0
Ammonia Aniline Benzene Bromine Brine, CaCl ₂	- 28 363.8 176.2 137.8	583.2 186.6 169.4 79.4	1.099 0.512 0.412 0.107	32 46-180 68 68	0.643 10.806 1.580 2.390	- 28.3 68 68 68	142.9 48.8 54.2 28.5	43.50 63.77 54.9 194.7	- 50 68 68 68	0.290 0.100 0.085	5-86 32-68 68	- 107.9 20.84 42.0 19.0
(20% by wt) Carbon			0.744	68	4.800	68		73.8	68	0.332	68	2.0
Disulfide Carbon Tetra-	115.3	148.8	0.240	68	0.880	68	24.8	78.9	68	0.093	86	- 168.0
chloride	170.2	83.7	0.201	68	2.340	68	12.8	99.5	68	0.062	68	- 9.0
Chloroform Ethyl Ether Ethyl Acetate Ethyl Chloride	142.3 94.06 170.8 54.2	106.0 151.0 183.8 165.9	0.234 0.541 0.468 0.368	68 68 68 32	1.360 0.560 1.090	68 68 68	42.4 51.2 29.68	92.96 44.61 52.3 56.05	68 68 68 68	0.075 0.081 0.101 0.179	68 68 68 33. 6	- 81.8 - 177.3 - 116.3 - 213.5
Ethylene Bromide	268.8	99.2	0.174	68	0.0694	68	24.82	136.05	68			49.2
Ethylene Chloride	182.3	153.4	0.301	68	0.0338	68	38.02	77.10	68			- 31.64
Ethylene Glycol	388.4	344.0					77.86	69.22	68	0.100	68	12.7
Formic Acid Glycerine (glycerol) Heptane Hexane	213.3 359 (20 mm) 209.2 154	215.8 138.0 145.0	0.526 0.532 0.538	68 68 68	0.0719 43.100 0.990 0.775	68 68 68 68	118.89 60.4 65.0	76.16 78.72 42.7 41.1	68 68 68 68	0.104 0.113 0.0741 0.0720	68 68 68	47.1 68.0 - 132.0 - 139.0
Hydrogen Chloride	- 120.8	191.0					23.6	74.6	b.p.			- 174.6
Kerosene Linseed Oil Methyl Acetate Methyl lodide Naphthalene Nitric Acid Nitrobenzene Octane Petroleum n-Pentane	400-560 134.6 108.5 411.4 186.8 411.6 258.3 96.8	177.0 82.6 136.0 270.0 142.0 131.7 98-165 153.6	0.500 0.468 0.402 0.420 0.348 0.510 0.4-0.6 0.558	68 68 m.p. 68 68 68 68 68	6.000 104.000 1.210 2.180 2.200 5.200 1.360 19-2900 0.546	68 68 68 68 m.p. 68 68 68 68	64.9 71.5 40.28 77.70 50.1	51,2 58.0 60.6 142.0 60.9 94.45 75.2 43.9 40-66 39.1	68 68 68 68 m.p. 68 68 68 68	0.086 0.093 0.160 0.960 0.084 0.066	68 68 68 68 68 68	- 11.0¹ - 144.6 - 87.7 176.4 - 42.9 42.3 - 69.7 - 201.5
Sodium Chloride Brine 20% by wt. 10% by wt. Sulfuric Acid and Water	220.8 215.5		0.745 0.865	68 68	3.800 2.850	68 68		71.8 66.9	68 68	0.337 0.343	68 68	2.6 20.6
• 100% by wt. • 90% by wt.	550.0 500.0		0.335 0.390	68 68	53.000 60.000	68 68		114.4 113.4	68 68	0.220	68	50.9 15.0
Toluene (C ₆ H ₃ CH ₃) Turpentine Water Xylene C ₆ H ₄ (CH ₈) ₂ • Ortho • Mata • Para	231.0 303.0 212.0	156.0 123.0 970.3	0.404 0.420 0.999	68 68 68	1.420 1.320 2.390	68 68 68	30.9 143.5	54.1 53.9 62.32	68 68 68	0.090 0.073 0.348	68 68 68	- 139.0 32.018
	291.0 283.0 281.0	149.0 147.0 146.0	0.411 0.400 0.393	68 68 68	2.010 1.520 1.620	68 68 68	55.1 46.9 69.3	55.0 54.1 53.8	68 68 68	0.900 0.900	68 68	- 13.0 - 53.0 + 56.0

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^{1.} Approximate solidification temperature.
2. Thermal conductivity units are Btu/(hr)(sq ft)(°F per ft)

TABLE 48	HEAT TRANSF	ER AND ELECTRICAL FORMULAS					
HEATT	RANSFER FORMULAS	KEY TO SYMBOLS					
HEAT	0-	QTot — Total Heat in Btu/hr					
TRANSMISSION	$\mathbf{Q}Tot = U \times A \times \Delta t$	U — Heat Transfer Coefficient in Btu/hr/ sq ft/°F					
	$QTot = Q_1 + QLat + Q_2 + QRes$	A — Surface Area thru which Heat is Conducted					
PRODUCT LOADS	$\mathbf{QSens} = \mathbf{W} \times \mathbf{C}_{1 \text{ or } 2} \times \Delta \mathbf{t}$	▲t — Temperature Difference Between Initial & Final Product Temp., Storage and Outside					
LOADO	$\mathbf{Q}_{Lat} = W \times h_{L}$	Temp., or Entering & Leaving Air Temperature					
	QRes = W × hr	Q ₁ — Sensible Product Heat Removal Above Freezing in Btu/hr					
	$QTot = 4.5 \times Cfm \times \Delta h$	Q ₂ — Sensible Product Heat Removal Below Freezing in Btu/hr					
00011810	$\mathbf{Q}Sens = 1.08 \times Cfm \times \Delta t$	Qsens — Sensible Heat in Btu/hr					
COOLING COILS	QLat = $0.68 \times \text{Cfm} \times \Delta \text{SH}$	QLat — Latent Heat in Btu/hr					
	4.5×Cfm× ΔSH	QRes — Respiration Heat in Btu/hr					
	$lbs/hr = \frac{4.3 \times cm \times \Delta SH}{7000 \text{ gr/lb}}$	C ₁ — Specific Heat Above Freezing in Btu/lb/°F					
	7000 gi7 ib	C ₂ — Specific Heat Below Freezing in Btu/lb/°F					
HEATING		HL — Latent Heat Of Fusion in Btu/lb					
COILS	QSens = $1.08 \times Cfm \times \Delta t$	HR — Heat Of Respiration in Btu/hr/lb					
HEAT RECLAIM		Cfm — Cubic Feet per Minute					
AND CONDENSER	$QSens = 1.08 \times Cfm \times \Delta t$	▲ H — Enthalpy Difference Between Entering & Leaving Wet Bulb in Btu/lb					
COILS	<u> </u>	△SH — Specific Humidity Difference (Grains of Water Removed per lb of Air).					
WATER	$\mathbf{Q}Tot = 500 \times Gpm \times (TLW - TEW)$	Gpm — Gallons per Minute					
HEATING	$\mathbf{Q}Tot = 500 \times Gpm \times (TLW - TEW)$	TEW — Entering Water Temp. in °F					
WATER	0	TLW — Leaving Water Temp. in °F					
COOLING	$\mathbf{Q}Tot = 500 \times Gpm \times (Tew - TLw)$	W — Product Weight in Pounds					
ELEC	TRICAL FORMULAS	CONVERSION FACTORS					
Full Load Current =	Watts I = P	4.5 — Converts Cfm to lbs/hr 60 Minutes					
(Single Phase)	Voltage E	$4.5 = \frac{60 \text{ Windres}}{13.35 \text{ ft}^3 \text{ per lb (Spec. Vol.)}}$					
Full Load Current	$= \frac{\text{Watts}}{1.732 \times \text{Voltage}} I = \frac{P}{1.732 \times E}$	1.08 — Combines 4.5 With Specific Heat					
(Three Phase)	1.732 × Voltage 1.732 × E	1.08 = 4.5 × 0.24 Btu/lb/°F					
Volts = Amperage	$e \times Resistance E = I \times R$	0.68 — Combines 4.5 With Heat of Vaporization & Grains per Ib					
Watts = Amperag		$0.68 = \frac{4.5 \times 1054.3 \text{Btu/lb}}{7000 \text{gr/lb}}$					
	$P_2 = P_1 \left(\frac{E_2}{E_1}\right)^2$	500 — Converts Gpm Water to lb/hr					
Watts (@ Voltage	E_2) = Watts (@ Voltage E_1) \times (Volts ₂ /Volts ₁) ²	$500 = \frac{60 \text{ Minutes} \times 62.4 \text{ lb/cu ft}}{7.48 \text{ gal/cu ft}}$					

Note: Heat Transfer Formulas are valid for standard air @ 69.8°F & 14.7 Psig; Conversion Factors must be utilized for other conditions.

TABLE	TABLE 49 FAHRENHEIT-CELSIUS TEMPERATURE CONVERSION CHART										
TE	TEMPERATURE			TEMPERATURE			MPERATU	RE	TEMPERATURE		
CELS.	CORF	FAHR.	CELS	CORF	FAHR.	CELS	CORF	FAHR.	CELS	CORF	FAHR.
40.0	40	40.0	6.7	+20	+68.0	+26.7	+80	+176.0	+60.0	+ 140	+284.0
39.4	39	38.2	6.1	+21	+69.8	+27.2	+81	+177.8	+60.6	+ 141	+285.8
38.9	38	36.4	5.5	+22	+71.6	+27.8	+82	+179.6	+61.1	+ 142	+287.6
38.3	37	34.6	5.0	+23	+73.4	+28.3	+83	+181.4	+61.7	+ 143	+289.4
37.8	36	32.8	4.4	+24	+75.2	+28.9	+84	+183.2	+62.2	+ 144	+291.2
-37.2	-35	-31.0	-3.9	+25	+77.0	+29.4	+85	+185.0	+62.8	+ 145	+293.0
-36.7	-34	-29.2	-3.3	+26	+78.8	+30.0	+86	+186.8	+63.3	+ 146	+294.8
-36.1	-33	-27.4	-2.8	+27	+80.6	+30.6	+87	+188.6	+63.9	+ 147	+296.6
-35.6	-32	-25.6	-2.2	+28	+ 82.4	+31.1	+88	+190.4	+64.4	+ 148	+298.4
-35.0	-31	-23.8	-1.7	+29	+84.2	+31.7	+89	+192.2	+65.0	+ 149	+300.2
-34.4	-30	-22.0	-1.1	+30	+86.0	+32.2	+90	+194.0	+65.6	+ 150	+302.0
-33.9	29	-20.2	-0.6	+31	+87.8	+32.8	+91	+195.8	+66.1	+ 151	+303.8
-33.3	28	-18.4	.0	+32	+89.6	+33.3	+92	+197.6	+66.7	+ 152	+305.6
-32.8	27	-16.6	+0.6	+33	+91.4	+33.9	+93	+199.4	+67.2	+ 153	+307.4
-32.2	26	-14.8	+1.1	+34	+93.2	+34.4	+94	+201.2	+67.8	+ 154	+309.2
-31.7	-25	-13.0	+1.7	+35	+95.0	+35.0	+ 95	+203.0	+68.3	+ 155	+311.0
-31.1	-24	-11.2	+2.2	+36	+96.8	+35.6	+ 96	+204.8	+68.9	+ 156	+312.8
-30.6	-23	-9.4	+2.8	+37	+98.6	+36.1	+ 97	+206.6	+69.4	+ 157	+314.6
-30.0	-22	-7.6	+3.3	+38	+100.4	+36.7	+ 98	+208.4	+70.0	+ 158	+316.4
-29.4	-21	-5.8	+3.9	+39	+102.2	+37.2	+ 99	+210.2	+70.6	+ 159	+318.2
28.9	-20	-4.0	+4.4	+40	+104.0	+37.8	+100	+212.0	+71.1	+ 160	+320.0
28.3	-19	-2.2	+5.0	+41	+105.8	+38.3	+101	+213.8	+71.7	+ 161	+321.8
27.8	-18	-0.4	+5.5	+42	+107.6	+38.9	+102	+215.6	+72.2	+ 162	+323.6
27.2	-17	+1.4	+6.1	+43	+109.4	+39.4	+103	+217.4	+72.8	+ 163	+325.4
26.7	-16	+3.2	+6.7	+44	+111.2	+40.0	+104	+219.2	+73.3	+ 164	+327.2
26.1	-15	+5.0	+7.2	+45	+113.0	+40.6	+ 105	+221.0	+73.9	+ 165	+329.0
25.6	-14	+6.8	+7.8	+46	+114.8	+41.1	+ 106	+222.8	+74.4	+ 166	+330.8
25.0	-13	+8.6	+8.3	+47	+116.6	+41.7	+ 107	+224.6	+75.0	+ 167	+332.6
24.4	-12	+10.4	+8.9	+48	+118.4	+42.2	+ 108	+226.4	+75.6	+ 168	+334.4
23.9	-11	+12.2	+9.4	+49	+120.2	+42.8	+ 109	+228.2	+76.1	+ 169	+336.2
-23.3	-10	+ 14.0	+10.0	+50	+ 122.0	+ 43.3	+110	+230.0	+76.7	+ 170	+338.0
-22.8	-9	+ 15.8	+10.6	+51	+ 123.8	+ 43.9	+111	+231.8	+77.2	+ 171	+339.8
-22.2	-8	+ 17.6	+11.1	+52	+ 125.6	+ 44.4	+112	+233.6	+77.8	+ 172	+341.6
-21.7	-7	+ 19.4	+11.7	+53	+ 127.4	+ 45.0	+113	+235.4	+78.3	+ 173	+343.4
-21.1	-6	+ 21.2	+12.2	+54	+ 129.2	+ 45.6	+114	+237.2	+78.9	+ 174	+345.2
-20.6	-5	+23.0	+12.8	+55	+131.0	+46.1	+115	+ 239.0	+79.4	+ 175	+347.0
-20.0	-4	+24.8	+13.3	+56	+132.8	+46.7	+116	+ 240.8	+80.0	+ 176	+348.8
-19.4	-3	+26.6	+13.9	+57	+134.6	+47.2	+117	+ 242.6	+80.6	+ 177	+350.6
-18.9	-2	+28.4	+14.4	+58	+136.4	+47.8	+118	+ 244.4	+81.1	+ 178	+352.4
-18.3	-1	+30.2	+15.0	+59	+138.2	+48.3	+119	+ 246.2	+81.7	+ 179	+354.2
-17.8	0	+32.0	+15.6	+60	+ 140.0	+48.9	+ 120	+ 248.0	+82.2	+ 180	+356.0
-17.2	+1	+33.8	+16.1	+61	+ 141.8	+49.4	+ 121	+ 249.8	+82.8	+ 181	+357.8
-16.7	+2	+35.6	+16.7	+62	+ 143.6	+50.0	+ 122	+ 251.6	+83.3	+ 182	+359.6
-16.1	+3	+37.4	+17.2	+63	+ 145.4	+50.6	+ 123	+ 253.4	+83.9	+ 183	+361.4
-15.6	+4	+39.2	+17.8	+64	+ 147.2	+51.1	+ 124	+ 255.2	+84.4	+ 184	+363.2
-15.0	+5	+41.0	+18.3	+65	+ 149.0	+51.7	+ 125	+ 257.0	+85.0	+ 185	+365.0
-14.4	+6	+42.8	+18.9	+66	+ 150.8	+52.2	+ 126	+ 258.8	+85.6	+ 186	+366.8
-13.9	+7	+44.6	+19.4	+67	+ 152.6	+52.8	+ 127	+ 260.6	+86.1	+ 187	+368.6
-13.3	+8	+46.4	+20.0	+68	+ 154.4	+53.3	+ 128	+ 262.4	+86.7	+ 188	+370.4
-12.8	+9	+48.2	+20.6	+69	+ 156.2	+53.9	+ 129	+ 264.2	+87.2	+ 189	+372.2
-12.2	+10	+50.0	+21.1	+70	+ 158.0	+54.4	+130	+266.0	+87.8	+ 190	+374.0
-11.7	+11	+51.8	+21.7	+71	+ 159.8	+55.0	+131	+267.8	+88.3	+ 191	+375.8
-11.1	+12	+53.6	+22.2	+72	+ 161.6	+55.6	+132	+269.6	+88.9	+ 192	+377.6
-10.6	+13	+55.4	+22.8	+73	+ 163.4	+56.1	+133	+271.4	+89.4	+ 193	+379.4
-10.0	+14	+57.2	+23.3	+74	+ 165.2	+56.7	+134	+273.2	+90.0	+ 194	+381.2
9.4	+15	+59.0	+23.9	+75	+ 167.0	+57.2	+ 135	+275.0	+90.6	+ 195	+383.0
8.9	+16	+60.8	+24.4	+76	+ 168.8	+57.8	+ 136	+276.8	+91.1	+ 196	+384.8
8.3	+17	+62.6	+25.0	+77	+ 170.6	+58.3	+ 137	+278.6	+91.7	+ 197	+386.6
7.8	+18	+64.4	+25.6	+78	+ 172.4	+58.9	+ 138	+280.4	+92.2	+ 198	+388.4
7.2	+19	+66.2	+26.1	+79	+ 174.2	+59.4	+ 139	+282.2	+92.8	+ 199	+390.2

Notes: 1. The numbers in bold-face type in the center column refer to the temperature, either in Celsius or Fahrenheit, which is to be converted to the other scale. If converting Fahrenheit to Celsius, the equivalent temperature will be found in the left column. if converting Celsius to Fahrenheit, the equivalent temperature will be found in the column on the right.

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^{2. 1} Degree Celsius = 1 Kelvin 3. Formula: Temp °F = 9/5 Temp. °C + 32; Temp. °C = 5/9 (Temp. °F - 32)

CHART 1

ESTIMATING UNIT COOLER CAPACITIES

GENERAL:

It is often necessary in the expansion or re-application of a cold storage room to estimate the capacity of existing equipment. Additionally, it is sometimes necessary to physically check evaporators to determine whether they are actually working. Chart 1 may be used for this purpose.

STEPS TO FOLLOW:

(1) Measure entering air temperature (t_1) and Leaving air temperature (t_0) .

- (2) Calculate Δt : $\Delta t = t_{10F} t_{20F}$
- (3) Measure face velocity and face area.
- (4) Calculate Cfm: Cfm = Vel fpm × Area ft2
- (5) Enter chart on the x-axis at the calculated Cfm and move vertically to the Δt calculated above. Read indicated capacity on the y-axis.
- (6) Apply the appropriate correction factor from the chart below to the indicated capacity for entering air temperatures other than $+20^{\circ}F$.

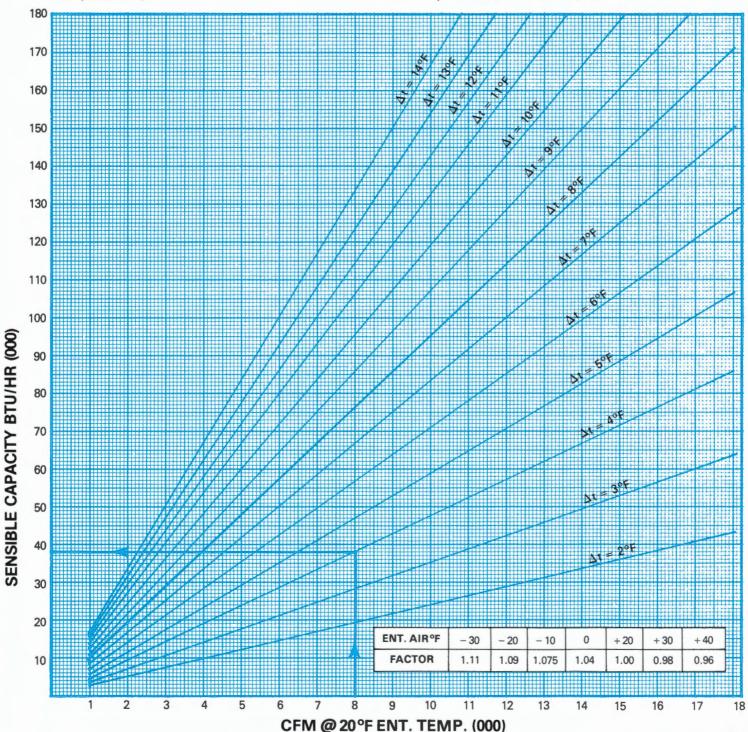
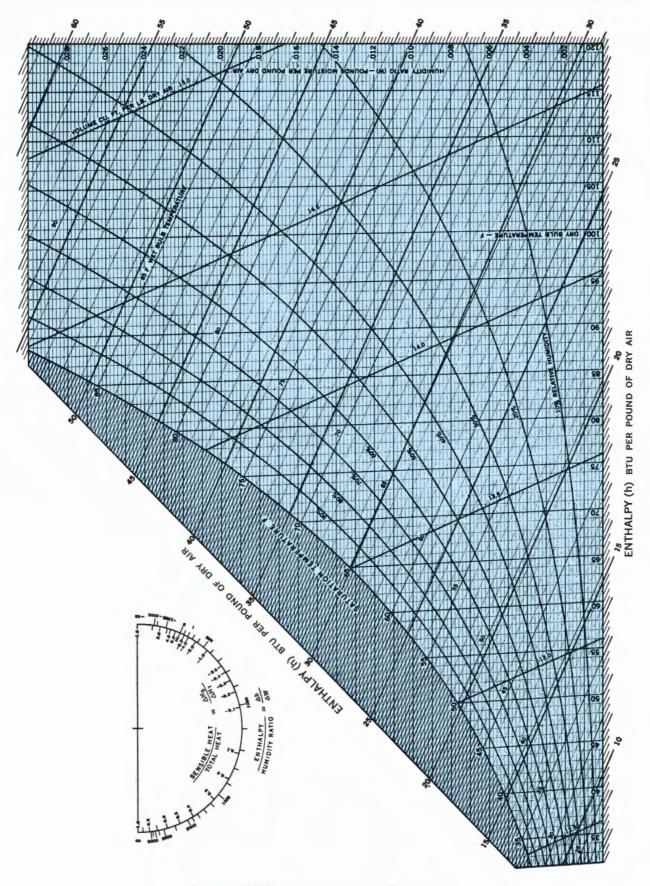


CHART 2

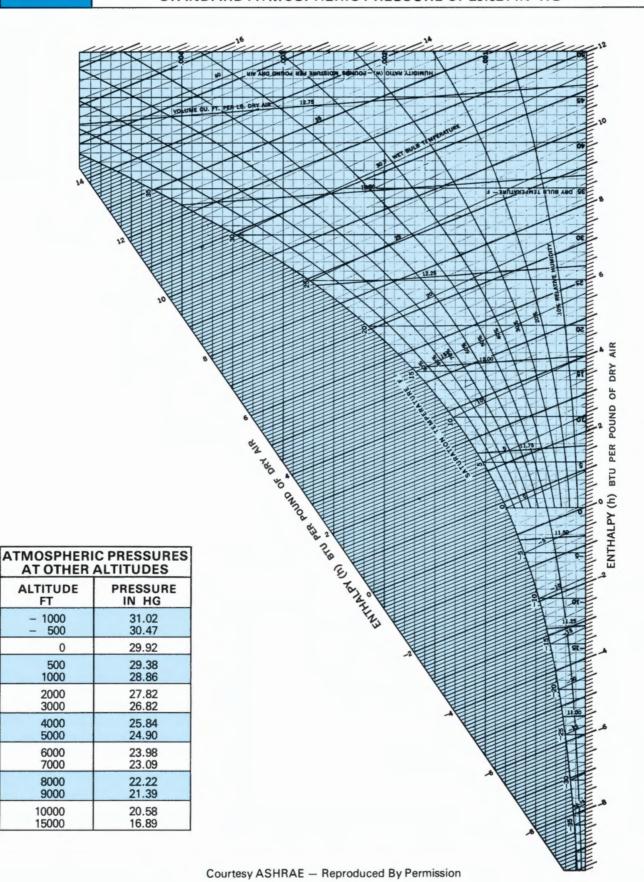
NORMAL TEMPERATURE PSYCHROMETRIC CHART (32 TO 130°F) STANDARD ATMOSPHERIC PRESSURE OF 29.921 IN HG



APPENDIX—CHARTS

CHART 3

LOW TEMPERATURE PSYCHROMETRIC CHART (– 40 TO 50°F) STANDARD ATMOSPHERIC PRESSURE OF 29.921 IN HG



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